



RICERCA SISTEMA ELETTRICO

HE-FUS3 Experimental Campaign for the Assessment of Thermal-Hydraulic Codes: Pre-Test Analysis and Test Specifications

Massimiliano Polidori



Report RSE/2009/88





Ministero dello Sviluppo Economico

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Massimiliano Polidori (ENEA)

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Sommario

This report deals with the design of an experimental campaign to be conducted in the HE-FUS3 loop (CR BRASIMONE) in order to provide an experimental data base for the assessment of thermal-hydraulic codes used for HTR and VHTR design and safety analysis.

In order to support the definition of the test matrix a pre-test activity has been carried out with the T/H system code RELAP5. To this aim a RELAP5 model of the loop (the related input deck is provided in attachment A of this report) has been developed taking advantage of the results of previous assessment activities and already available experimental data. The pre-test activity has allowed defining a set of transients representative of operational and accident conditions that are of particular meaning for the assessment of T/H codes: the plant start-up by steps, 2 Loss of Flow Accidents with a different dynamic of the accidental event, 2 Loss of Coolant Accidents at different loop pressure.

On the basis of the calculation results reported in the chapter 4 it has been possible to draw up the test specifications in attachment B taking into account the requirement for the operation of the HE-FUS3 loop and the actual conditions of the instrumentation implemented in the facility.



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1. Introduction

HE-FUS 3 is a helium facility that was designed and constructed at ENEA CR Brasimone in mid 90's for the thermal-mechanical testing of prototypical module assemblies of the DEMO reactor. Within the frame of the SP Safety (WP1) of the RAPHAEL Integrated Project, ENEA has offered the experimental data coming from a testing program carried out at the end of the nineties, for a benchmark exercise aimed at the validation of the system transient analysis codes for Very High Temperature Reactors (VHTR).

This benchmark exercise presently in progress has revealed, in agreement with previous assessment activity conducted on the same data, the large uncertainty that affect the data themselves. For this reason a new experimental campaign in the HE-FUS3 facility has been proposed within the framework of the ENEA-MSE research program with the objective to provide a reliable experimental data base for the assessment of thermal-hydraulic codes used for HTR and VHTR design and safety analysis. This new campaign will be also addressed to a complete characterization of the loop.

In order to support the definition of the test matrix a pre-test activity has been carried out with the T/H system code RELAP5. To this aim a RELAP5 model of the loop (the related input deck is provided in attachment A of this report) has been developed taking advantage of the results of previous assessment activities and already available experimental data. The pre-test activity has allowed defining a set of transients representative of operational and accident conditions that are of particular meaning for the assessment of T/H codes: the plant start-up by steps, 2 Loss of Flow Accidents with a different dynamic of the accidental event, 2 Loss of Coolant Accidents at different loop pressure.

On the basis of the calculation results reported in the chapter 4 it has been possible to draw up the test specifications in attachment B taking into account the requirement for the operation of the HE-FUS3 loop and the actual conditions of the instrumentation implemented in the facility.



2. Description of the HE-FUS3 facility

2.1 General Layout

Within the frame of the European Fusion Technology Program, ENEA in 1993 obtained an economic support from EU for the construction of a helium facility, called HE-FUS3 [1]. The facility, which had been planned for the thermal mechanical testing of prototypical module assemblies for the DEMO reactor, was chosen for the selected European Helium Cooled Pebble Bed (HCPB) Blanket design to be tested on ITER reactor. The facility, also defined as the European Helium Cooled Blanket Test Facility, is located at the ENEA Brasimone Laboratories in Italy.

Its eight loop configuration [2], shown in Fig. 2.1, supplies the helium flowrate to an experimental Test Section, where the mock-up of the HCPB Blanket can be tested. The purpose of the eight-shaped closed loop arrangement is to separate two zones at different temperatures, the cold one including the compressor and the hot one the Test Section. An economizer, placed at the crossover point, recovers the gas enthalpy before recirculating the helium through the compressor. Thereby it has been possible to reduce both the need for external power to get the required temperature at the Test Section inlet and the cooler size to reduce the compressor inlet temperature to the level of its maximum continuative operating temperature. The main performances expected for the facility are reported in Tab. 2.1.

The piping overall length is about 80 m, with an integral volume of 4m3 including 3m3 of the expansion tank and a weight of about 15 ton. The diameters of the main pipes were preliminary fixed at 4" (sch. 80) for the cold zone et 5" (sch.80) for the hot zone in order to limit at 20 m/s the helium velocity in the loop. The piping material is stainless steel AISI 316. Contact temperatures are reduced below 50 °C by means of heat insulator with special asbestos-free material, 60 to 160 mm in thickness.

Parameter		Design Value
Max Pressure	MPa	10.5
Max Temperature	°C	530
Inlet Compressor Max Temperature	°C	100
Compressor Helium Flow Rate	kg/s	0.5-0.35
Max Compressor Speed	rpm	18000
Max Compressor Head	MPa	0.5
Compressor Electrical Power	kVA	136
Heaters Electrical Power	kW	210
Economizer Thermal Power	kW	564
Air-Cooler Thermal Power	kW	280
Helium Tank Capacity	m ³	3
Test Section Electrical Power	kW	350
Helium Leak	mbar l/s	2 10 ⁻³

Tab. 2.1 -	HE-FUS3	Main	Performances
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2.2 Major Components

The main features of the loop components relevant for the code modeling (Fig. 2.2) are described in Tabs. 2.2 to 2.9, they are the following:

- A prototypical compressor (*K200*) with pneumostatic helium shaft supporting system developed by RTM company that has the electrical motor completely immersed in the helium flow. The electrical motor is provided with an inverter driving system capable of controlling the frequency in the range 5-300 Hz, driving the rotor speed at 300-18000 rpm.
- Three modules of a flanged immersion rod bundle electrical heater (E219-1/2/3) that can supply 70 kW of nominal power each (210 kW in total). The electrical supply, control and monitoring is independent for each module.
- A high efficiency (>79%), helium-helium economizer (*E214*) that has a tube shell geometry with vertical axis. The hot helium coming from the Test Section flows through a bundle of straight tubes that are welded between two tube plates and immersed in a cylindrical pressure vessel. The cold helium counter-flows in the shell zone where a series of diaphragm sheets allow improving the global thermal exchange.
- A counter flow helium-air heat exchanger that is located at the compressor inlet in order to reduce the corresponding helium temperature below the maximum design value (100°C). The helium flows inside the tube bundle whilst the air flows outside the external surface of the tubes. A helicoidal stainless steel sheet is welded on the outside surface of the tube to increase the overall thermal conductance.
- An expansion vessel that is located at the compressor outlet, in order to dump pressure and flow fluctuations during loop operation. The vessel is an 8 m high vertical cylinder with a volumetric capacity of 3 m^3 .
- Two mixers that are used in the loop for the temperature mixing between different main and by-pass flow rates.
- Four globe valves (FV 213, FV 234, FV 235 and FV 10) that are used for the loop regulation.
- A 7-pin bundle electrically heated Test Section with 50 kW of nominal power each. The heated pins are made of Ni-Cr spiral wires insulated by MgO powders with a Ni-Fe-Cr alloy cladding. The helium enters in the annular space between the tubular pressure vessel of the dummy mock-up and the Test Section pipe, flows down to the TS inlet then flow up within the pipe around the pins. The bundle is appropriately equipped with thermocouples in order to monitor the transient temperature field during the accident simulations planned in the facility.

Operation and control of the system are guaranteed through several auxiliary systems which are not relevant for the modeling: passive safety system, filling and pressure control system, vacuum preservation system, gas analysis and facility control system. The loop is also provided with 5 on/off valves for the safety control.





Fig. 2.2 – HE-FUS3 Vertical View



Parameter		Design Value
Maximum Design Helium Temperature	°C	160
Maximum Design Helium Pressure	MPa	10.5
Design Flowrate	kg/s	0.05 -0.35
Vessel Inside Diameter	mm	350
Vessel Sheet Thickness	mm	45
Vessel Total High	mm	700
Inlet Design Pressure	MPa	6.0
Outlet Design Pressure	MPa	6.5
Maximum Design Flowrate	kg/s	0,35
Maximum Design Inlet Temperature	°C	100
Mechanical Power	kW	90
Electrical Motor Power	kVA	110
Maximum Inverter Current	A	210
Maximum Inverter Frequency	Hz	400
Impeller Maximum Speed	rpm	18000
Impeller Diameter	mm	230
Motor Shaft Diameter	mm	65
Rotor Diameter	mm	130
Diametrical rotor Clearances	mm	1
Bearing clearances	μm	40

Tab. 2.2 – Compressor Main Design Parameters

Parameter		Design Value
Nominal Helium Inlet Temperature	°C	420
Nominal Helium Outlet Temperature	°C	525
Design Helium Temperature	°C	530
Design Cladding Temperature	°C	560
Design Helium Pressure	MPa	10.5
Design Helium Flowrate	kg/s	0.35
Electrical Power	kW	70
Overall Heat Transfer Surface	m²	5.09
Overall Thermal Conductance	W/m²K	809
Design Pressure Drop	Ра	1011
Rod Diameter	mm	15
Nr U-bent Rods		30
Rod Heated Length	mm	1800
Rod Cold Leg Length	mm	300
Nr of Diaphragm Plates		12
Diaphragm Pitch	mm	145
Vessel Internal Diameter	mm	270
Diaphragm Diameter	mm	268
Diaphragm Thickness	mm	3

Tab. 2.3 – Heater Single Module Main Design Parameters



Parameter		Design Value
Cold Helium Inlet Temperature	°C	130
Cold Helium Outlet Temperature	°C	440
Hot Helium Inlet Temperature	°C	530
Hot Helium Outlet Temperature	°C	220
Maximum Design Pressure	MPa	10,5
Cold Side Pressure Drop	Ра	1660
Hot Side Pressure Drop	Pa	212
Overall Heat Transfer Surface	m²	27.0
Overall Thermal Conductance	W/m ² K	258
1/2" Tube Multiplicity		73
1/2" Tube Outside Diameter	mm	21.3
1/2" Tube Thickness	mm	1.65
3/8" Tube Multiplicity		12
3/8" Tube Outside Diameter	mm	17.2
3/8" Tube Thickness	mm	1.65
Vessel Active Length	mm	4920
Diaphragm multiplicity		18
Diaphragm Thickness	mm	3
Diaphragm Diameter	mm	266
Tubes Support Plate Thickness	mm	23

Tab. 2.4 – Economizer Main Design Parameters

Parameter		Design Value
Nominal Helium Inlet Temperature	°C	240
Nominal Helium Outlet Temperature	°C	100
Design Helium Temperature	°C	240
Design Helium Pressure	MPa	10.5
Design Helium flow rate	kg/s	0.35
Design Helium Pressure Drop	Pa	4000
Nominal Air Inlet Temperature	°C	30
Nominal Air Outlet Temperature	°C	70
Design Air pressure	MPa	1
Design Air Flowrate	kg/s	6.1
Design Air Pressure Drop	Pa	1200
Nominal Thermal Power	kW	280
Overall Heat Transfer Surface	m²	165
Overall Thermal Conductance	W/m² K	400
Nr of 1⁄2" Finned Tubes		22
Finned Tube Outside Diameter	mm	21.3
Fin thickness	mm	0.4
Fin pitch	mm	3.4
Fan Electrical Power	kW	15
Fan Speed	rpm	50-3000

Tab. 2.5 – Air Cooler Main Design Parameters



Parameter		Design Value
Max Design Pressure	MPa	10.5
Max Design Temperature	°C	160
Maximum Design Flowrate	kg/s	0.35
Vessel Capacity	m ³	3
Vessel Outside Diameter	mm	890
Vessel Inside Diameter	mm	800
Vessel Total Height	mm	6638.2

Tab.2.6 - Expansion Vessel Main Design Parameters

Parameter		Design Value
Cold Mixer		
Nominal Cold Helium Temperature	°C	130
Nominal Hot Helium Temperature	°C	220
Design Helium Pressure	MPa	10.5
Design Helium Flowrate	kg/s	0.35
Hot Mixer		
Nominal Cold Helium Temperature	°C	130
Nominal Hot Helium Temperature	°C	530
Design Helium Pressure	MPa	10.5
Design Helium Flowrate	kg/s	0.35

Tab. 2.7 – Mixers Main Design Parameters

Nr Valve	Builder	LINE	Ø	operation
FV 213	NUOVO PIGNONE	D	1 1⁄2"	Regulated
FV 234	"	I	1 1⁄2"	"
FV 235	"	Н	1 1⁄2"	"
FV 10	"	С	1 1⁄2"	"

Tab. 2.8 – Main Valves Data Sheet

Parameter		Design Value
Nominal Helium Inlet Temperature	°C	420
Nominal Helium Outlet Temperature	°C	525
Design Pressure	MPa	20
Effective Power per Rod	kW	40
Max Cladding Temperature	°C	950
Max Heat Flux	W/cm ²	110.6
Heated Length	mm	2000
Rod Diameter	mm	9.5
Clad thickness	mm	1
TS Pipe		1 1/2" (sch.10)
Mock-up Tubular Vessel		3" (sch. 80)

Tab. 2.9 – 7-pin TS Main Design Parameters



2.3 Instrumentations

The instrumentation map of the facility is shown in Fig. 2.3 [3]. In the following is given a brief description of the instrumentation installed in the main loop:

- Flow measurements The volumetric flow is measured with Vortex flow meters of 2". In order to compute the mass flowrate, the signal is integrated with measurements of temperature and pressure upstream of the flow meter location. The accuracy is better than 0.5% for a flowrate above 10% of the measuring range.
- Temperature measurements The temperature sensors are thermocouples ANSI K (NiCr/NiAl) for temperature values higher than 200 °C and Platinum Thermoresistances ANSI PT 100 for lower temperature values. The accuracy is better than 0.5% on the measuring point.
- Pressure measurements The pressure measurements are based on diaphragm cell transmitters. Only one manometer, mounted on the expansion tank, is a Bourdon type without signal transmission. The accuracy of the gauges is better than 0.5% on the measuring point.
- 7-pin bundle thermocouples. 28 thermocouples are inserted in the cladding of the heating pins at different elevations and positions in the bundle (Fig. 2.4). In previous test 7 signals were related to these thermocouples (TT400, TT403, TT407, TT411, TT415, TT419, TT427).

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Fig. 2.3 – Instrumentation Map

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Fig. 2.4 - Test Section Thermocouples Location



3. Numerical Model

3.1 RELAP5 Computer Code

RELAP5 [4] is a thermal-hydraulic system code originally developed at the Idaho National Engineering Laboratory (INEL) for the US Nuclear Regulatory Commission (NRC) and extensively validated for Light Water Reactors, which potentially has a large flexibility to treat different fluids. ENEA is already using this peculiarity for the study of Accelerator Driven System cooled with heavy liquid metals (Lead and LBE).

The Relap5 program is based on a non-homogeneous and non-equilibrium model for the twophase system that is solved by a fast, partially implicit numerical scheme to permit economical calculation of system transients. The objective of the Relap5 development effort from the outset was to produce a code that included important first-order effects necessary for accurate prediction of system transients but that was sufficiently simple and cost effective so that parametric or sensitivity studies were possible. The code includes many generic component models from which general systems can be simulated. The component models include pumps, valves, pipes, heat releasing or absorbing structures, reactor point kinetics, electric heaters, jet pumps, turbines, separators, accumulators, and control system components. In addition, special process models are included for effects such as form loss, flow at an abrupt area change, branching, choked flow, boron tracking, and non condensable gas transport.

The system mathematical models are coupled into an efficient code structure. The code includes extensive input checking capability to help the user discover input errors and inconsistencies. Also included are free-format input, restart, re-nodalization, and variable output edit features. These user conveniences were developed in recognition that generally the major cost associated with the use of a system transient code is in the engineering labor and time involved in accumulating system data and developing system models, while the computer cost associated with generation of the final result is usually small. The development of the models and code versions that constitute Relap5 has spanned approximately 17 years from the early stages of Relap5 numerical scheme development to the present.

Relap5 represents the aggregate accumulation of experience in modeling reactor core behavior during accidents, two-phase flow processes, and LWR systems. The development of the last version Relap5/MOD3.3 for LWRs systems ha benefited from extensive application and comparison to experimental data in the LOFT, PBF, Semiscale, ACRR, NRU, and other experimental programs.

An extension of the RELAP5/Mod3.1 version, called ATHENA/Mod16, was developed at INEL for thermal-hydraulic analyses of the ITER Tokamak cooling systems. The main peculiarity of ATHENA was the capability to represent a wide variety of working fluids by means of a generalized equation of state. For instance, in ATHENA were implemented properties for water, helium, hydrogen, nitrogen, ammonia, potassium, sodium and lithium. The development of ATHENA was not continued with the following RELAP5 versions such as Mod3.2 and MOD3.3, however also the standard RELAP5 allows treating helium as a coolant by describing it as a pure incondensable gas.



Taking advantage of the characterization testing of the facility, in the late Nineties, ENEA began assessing the ATHENA/Mod1 capability to simulate helium cooled systems [5] and then the activity was continued with the most recent versions of RELAP5 [6]. This activity allowed developing and upgrading a RELAP5/MOD3.3 model of HE-FUS3 that is now used for the pretest calculations of the new test campaign.



3.2 Nodalization Scheme

A RELAP5 model of the facility that includes all the main parts of the loop (piping, heat exchangers, heaters, Test Section, valves, compressor, etc) described in the previous chapter has been developed by means of the generic RELAP5 modules (pipes, branches, pumps). The nodalization scheme is shown in Fig. 3.1. It consists of 211 thermal-hydraulic nodes, 215 junctions, and 46 heat structures with a total number of mesh points of about 1400.

The nodalization has been developed according to the rules and the advice contained in the RELAP5/Mod3.2 user's documentation [4]:

- the volume flow lengths have been imposed generally between 0.5 m and 1 m, in order to reach a compromise between a reasonable calculation time, limiting the control volume number, and a good simulation of the peculiar features of the system (geometry, materials etc.)
- the mesh thickness for the conduction heat transfer calculation has been selected generally less than 10 mm
- non-equilibrium and smooth area change option have been used in the junctions, choking and stratification models have generally been applied.



Fig. 3.1 – RELAP5 Nodalization Scheme of HE-FUS3



3.3 Modeling Assumptions

3.3.1 Economizer

The Economizer is simulated by means of the 2 pipes 200 and 400, respectively representing the shell side and the tube side, and thermally coupled through the pipe wall heat structure. A tuning has been performed to obtain design performance in term of heat transfer capability and pressure drop.

Due to its great importance for the temperature distribution in the hot part of the loop, the simulation of heat exchanger performance has represented a particular challenge to model. The heat transfer coefficient for convection in single phase gas, calculated by RELAP5 with the standard Dittus-Boelter correlation, is inadequate for the shell side, where the presence of diaphragms causes helium cross-flow and thermal exchange improvement. In order to increase the heat transfer coefficient, a common place approach has been applied to the shell side by reducing appropriately the heating diameter. Some available steady state tests have allowed tuning the heating diameter value in order to obtain temperature distributions in good agreement with the experimental data [5]. The value introduced in the model (1.63 10⁻³ m against 1.82 10⁻² m) has been selected as a compromise between different conditions.

Stand alone model of the shell side/tube side of the Economizer has been built to tune the energy loss coefficients. In order to match the design pressure drops at design flow conditions (i.e. mass flow, temperature, etc) it has been found the value of a dimensionless concentrated pressure drop coefficient to assume on the 18 junctions representing the diaphragms of the shell side (k=8 referred to the relative cross section area).

3.3.2 Compressor

Because a specific module for this component is not available in RELAP5 the rotating pump component is used for the simulation of the compressor (component 600).

In this case, the interaction of the pump and the fluid should be described by means of the empirically developed curves relating pump head (H), and torque (τ) to the volumetric flow (Q) and pump angular velocity (ω) (pump characteristic curves). These curves, frequently referred to as four-quadrant curves, for use in Relap5, must be converted to a more condensed form, called homologous curves, which uses dimensionless quantities, involving the head ratio (H/H_r), torque ratio (τ/τ_r), volumetric flow ratio (Q/Q_r) and angular velocity ratio (ω/ω_r). These ratios are actual values divided by rated values that are the design point or point of maximum efficiency for the pump [4].

The homologous curves in the model was originally provided on the basis of characterisation tests both for head and torque (this latter has been deduced from helium heating) performed on 1998 [7]. As in 1999 a new rotor was mounted in the facility the characterization tests were repeated [8] and the related data (Tab. 3.1), that refers to the compressor sketch in Fig. 3.2 has been used to construct a new set of homologous curves for the present simulation of the compressor behaviour (Figs. 3.3 and 3.4).



The compressor cooling system model is simulated by means of a constant compressor by-pass flow rate, properly cooled to simulate the heat removed by a two stage water heat exchanger. This helium auxiliary flow is derived from the compressor outlet and then reintroduced at the compressor inlet. On the basis of compressor performance tests the by-pass mass flowrate and the recycling temperature are described as a function of the actual pump head by means of RELAP5 control components.

Compressor Character	rization Tes	sts 19/02/	/99						
FV10	FV 213	G 212	DP 201	Ti 202	Pi 298	Te out 204	Tcusc 276	Te rit 275	G 256
rpm	%	kg/s	bar	°C	bar ass	°C	°C	°C	kg/s
10000 (55.5%)	100	0,068	0,57	71,8	23,1	81,8	43,2		0,018
	80	0,066	0,59	71,8	23,1	82,1	43		0,019
	70	0,062	0,61	71,8	23	82,3	42,9		0,019
	60	0,055	0,65	71,6	23	82,6	42,9		0,020
	50	0,046	0,7	71,6	22,9	83,5	42,9		0,020
	40	0,036	0,75	71,4	22,9	84,8	43		0,021
	30	0,024	0,83	71,2	22,8	86,4	43,4		0,022
12000 (66.6%)	100	0,081	0,79	71,8	22,9	88,9	46,9		0,023
	80	0,078	0,81	71,6	22,9	89,4	47,1		0,023
	70	0,073	0,85	71,8	22,8	90,1	47,2		0,023
	60	0,065	0,9	71,5	22,8	91,3	47,3		0,024
	50	0,055	0,95	71,5	22,7	93,5	47,7		0,025
	40	0,043	1,04	71,4	22,6	97	48,4		0,026
	30	0,029	1,11	71,2	22,5	101,2	49,1		0,027
13000 (72.2%)	100	0,087	0,92	72,1	22,8	93,3	49,8		0,024
	80	0,084	0,94	71,8	22,8	93,6	49,8		0,025
	70	0,079	0,97	71,8	22,8	95,1	50,3		0,025
	60	0,071	1,03	71,5	22,7	96,5	50,6		0,026
	50	0,059	1,1	71,5	22,7	99,6	51,2		0,027
	40	0,046	1,18	71,5	22,6	103,7	52		0,028
	30	0,031	1,3	71,1	22,5	110	53,2		0,029
14000 (77.7 %)	100	0,094	1,05	71,9	22,8	98	52,9		0,026
	80	0,091	1,07	71,6	22,8	98,6	53,3		0,026
	70	0,085	1,11	72,2	22,9	102,7	55,4		0,027
	60	0,076	1,18	72,1	22,8	112,5	56		0,028
	50	0,063	1,26	73,1	22,7	109,2	56,8		0,029
	40	0,05	1,37	70,5	22,6	113	56,9		0,030
15000 (83.3%)	100	0,101	1,2	71,8	22,9	103,6	56,8		0,028
	80	0,098	1,22	71,8	22,9	104,5	56,9		0,028
	70	0,091	1,27	71,6	22,8	105,9	57,3		0,029
	60	0,081	1,35	71,5	22,7	108,6	57,8		0,030
	50	0,067	1,45	71,2	22,6	113,5	58,8		0,031
16000 (88.8%)	100	0,107	1,34	72,8	22,9	108,9	58,8		0,030
	80	0,104	1,38	71,5	22,8	109,2	59,1		0,031
	70	0,101	1,43	71,4	22,8	111	59,5		0,031
	60	0,087	1,51	71,5	22,7	114	60,2		0,032

Tab. 3.1 – Compressor Characterization Tests (new rotor)





Fig. 3.2 – Scheme of the Compressor Cooling System



Fig. 3.3 – RELAP Homologous Head Curve





Fig. 3.4 - RELAP Homologous Torque Curve

3.3.3 Air Cooler

The Air Cooler model contains a detailed primary side (helium) model while the secondary side (air) with its regulation system has been modelled in a simplified way.

The Air Cooler primary side model (pipe 460) has been set up in order to tune the dimensionless pressure loss coefficients on the basis of the design data of the heat exchanger. It reproduce the coil configuration, made of straight parts and curves, with 11 junctions that represent the pipe bends where a dimensionless concentrate pressure drop coefficient equal to 0.8 has been set in order to reproduce design pressure drop.

The secondary side (air) of the air cooler with its regulation system is not modelled. The temperature at the compressor inlet is kept lower than the maximum continuative operating temperature through a heat sink thermally coupled with the air cooler tubes.

3.3.4 ElectricalHeaters

Each Electrical Heater has been modelled in the same way, as follows:

- Pipes 240 260 300 represent the Electrical Heaters, A stand alone model of a single Electrical Heater module has been built in order to tune the energy loss coefficients. In order to match the design pressure drops at design flow conditions (i.e. mass flow, temperature, etc) it has been found the value of a dimensionless concentrated pressure drop coefficient to assume on the 12 junctions representing the heater diaphragm plates.
- Branches 210 230 250 270 290 310 and pipes 220 280 represent Electrical Heaters inlet, outlet and connection: it has been associated to these components the typical inlet, outlet and 90° curve energy loss coefficients.
- Single junctions 225 275 represent the manual valves HV 250 HV 252 at with are associated pertinent dimensionless concentrate pressure drops.



Each bundle of heating rods, which are made of Ni - Cr spiral wires insulated by MgO powders, is modelled through a Relap5 cylindrical heat structure component which preserves design geometrical parameters (i.e. pin radius, thickness, total external surface). Electrical power supply is independent for each bundle. The heat transfer coefficient at the boundary of the structure in contact with the coolant is computed by the code with the "Dittus Boelter" correlation.

3.3.5 Test Section

The hydraulic path of the test section has been accurately modelled with pipe (340 and 360) and branch (330-352-365-367-370) with suitable energy loss coefficient for bends and flow section variations. A Test Section stand alone model has been used to tune pressure drop coefficient. In order to match the design pressure drop at different flow conditions some assumptions have been made on distributed friction losses:

- In pipe 340 that represents the annular downward pipe the model that specifies that wall friction effects are to be computed have been activated and the roughness of the wall has been set equal to 0, moreover the energy loss coefficient of the grids (two) is set to a low value (k=0.1)
- In pipe 360 that represents the upward pipe the model that specifies that wall friction effects are to be computed have been activated and the roughness of the wall has been set equal to 0, moreover the energy loss coefficient of the grids (two) is set to a low value (k=0.1)

The seven electrically heated pins are modelled through a Relap5 cylindrical heat structure component which preserves design geometrical parameters (i.e. pin radius, thickness, total external surface) and provides the required power. Table of thermo-physical properties are provided in the model for the three material layers that compose the heat structure (i.e. Ni-Cr spiral wires, MgO insulator material and Ni – Fe – Cr alloy cladding). The heat transfer coefficient at the boundary of the structure in contact with the coolant is computed by the code with the "Dittus Boelter" correlation.

Downward and upward pipes are thermally coupled by means of a cylindrical heat structure representing the pipe walls and the stagnant helium gap between them that has a fundamental role in reducing the effect of this coupling.

3.3.6 Regulation Valves

The flow control valves (FV213, FV235, FV234) have been modelled by using Relap5 motor valve (FV213, FV235) and servo valve components (FV234). For these components a suitable Flow Coefficient (Cv) vs. percent Stroke curve has been provided starting from the Cv data supplied by the manufacturer (Fig. 3.5). On the contrary, regulation valve FV10 (equal to the previously cited three) has been modelled as a junction with an appropriate concentrated pressure drop coefficient derived from the flow coefficient data.





Fig. 3.5 – Characteristic of the Regulation Valves

3.3.6 Control System

FNFN

Loop pressure and mass flowrate are controlled in the numerical model respectively by means of a boundary condition imposing the pressure in the expansion tank, and through the pump rotation speed.

The valve FV234, which is modelled by means of the Relap5 servo valve component 172, regulates the hot by-pass flow (i.e. a cold temperature helium flow rate taken upstream of the Economizer cold side inlet) in order to avoid high temperature at the Test Section inlet. To do this the opening of the valve is driven by a proportional-integral controller that causes a specific valve position consequent to a specific deviation of the regulated parameter (inlet temperature at TS).

3.3.7 Heat Losses

All the hydraulics components of the loop are thermally coupled with the environment in order to simulate the actual thermal energy losses. The external loop walls have been described as a multi-layers material (stainless steel, mineral fibre wool) and thermally coupled with the environment. The external heat transfer coefficient has been calculated with a correlation of natural convection in turbulent regime.

However, direct observations made on the facility during the past experiments reports that there are zones of the loop in which the thermal losses are significant (e.g. Economizer – Heaters) [8]. The observed "thermal bridges" have been simulated through a high fictitious thermal conductivity of the rock wool (see Table 3.2) imposed in the hot loop portion. These values have been calibrated on the basis of an evaluation of the real heat losses obtained through thermal balance on the loop hot zones and on the single components. For all the other heat structures simulating the external heat losses, the heat conductivity of the rock wool set is in the range of nominal values for the loop working temperatures.



Part of the Loop	Temperature (°C)	λ (w/m°C)
	0	0.035
	200.	0,.05
Cold zone	350.	0.075
	500.	0.10
	650.	0.125
Electrical Heaters and Economizer	0. – 650,	0.35
Test Section	0. – 650.	0.25

Table 3.2 – Insulator Material Thermal Conductivity

3.3.8 Helium Leakage

According to the design performance of the facility the helium leakage is very low and should not have valuable effects on loop conditions (Table 2.1), therefore it has not been simulated in the numerical model.



3.3 Numerical Model Assessment

The RELAP5 described above has been assessed against available HE-FUS3 experimental data, before performing the pre-test analysis to support the design of the experimental program to conduct in the HE-FUS3 facility within the ENEA/MSE framework program.

The experimental data already available for the facility are described in Ref. [8]. Most part of these data, which are currently being used for the RAPHAEL benchmark exercise, are related to the operation of the facility with the original rotor of the compressor. As the characteristics of the compressor with the new rotor mounted at the beginning of 1999 are quite different respect to the original ones, the only experimental data we can rely to assess the RELAP model of the present loop configuration change are the two steady state recorded on February 1999.

The previous re-interpretation activities of the HE-FUS3 old data [5], [6] have highlighted the large uncertainty on the experimental parameters that has allowed assessing the numerical results from a qualitative point of view a rather than a quantitative one. The main source of uncertainty is the actual amount of the heat losses in the loop that joined to the lack of a precise measurement of the TS electrical power has a relevant effect on the loop temperature distribution. As the maximum temperature of the helium is the most important parameter to be considered in the pretest calculations in order to guarantee the loop integrity, the two available steady state have been used, to estimate, in particular the calculation accuracy of this parameters.

To this aim the simulation of the first steady state at 95 Kw electrical power in TS has carried out for the RELAP5 model set-up in order to obtain calculation results in good agreement with the experimental data. The simulation of the second steady state at 70 kW electrical power in TS has been performed with the same model in order to evaluate the accuracy of the calculation results we can expect in the pre-test activity.

3.3.1 Re-calculation of the 40%ST19-02-99 Steady State

The relevant boundary conditions introduced in the RELAP model for the recalculation of the HE-FUS3 steady state are reported in Table 3.3. The final results of the simulation obtained by means of an interative calculation process that has allowed the model tuning are compared with the experimental data in Table 3.4.

In the following are listed and commented the changes made in the model to obtain the good agreement between experiment and calculation showed in the Table 3.4:

- The Heat Losses in the loop have been re-calibrated in order to match the experimental thermal balance in the hot part of the loop that has been calculated by means of measured parameters.
- The heating diameter in the shell side of economizer heat structure has been re-calibrate in order to obtain inlet and outlet temperature of the component in good agreement with the experimental data.
- The heating diameter of the heat structure simulating the 7 pins of the TS has been doubled respect to the theoretical value thus decreasing the heat transfer coefficient in order to calculate a pin cladding temperature that is interpolated by the experimental results. A more precise calibration is not possible due to the large spread of the measurements in the different pins.



Controlled Parameter	Experimental Value
Loop Pressure (bar)	23.
TS Electrical Power (kW)	95.
Heaters Electrical Power (kW)	0.
Loop Mass Flowrate (kg/s)	0.99
TS Helium Inlet Temperature	350.
Valve F213 % Opening	88

Tab.3.3 – 40%ST19-02-99 Steady State Relevant Boundary Conditions

Parameter	HE-FUS3 Tag	Experimental Value	RELAP Reference	Calculated Value
Total Pressure Drop (bar)	PD201	1.12	cntrlvar 40	1.11
TS Pressure Drop (bar)	PD229	0.466	cntrlvar 41	0.445
Compressor Speed (rad/s)	ST270	1501.	pmpvel 600	1548.
Valve F234 % Opening	ZT234	47.7	vlvarea 172	51.0
E214 Inlet Cold Side Temperature (°C)	TR215	90.0	cntrlvar 215	94.0
E214 Outlet Cold Side Temperature (°C)	TR216	460.	cntrlvar 216	460.
E219/3 Outlet Temperature (°C)	TR220	448.	cntrlvar 220	445.
E219/2 Outlet Temperature (°C)	TR222-TR297	442 445.	cntrlvar 222	438.
E219/1 Outlet Temperature (°C)	TR223-TR236	433 434.	cntrlvar 223	427.
E214 Inlet Hot Side Temperature (°C)	TR217	521.	cntrlvar 217	520.
E214 Outlet Hot Side Temperature (°C)	TR218-TR239	230. – 234.	cntrlvar 218	230.
Air Cooler Outlet Temperature (°C)	TR242-TR202	75. – 74.	cntrlvar 202	75.
Compressor Outlet Temperature (°C)	TR204	99.	cntrlvar 204	97.
Pin Temperature at 0.25 m High (°C)	TT400	556	cntrlvar 210	531.
Pin Temperature at 1.25 m High (°C)	TT403, TT407, TT411, TT415, TT419, TT427	688-774	cntrlvar 211	710.

Tab.3.4 – 40%ST19-02-99 Steady State Comparison of Experimental and Calculated Parameters

3.3.2 Re-calculation of the 30%ST19-02-99 Steady State

The relevant boundary conditions introduced in the RELAP model for the recalculation of the HE-FUS3 steady state are reported in Table 3.5. The final results of the simulation obtained with the frozen model tuned in the previous calculation are compared with the experimental data in Table 3.6.

The agreement between calculation results and experimental data remains quite good. The major discrepancies appears in the temperatures of the heaters zone, thus confirming that the heat losses in the loop deduced from the experimental data are affected by a very high uncertanty. One reason for this could be that the data were acquired at not completely stabilized steady state conditions, but we do not have any evidence to confirm this hypothesis.

In order to avoid an under-estimation of the maximum helium temperature as a consequence of an over estimation of the heat losses in the hot part of the loop, on the basis of the results of the



HE-FUS3 model assessment, it has been decided to run the pre-test calculatios with the nominal value for the heat conductivity of the insulant material (rock wool). That means not to use a fictious value of the rock wool thermal conductivity for simulating "thermal bridges" effects. This assumption is conservative for the calculation of the loop maximum temperatures and makes us more confident that the maximum design temperature of the loop (530 °C) will not be exceded during the experimental campaign, in particular in the tests simulating accident transients .

Controlled Parameter	Experimental Value
Loop Pressure (bar)	24.
TS Electrical Power (kW)	71.
Heater 2 Electrical Power (kW)	10.
Loop Mass Flowrate (kg/s)	0.99
TS Helium Inlet Temperature	350.
Valve F213 % Opening	88

Tab.3.5 - 30%ST19-02-99 Steady State Relevant Boundary Conditions

Parameter	HE-FUS3 Tag	Experimental Value	RELAP Reference	Calculated Value
Total Pressure Drop (bar)	PD201	1.12	cntrlvar 40	1.11
TS Pressure Drop (bar)	PD229	0.441	cntrlvar 41	0.410
Compressor Speed (rad/s)	ST270	1484.	pmpvel 600	1474.
Valve F234 % Opening	ZT234	42.0	vlvarea 172	42.0
E214 Inlet Cold Side Temperature (°C)	TR215	89.0	cntrlvar 215	92.0
E214 Outlet Cold Side Temperature (°C)	TR216	408.	cntrlvar 216	409.
E219/3 Outlet Temperature (°C)	TR220	399.	cntrlvar 220	397.5
E219/2 Outlet Temperature (°C)	TR222-TR297	417 420.	cntrlvar 222	407.
E219/1 Outlet Temperature (°C)	TR223-TR236	420 421.	cntrlvar 223	406.
E214 Inlet Hot Side Temperature (°C)	TR217	467.	cntrlvar 217	475.
E214 Outlet Hot Side Temperature (°C)	TR218-TR239	204. – 208.	cntrlvar 218	206.
Air Cooler Outlet Temperature (°C)	TR242-TR202	75. – 74.	cntrlvar 202	75.
Compressor Outlet Temperature (°C)	TR204	98.	cntrlvar 204	95.

Tab.3.6 - 30%ST19-02-99 Steady State Comparison of Experimental and Calculated Parameters



4. **Pre-test Calculations**

The HE-FUS3 experimental program has been proposed in order to provide an experimental data base for the assessment of thermal-hydraulic codes used for HTR and VHTR design and safety analysis. Moreover, the experimental program will be also addressed to a better characterization of the facility, that is a fundamental thing in the development of the facility numerical model. In fact, previous works [5], [6] concluded that the large uncertainty present in the old experimental data makes very difficult the evaluation of the code results.

With these objectives in mind the pre-test activity has allowed defining a set of transients: plant start-up step by step, 2 Loss of Flow Accidents with a different dynamic of the accidental event, 2 Loss of Coolant Accidents at different loop pressure that are described in the following subsections.



4.1 Start-up by steps

A start-up procedure by steps has been investigated in the pre-test analysis in order to collect data at different steady state conditions for the characterization of the heat losses in the hot zone of the loop and of the thermal exchange performance in the economizer. In order to have more flexibility on the heating up dynamics only TS electrical power been considered as heat source in this transient.

In the Table 4.1 are reported the relevant boundary conditions for the start-up transient. A 3-step increase of supplied power combined with a 3-step increase of compressor speed allow defining 5 different steady states characterized by different temperature distributions in the loop hot zone and different mass flowrates in the economizer. Each step of power and compressor speed lasts 2000 seconds in order to have 1000 seconds for each steady state condition given by a combination of the previous ones (Fig. 4.1). It is important to notice that stabilized conditions are obtained after some hundred seconds of calculation because the thermal capacities of the loop materials have been decreased by a factor 1000. This assumption has been made only in this calculation where the interest is not to simulate the response of the system to accidental events as in the following transient calculations, but just to reproduce the different steady state conditions that will be recorded during the start-up.

The main loop parameters calculated are reported in Figs. 4.2 to 4.10. Fig. 4.1, in particular, shows how the loop temperature stabilizes at 5 different levels during the start-up. In Fig.4.3 it can been noticed that the temperature regulation at the inlet of the test section is active only in the second part of the start-up when the by-pass valve opens (Fig. 4.9) to limit this temperature below 300 °C. Finally, the steps showed in Fig. 4.10 by the total pressure drop in the loop and in the test section that follow both the mass flowrate and the temperature increase are a further interesting information for the characterization of the loop.

In order to evaluate the time needed to achieve a sufficiently stabilized steady state in the loop after having modified the boundary conditions, the first step of the start-up has been re-calculated with actual thermal capacities. The hot loop temperature and the total heat loss reported in Figs. 4.11 and 4.12 show that after 50000 s the loop has achieved acceptable steady state conditions. In fact, the temperature variations are less that 1 °C for hour and the total heat loss variation is lower that 3%.

Initial and Boundary Conditions	Value	Time (s)
Initial Pressure (bar)	30.	0.
TS Electrical Power (kW)	0.	0.
Compressor Speed (rad/s)	1000.	0.
1 st Step of Power (kW)	36.	300.
1 st Step of compressor speed (rad/s)	1200.	1300.
2 nd Step of Power (kW)	52.5	2300.
2 nd Step of compressor speed (rad/s)	1480.	3300.
3 rd Step of Power (kW)	75.	4300.
TS Helium Inlet Temperature (°C)	300.	All transient
Air Cooler Helium Outlet Temperature (°C)	75	All transient
Valve F213 % Opening	100.	All transient

Table 4.1 – Initial and boundary conditions for the start-up transient

_ \ _ \		Sigla di identificazione	Rev.	Distrib.	Pag.	di
ENEL	Centro Ricerche Bologna	FPN – P9LU – 015	0	R	30	132



Fig. 4.1 – Compressor Speed and TS Power



Fig. 4.2 - Inlet and Outlet Economizer Temperatures

	Centro Ricerche Bologna	Sigla di identificazione	Rev.	Distrib.	Pag.	di
ENEL		FPN – P9LU – 015	0	R	31	132





Fig. 4.4 – Inlet and Outlet Air Cooler Temperatures

		Sigla di identificazione	Rev.	Distrib.	Pag.	di
ENEL	Centro Ricerche Bologna	FPN – P9LU – 015	0	R	32	132













Fig. 4.8 – Loop Mass Flowrates




Fig.4.9 – Main and Bypass Valve Opening



Fig.4.10 – Loop and Test Section Pressure Drops





Fig. 4.11 – Inlet and Outlet Economizer Temperatures (actual thermal capacities)



Fig. 4.12 – Heat Losses (actual thermal capacities)



4.2 LOFA through bypass valve opening

A Loss of Flow Accident with a sharp reduction of the TS mass flow rate has been simulated with a complete opening of the valve F235 that allows the helium to bypass the hot part of the loop. This procedure to simulate a LOFA scenario was already applied with success [8] during the characterization of the facility in 1998.

The main point investigated with the pre-test calculation has been the maximum helium and pin cladding temperatures reached during the transient in order to verify that the design limits for the loop and for the pin cladding are not attained. The results of the calculation reported in Figs. 4.13 to 4.23 show that the margin respect to these limits is sufficient also taking into account the conservative assumptions made in the calculation model.

The LOFA scenario, which start from the steady state conditions attained at the conclusion of the start-up transient, is simulated for 1000 s before retrieving the initial state of the loop as showed by the boundary conditions reported in Table 4.2. The operation of the valve F235 is reported in Fig. 4.13 together with valve FV213 and FV234, while the main valve FV213 remains stuck open during the transient the bypass valve FV234 start opening following the helium temperature increase in the heaters zone in order to guarantee 300 ° at the TS inlet. The mass flowrates in Figs. 4.14 and 4.15 coherently follow the valve operations, in particular, the Test Section mass flowrate is halved after the valve opening. Just before the closing of the bypass valve the maximum helium temperature reaches 500 °C against a limit of 530° C (Fig. 4.19), the temperature increase is very slow so the risk to exceed this value is practically null. Larger margin is showed by the temperature of the TS pin cladding (Fig. 4.22) that reaches the peak value of 712 °C (against a limit of 800 °C adopted for the 7-pin protection) after 600 s of transient.

Initial and Boundary Conditions	Value	Time (s)
Initial Pressure (bar)	33.7	0.
TS Electrical Power (kW)	75.	0.
Compressor Speed (rad/s)	1480.	0.
Valve F235 beginning opening (%)	0.	300.
Valve F235 complete opening (%)	100.	304.
Valve F235 beginning closure (%)	100.	1300.
Valve F235 complete closure (%)	0.	1304.
TS Helium Inlet Temperature (°C)	300.	All transient
Air Cooler Helium Outlet Temperature (°C)	75.	All transient
Valve F213 % Opening	100.	All transient

Table 4.2 – Initial and boundary conditions for the LOFA through by-pass

		Sigla di identificazione	Rev.	Distrib.	Pag.	di
EN.	Centro Ricerche Bologna	FPN – P9LU – 015	0	R	37	132

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Fig.4.13 – Main and Bypass Valves Opening



Fig.4.14 - Cold Loop, Test Section and Cold-Bypass Mass Flows





.Fig. 4.15 - Test Section, Economizer and Hot-Bypass Mass Flows



Fig. 4.16 – Loop and Test Section Pressure Drops





Fig. 4.17 – Inlet and Outlet Economizer Temperatures



Fig. 4.18 – Heaters Zone Temperatures

		Sigla di identificazione	Rev.	Distrib.	Pag.	di
ENEL	Centro Ricerche Bologna	FPN – P9LU – 015	0	R	40	132



Fig. 4.19 – Inlet and Outlet TS Temperatures



Fig. 4.20 – Inlet and Outlet Air Cooler Temperatures





Fig. 4.21 – Inlet and Outlet Compressor Temperatures









. Fig. 4.23 – Loop Pressures



4.3 LOFA through Compressor Speed Reduction

A Loss of Flow Accident with a slower reduction of the TS mass flow rate that is a typical effect of the compressor coastdown has been simulated with a reduction of the compressor speed. As in the previous LOFA transient, the main point investigated with the pre-test calculation has been the maximum helium and pin cladding temperatures reached during the transient. The results of the calculation reported in Figs. 4.24 to 4.33 show that the margin respect to these limits is sufficient also taking into account the conservative assumptions made in the calculation model.

The LOFA scenario, which start from the steady state conditions attained at the conclusion of the start-up transient, has been simulated by means a reduction of the compressor speed in 50 s. After 1000 s the initial compressor speed has been restored in 50 s as well. The initial and boundary conditions of the transient are reported in Table 4.3.

Figure 4.24 shows the reduction of the TS mass flowrate following the reduction of the compressor speed, which results about halved at the lower speed. Due to the decease of mass flowrate the temperatures increase in the hot part of the loop. Just before the restoring of the initial pump speed the maximum helium temperature reaches 470 °C (Fig. 4.27) that is a relevant margin respect to the limit of 530° C, and more relevant it is the margin of the pin cladding temperature, 651 °C against the limit of 800 °C (Fig. 4.30). The behavior of the bypass valve FV234 in Fig. 4.33 is similar to the previous LOFA transient.

Initial and Boundary Conditions	Value	Time (s)
Initial Pressure (bar)	33.7	0.
TS Electrical Power (kW)	75.	0.
Initial Compressor Speed (rad/s)	1480.	0.
Compressor speed start decreasing (rad/s)	1480.	300.
Compressor speed stop decreasing (rad/s)	800.	350
Compressor speed start increasing (rad/s)	800.	1300.
Compressor speed stop increasing (rad/s)	0.	1350.
TS Helium Inlet Temperature (°C)	300.	All transient
Air Cooler Helium Outlet Temperature (°C)	175.	All transient
Valve F213 % Opening	100.	All transient

Table 4.3 – Initial and boundary conditions for the LOFA through compressor speed reduction

		Sigla di identificazione	Rev.	Distrib.	Pag.	di
ENEL	Centro Ricerche Bologna	FPN – P9LU – 015	0	R	44	132



Fig. 4.24 – Compressor Speed and TS Mass Flowrate



Fig. 4.25 - Inlet and Outlet Economizer Temperatures

		Sigla di identificazione	Rev.	Distrib.	Pag.	di
ENEL	Centro Ricerche Bologna	FPN – P9LU – 015	0	R	45	132



Fig. 4.26 – Heaters Zone Temperatures



Fig. 4.27 –Inlet and Outlet Test Section Pressure Temperatures

		Sigla di identificazione	Rev.	Distrib.	Pag.	di
ENEL	Centro Ricerche Bologna	FPN – P9LU – 015	0	R	46	132



Fig. 4.28 – Inlet and Outlet Air Cooler Temperatures





		Sigla di identificazione	Rev.	Distrib.	Pag.	di
ENEL	Centro Ricerche Bologna	FPN – P9LU – 015	0	R	47	132



Fig. 4.30 – Pin temperatures at 0.25 m and at 1,75 m



Fig. 4.31 - Main and Bypass Valves Opening





Fig. 4.32 – Loop and TS pressure Drops



Fig. 4.33 – Loop Pressures



4.4 LOCA at 34 bar

A first LOCA transient has been simulated starting with a loop pressure of about 34 bar, that is the pressure restored in the loop stabilizing the loop conditions after LOFA transients. The transient has been started imposing a 1 % break in the cold part of the loop. This small area has been selected after some sensitivity calculation that showed a very fast depressurization that occurred after the break opening. In the calculation the break has been supposed to remain opened for 50 s than closed again to avoid an excessive depressurization of the loop. In the experiment this depressurization could be reproduced by using the pressure control in the tank, the dynamic of the depressurization should be as much as possible similar to the calculated one. As in the previous transients, a fundamental point in the pre-test calculation is to guarantee that the maximum helium and pin cladding temperatures reached during the LOCA transient.

The LOCA transient will allow to investigate that behavior of the loop against a strong variation of the loop pressure. In order to acquire enough data for the characterization of the loop at the new lower pressure, after the closure of the break the calculation has been run with the initial electrical power and compressor speed before decreasing the supplied power to avoid excessive heating. The initial and boundary conditions of the transient are reported in Table 4.4.

The results of the calculation are reported in Figs. 4.34 to 4.44. Figure 4.34 shows the instantaneous increase of the break mass flowrate at the break opening that is limited at 0.226 kg/s by the critical conditions. During the 50 s of the break opening the loop pressure decreases down to 15 bar then goes up to 18 bar following the loop heating (Fig. 4.35). In the mean time loop and TS mass flowrates strongly decrease in agreement with the characteristic of the compressor (Fig. 4.43) and as a consequence the temperature in the hot part of the loop increases. The helium temperature reaches 486 °C after 1000 s from the beginning of the transient (Fig. 4.38) when the TS power is reduced. The margin respect to the limit of 530° C is sufficient and more relevant is the margin for the pin cladding temperature, 690 °C against the limit of 800 °C (Fig. 4.41).

Initial and Boundary Conditions	Value	Time (s)
Initial Pressure (bar)	33.7	0.
TS Electrical Power (kW)	75.	0.
Initial Compressor Speed (rad/s)	1480.	0.
Break Opening (m ²)	0.075 10 ⁻³	300.
Break Closure (m ²)	0.	350.
TS Electrical Power (kW)	36.	1300.
TS Helium Inlet Temperature (°C)	300.	All transient
Air Cooler Helium Outlet Temperature (°C)	75.	All transient
Valve F213 % Opening	100.	All transient
Initial Compressor Speed (rad/s) Break Opening (m ²) Break Closure (m ²) TS Electrical Power (kW) TS Helium Inlet Temperature (°C) Air Cooler Helium Outlet Temperature (°C) Valve F213 % Opening	75. 1480. 0.075 10 ⁻³ 0. 36. 300. 75. 100.	0. 0. 300. 350. 1300. All transient All transient All transient

Table 4.4 – Initial and boundary conditions for LOCA at 34 bar





Fig. 4.34 – Test Section, Loop and Break Mass Flowrate



. Fig.4.35 - Loop Pressures





Fig.4.36 – Inlet and Outlet Economizer Temperature



Fig. 4.37 - Heaters Zone Temperatures

		Sigla di identificazione	Rev.	Distrib.	Pag.	di
ENEL	Centro Ricerche Bologna	FPN – P9LU – 015	0	R	52	132



Fig. 4.38 – Inlet and Outlet TS Temperatures



Fig. 4.39 – Inlet and Outlet Air Cooler Temperatures





Fig. 4.40 – Inlet and Outlet Compressor Temperatures



Fig. 4.41 – Pin temperatures at 0.25 m and at 1,75 m

-		Sigla di identificazione	Rev.	Distrib.	Pag.	di
EV.	Centro Ricerche Bologna	FPN – P9LU – 015	0	R	54	132

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Fig. 4.42 – Main and Bypass Valves Opening



.Fig. 4.43 - Test Section, Main and Bypass Valves Mass Flowrates





Fig. 4.44 – Loop and TS pressure Drops



4.4 LOCA at 18 bar

A second LOCA transient has been simulated starting from 18 bar, the stable pressure attained by the loop after the previous LOCA. As in the previous case the transient has been started imposing a 1 % break in the cold part of the loop, for the transposition from the calculation to the experiment are still valid the comments reported in the description of the LOCA at 30 bar.

The break is supposed to remain opened for 50 s in order to have a relevant depressurization of the loop and, in the mean time, to avoid an excessive heating. For this reason after 1000s the power supplied by the test section has been switched off. The initial and boundary conditions of the transient are reported in Table 4.5.

The results of the calculation are reported in Figs. 4.45 to 4.55 and are very similar to the results commented in the previous subsection. The break mass flowrate at the break opening is now limited at 0.117 kg/s by the critical conditions (Fig. 4.45). During the 50 s of the break opening the loop pressure decreases down to 8.3 bar (Fig. 4.46), while the loop and TS mass flowrates strongly decrease (Fig. 4.54) thus provoking the increase of temperature in the loop. The helium temperature reaches 460 °C after 1000 s from the beginning of the transient (Fig. 4.49) when the TS power is reduced. The margin respect to the limit of 530° C is sufficient and more relevant is the margin for the pin cladding temperature, 640 °C against the limit of 800 °C (Fig. 4.52).

Initial and Boundary Conditions	Value	Time (s)
Initial Pressure (bar)	33.7	0.
TS Electrical Power (kW)	75.	0.
Initial Compressor Speed (rad/s)	1480.	0.
Break Opening (m ²)	0.075 10 ⁻³	300.
Break Closure (m ²)	0.	350
TS Electrical Power (kW)	36.	1300.
TS Helium Inlet Temperature (°C)	300.	All transient
Air Cooler Helium Outlet Temperature (°C)	75.	All transient
Valve F213 % Opening	100.	All transient
Tab 15 Initial and have dome	anditions for LOCA	at 21 han

Tab. 4.5 – Initial and boundary conditions for LOCA at 34 bar





Fig. 4.45 – Test Section, Loop and Break Mass Flowrate









Fig. 4.47 – Inlet and Outlet Economizer Temperature



Fig. 4.48 - Heaters Zone Temperatures

Æ	Centro Ricerche Bologna	Sigla di identificazione	Rev.	Distrib.	Pag.	di
		FPN – P9LU – 015	0	R	59	132

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Fig. 4.49 – Inlet and Outlet TS Temperatures



Fig. 4.50 – Inlet and Outlet Air Cooler Temperatures





Fig. 4.51 – Inlet and Outlet Compressor Temperatures



Fig. 4.52 – Pin temperatures at 0.25 m and at 1,75 m

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.Fig. 4.53 – Main and Bypass Valves Opening



.Fig. 4.54 - Test Section, Main and Bypass Valves Mass Flowrates





Fig. 4.55 – Loop and TS pressure Drops



5. References

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[4] "Relap5/Mod 3.3 Code Manual" Information Systems Laboratories, Inc., Document NUREG/CR-5535/

[5] P. Meloni and G. Dell'Orco, "Assessment of ATHENA Code Capability to Simulate Helium Cooled Systems for Fusion Reactors", Proc. of Ninth International Topical Meeting on Nuclear Reactor Thermal Hydraulics (NURETH-9), San Francisco, California, (1999)

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APPENDIX A: Input Deck

```
*
*
         HE-FUS3 Input Deck per RELAP5 Mod3.3
*
    _____
=Helium Loop
100 new transnt
101 run
110 helium
120 120010000 0. he *circuito helio*
* time steps
                       min mj re
201 5000. 1.e-7 0.01 3 100 5000 5000
*_____
* Extended variables
*_____
20800001 httemp 360300114 * test section pin 222 mm
20800002 httemp 360300113 * test section pin 222 mm
20800003 httemp 360300814 * test section pin 1776 mm
20800004 httemp 360300813 * test section pin 1776 mm
*_____
* Minor edits
*______
*
310 tempg 140010000 * tank
311 tempg 180020000 * inlet econom. cold side
312 tempg 210010000 * outlet econom. cold side
313 tempg 315040000 * outlet by-pass
314 tempg 250010000 * out E/3
315 tempg 270010000 * out E/2
316 tempg 300140000 * out E/3
317 tempg 320010000 * inlet TS
318 tempg 390020000 * inlet econom. hot side
319 tempg 420010000 * outlet econom. hot side
320 tempg 480010000 * outlet areotermo
321 tempg 120010000 * outlet compressore
322 mflowj 150000000 * portata totale
323 mflowj 175000000 * portata resistori
324 mflowj 172000000 * portata by-pass
325 cntrlvar 040 * salto pressione compressore
326 cntrlvar 041 * salto pressione TS
327 pmphead 600
328 pmpvel 600
```



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* * potenza risc 1 338 cntrlvar 011 339 cntrlvar 012 * potenza risc 2 340 cntrlvar 013 * potenza risc 3 341 cntrlvar 014 * potenza mantello 342 cntrlvar 015 * potenza tubi 343 cntrlvar 016 * potenza scambiata aerotermo 344 cntrlvar 017 * potenza scambiata bacchette * perdite termiche econimiz. 345 cntrlvar 031 * perdite termiche heaters 346 cntrlvar 032 * perdite termiche TS 347 cntrlvar 033 * perdite termiche cold part 348 cntrlvar 034 * perdite termiche totali 349 cntrlvar 030 350 p 140040000 351 p 365010000 352 p 480090000 * 360 cntrlvar 200 361 cntrlvar 201 362 cntrlvar 202 363 cntrlvar 203 364 cntrlvar 204 365 cntrlvar 205 366 cntrlvar 206 367 cntrlvar 207 368 cntrlvar 208 369 cntrlvar 209 370 cntrlvar 210* test section pin 222 mm371 cntrlvar 211* test section pin 1776 mm * test section pin 1776 mm 371 cntrlvar 211 *_____ * trips *_____ * * Pump trip for decay 501 time 0 ge null 0 1.e6 n * pump-trip * Pump regulation 510 time 0 ge null 0 50. 1 511 time 0 le null 0 99999. 1 610 510 and 511 n * regulation on * * Pressure regulation 515 time 0 ge null 0 1000. l * regulation on 601 -515 and -515 n *_____ * Main line motor-valves regulation 517 time 0 le null 0 99999. l *trip closure fv234 603 -517 and -517 n *trip opening fv234 516 time 0 ge null 0 99999. 1 *trip closure fv213 616 -517 and -517 n *trip opening fv213 *_____ *



* Compressor Cooling Regulation trough dummy motor-valve 530 time 0 ge null 0 0. 1 * trip activation water recycle 521 cntrlvar 056 ge cntrlvar 050 .001 n *trip valve closing 522 cntrlvar 056 le cntrlvar 050 -.001 n 604 522 and 530 n *trip valve opening *_____ * Regulation of hot part by-pass through motor-valve FV235 525 time 0 ge null 0 99999. n 526 time 0 le null 0 999999. n 625 525 and 526 n *trip valve opening 626 -526 and -526 n *trip valve closing *_____ 590 time 0 ge null 0 1200. 1 * end of transient * end of programm 600 590 * *_____ Hydraulic components *_____ _____ * Line P 1200000 ptubo pipe * partizioni 1200001 2 * sez.(m 2) elem. 1200101 0.002163 2 * lung.(m) elem. 1200301 0.5 2 * vol(m 3) elem. 1200401 0. 2 * azimut elem. 1200501 120. 2 * ang.vertic elem. 1200601 0. 2 * rugos(m) Didr(m) elem. 1200801 4.e-5 0.052 2 * Kdir Kinvr junct. 1200901 3. 3. 1 tlpvbfe elem. * 1201001 00000 2 * efvcahs junct. 1201101 001000 1 ebt P(Pa) T(K) state elem. 1201201 004 5.1e6 361.16 0.0 0. 0. 2 0:(m/s) 1:(kg/s) 1201300 1 initial conditions mliq mgas ! giunz. 1201301 0. .225 0. 1 *_____ * Dummy Valve for compressor cooling 2560000 bypvl2 valve sez.giu(m 2) Kdir Kinv efvcahs а da 2560101 120010000 257000000 4.0579e-3 0. 0. 000000



```
*
       condizioni iniziali
* (kg/s) mliq mgas !
2560201 1 0. 0.00 0.
* tipo valvola
2560300 mtrvlv
* open.trip clos.trip velocity initial pos.
2560301 604 521 .01
                                   0.
* normal.pos. CSUBVdir CSUBVinv
2560400 1. 1.

      1.

      2.354
      2.354

      4.62
      4.62

      6.16
      6.16

2560401 0.
2560402 0.1
2560403 0.2
25604040.36.166.1625604050.47.157.1525604060.57.9757.97525604070.68.6468.64625604080.79.2299.22925604090.89.8239.82325604100.910.37310.37325604111.14.514.5
2560404 0.3
*_____
2570000 closure branch
2570001 1 1
* sez(m 2) lung(m) vol(m 3) azim incli elev(m) rug(m) Didr(m) tlpvbfe
2570101 4.0579e-3 0.2 0. 0. -90. -0.2 4.e-5 0.072 00000
* ebt P(Pa) T(K)
2570200 004 4.8e6 343.16 0.0
* da a sez.giu(m 2) Kdir Kinv efvcahs
25711012570100004800000000.0.0.001000
* condizioni iniziali
*
      mliq mgas !
2571201 0. 0.06 0.
*_____
* Line P-Tank
*
1300000 jun2 sngljun
* da a sez.giun(m 2) Kf Kr efvcahs
1300101 120010000 140000000 0. 1. 0.5 001100
* (kg/s) mliq mgas !
1300201 1 0. .225 0.
            ------
*_____
                                _____
* Tank
*
1400000 vess pipe
* partizioni
1400001 5
* sez.(m 2) elemento
1400101 0.650 5
* lung.(m) elem.
1400301 0.923
                5
      vol(m 3) elem.
1400401 0.
                 5
      azimut elem.
1400501 0.
                5
* ang.vertic elem.
1400601 90. 5
* rugos(m) Didr(m) elem.
1400801 4.e-5 0.710 5
```



* Kdir Kinvr giunzione
1400901 0. 0. 4
* tlpvbfe elem. 5 1401001 00000 * efvcahs giunz. 1401101 001000 4 * ebt P(Pa) T(K) stato ? ? elem. 1401201 004 5.1e6 361.16 0.0 0.0. 5 0:(m/s) 1:(kg/s) * 1401300 1 * mliq mgas ! giunz. 1401301 0. .225 0. 4 *_____ _____ * Loop Pressure 1430000 prescomp tmdpvol sez(m 2) lung(m) vol(m 3) azim ang.vert elev(m) rug(m) Didr(m) * tlpvbfe 1430101 100. 1. 0. 0. 0. 0. 0. 0. 00000 * ebt 1430200 004 * ? P(Pa) T(K) 14302010.5.0e6361.0.0143020250.5.0e6361.0.0 1430203 200. 5.0e6 361. 0.0 1430204 500. 3.446e6 363. 0.0 1430205 1000. 3.446e6 363. 0.0 1430206 9999. 3.446e6 363. 0.0 *_____ * Pressurizer Valve * 1450000 prsvalv valve 1450000 prsvalv valve * da a sez.giu(m 2) Kdir Kinv efvcahs 14501011430000001400100000.0250.0.001000 * condizioni iniziali * (kg/s) mliq mgas ! 1450201 1 0. .0 0. * tipo valvola 1450300 trpvlv * apritrip 1450301 601 *_____ ------* Tank - Line D * 1500000 jun3 sngljun sez.giun(m 2) Kf Kr efvcahs * da a 1500101 140010000 160000000 0. 0.5 1. 001100 * (kg/s) mliq mgas ! 1500201 1 0. .225 0. *_____ * Line D 1600000 dtubo pipe * partizioni 1600001 9 * sez.(m 2) elemento 1600101 0.007371 5 7 1600102 0.001444



di

1600103 0.007371 9 elem. * lung.(m) 1600301 0.447 1 4 1600302 0.869 1600303 0.973 9 * vol(m 3) elem. 1600401 0. 9 azimut * elem. 1 1600501 180. 1600502 0. 4 1600503 270. 9 * ang.vertic elem. 1 1600601 0. 1600602 -90. 4 1600603 0. 9

 1000003 0.
 9

 *
 rugos(m)
 Didr(m) elem.

 1600801 4.e-5
 0.097
 5

 1600802 4.e-5
 0.043
 7

 1600803 4.e-5
 0.097
 9

 *
 Kdir
 Kinvr
 giunzione

 1600901 0.5
 0.5
 1

 1600902 0.5
 0.5
 5

 1600903 8.7
 8.7
 6

 1600904 0.
 0.
 8

 *
 tlpvbfe
 elem.

 * tlpvbfe elem. 1601001 00000 9 * efvcahs giunz. 1601101 001000 8 * ebt P(Pa) T(K) stato ? ? elem. 1601201 004 5.1e6 361.16 0.0 0.0. 9 * 0:(m/s) 1:(kg/s) 1601300 1 * mliq mgas ! giunz. 1601301 0. .225 0. 8 *_____ * By-pass of the Hot part of the loop *_____ * Line I 4990000 closure branch * 4990001 1 1 * sez(m 2) lung(m) vol(m 3) azim incli elev(m) rug(m) Didr(m) tlpvbfe 4990101 4.0579e-3 1.636 0. 0. -90. -1.636 4.e-5 0.072 00000 * ebt P(Pa) T(K) 4990200 004 5.1e6 361.16 0.0 * da a sez.giu(m 2) Kdir Kinv efvcahs

 4991101
 160010000
 499000000
 0.
 0.
 0.
 001000

 condizioni iniziali * * mliq mgas ! 4991201 0. 0.01 0. *_____ * Valve 235 * 5100000 bypvl2 valve sez.giu(m 2) Kdir Kinv efvcahs * da а 5100101 499010000 520000000 4.0579e-3 0. 0. 001000


```
*
      condizioni iniziali
*
      (kg/s) mliq mgas !
5100201 1 0. 0.01 0.
*
      tipo valvola
5100300 mtrvlv
      apritrip chiuditrip vel.cambio pos.iniz.
*
             626 .25
5100301 625
                                 0.0001
      pos.normaliz CSUBVdir CSUBVinv
*
5100400 1. 0.08
5100401 0.
                 Ο.
                         Ο.
                  9.965
                         9.965
5100402 0.08
5100403 0.11
                  15.06
                          15.06
5100404 0.16
                  21.17
                          21.17
5100405 0.3
                  25.55
                          25.55
5100406 0.4
                  37.45
                          37.45
5100407 0.47
                  50.67
                          50.67
5100408 0.5
                  55.06
                          55.06
5100409 0.58
                  70.68
                          70.68
5100410 0.6
                  77.79
                          77.79
                         105.68
5100411 0.7
                  105.68
                         140.20
5100412 0.8
                 140.20
5100413 0.9
                 179.33
                          179.33
                 224.
5100414 1.
                          224.
*_____
* Line I
5200000 itubo2 pipe
* partizioni
5200001 2
*
      sez.(m 2) elemento
5200101 4.0579e-3 2
*
      lung.(m)
               elem.
5200301 0.5
               2
*
      vol(m 3)
                elem.
5200401 0.
                2
*
      azimut
                elem.
5200501 0.
                2
*
      ang.vertic elem.
5200601 0.
               2
*
      rugos(m) Didr(m) elem.
5200801 4.e-5 0.072
                     2
*
      Kdir
              Kinvr
                      giunzione
            0.0
5200901 0.0
                      1
      tlpvbfe elem.
*
5201001 00000
                2
      efvcahs
                giunz.
5201101 001000
               1
      ebt P(Pa) T(K) stato ? ? elem.
5201201 004 4.9e6 400.16 0.0 0.0. 2
      0:(m/s) 1:(kg/s)
5201300 1
      mliq mgas ! giunz.
*
5201301 0. 0. 0.01 1
*_____
5210000 closure branch
          1
5210001 2
```



sez(m 2) lung(m) vol(m 3) azim incli elev(m) rug(m) Didr(m) tlpvbfe 5210101 4.0579e-3 0.2 0. 0. 0. 0. 4.e-5 0.072 00000 * ebt P(Pa) T(K) 5210200 004 4.9e6 400.16 0.0 sez.giu(m 2) Kdir Kinv efvcahs * da a 52111015200100005210000000.0.0.00100052121015210100004400000000.0.0.001000 condizioni iniziali * mliq mgas ! 5211201 0. 0.01 0. 5212201 0. 0.01 0. *_____ * Main Line Restart *_____ * Line D 1700000 Hltubo branch * tipo? (kg/s) 1700001 3 1 * sez(m 2) lung(m) vol(m 3) azim incli elev(m) rug(m) Didr(m) tlpvbfe 1700101 0.007371 2.902 0. 0. 90. 2.902 4.e-5 0.097 00000 * ebt P(Pa) T(K) 1700200 004 5.1e6 361.16 0.0 * da sez.giu(m 2) Kdir Kinv efvcahs a
 1701101
 160010000
 170000000
 0.
 1.5
 1.5
 001000
 1.5 1.5 001000 1.0 1.0 001000 1702101 170010000 173000000 0. 1703101 170010000 171000000 0. condizioni iniziali * * mliq mgas ! 1701201 0. .225 0. 1702201 0. .225 0. 1703201 0. 0. 0. *_____ * Economizer By-pass *_____ * Line I * 1710000 itubol pipe * partizioni 1710001 4 sez.(m 2) elemento * 1710101 0.007371 4 * lung.(m) elem. 1710301 0.6266 4 vol(m 3) elem. 1710401 0. 4 azimut elem. 1710501 90. 4 ang.vertic elem. 1710601 0. 4 rugos(m) Didr(m) elem. 1710801 4.e-5 0.097 4 * Kdir Kinvr giunzione 1710901 0.0 0.0 3 * tlpvbfe elem. 4 1711001 00000 efvcahs giunz. *



1711101 001000 3 * ebt P(Pa) T(K) stato ? ? elem. 1711201 004 5.1e6 361.16 0.0 0.0. 4 * 0:(m/s) 1:(kg/s) 1711300 1 * mliq mgas ! giunz. 1711301 0. 0. 3 _____ *____ _____ * Valvola Fv234 1720000 bypvl2 valve da a sez.giu(m 2) Kdir Kinv efvcahs * 1720101 171010000 315000000 4.0579e-3 0. 0. 001000 condizioni iniziali * * (kg/s) mliq mgas ! 1720201 1 0. 0. 0. * tipo valvola 1720300 srvvlv * control 1720301 156 * pos.normaliz CSUBVdir CSUBVinv 1720400 1. 0.08 1720401 0. 0. 0. 9.965 9.965 1720402 0.08 1720403 0.11 15.06 15.06 1720404 0.16 21.17 21.17 1720405 0.3 25.55 25.55 37.4537.4550.6750.67 1720406 0.4 1720407 0.47 55.06 55.06 70.68 70.68 1720408 0.5 1720409 0.58 1720410 0.6 77.79 77.79 1720411 0.7 105.68 105.68 140.20 179.33 179.33 1720412 0.8 1720413 0.9 1720414 1. 224. 224. *_____ * Mean Line Restart *_____ * Line D * 1730000 H2tubo pipe * partizioni 1730001 2 * sez.(m 2) elemento 1730101 0.007371 1 1730102 4.0579e-3 2 lung.(m) elem. 1730301 0.600 1 1730302 0.050 2 vol(m 3) elem. 1730401 0. 2 azimut elem. 1730501 360. 2 * ang.vertic elem. 1730601 0. 2 * rugos(m) Didr(m) elem. 1730801 4.e-5 0.097 1



17308024.e-50.072*KdirKinvr17309010.751.0*tlpvbfeelem. 2 giunzione 1 1731001 00000 2 * efvcahs gi 1731101 001000 1 giunz. * ebt P(Pa) T(K) stato ? ? elem. 1731201 004 5.0e6 361.16 0.0 0. 0. 2 * 0:(m/s) 1:(kg/s) 1731300 1 * mliq mgas ! giunz. 1731301 0. .225 0. 1 *_____ _____ * Valve Fv213 1750000 bypvll valve da a sez.giu(m 2) Kdir Kinv efvcah * 1750101 173010000 180000000 4.0579e-3 0. 0. 001000 condizioni iniziali * (kg/s) mliq mgas ! 1750201 1 0. 0.225 0. * tipo valvola 1750300 mtrvlv * apritrip chiuditrip vel.cambio pos.iniz. 1750301 516 616 .033333 1.0 * pos.normaliz CSUBVdir CSUBVinv 1750400 1. 0.08 1750401 0. 0. 0. 14.72 14.72 22.24 22.24 31.28 31.28 37.74 37.74 55.32 55.32 1750402 0.08 1750403 0.11 22.24 1750404 0.16 1750405 0.3 1750406 0.4 74.8574.8581.3381.33 1750407 0.47 1750408 0.5 104.4 104.4 114.9 114.9 156.1 156.1 207.1 207.1 264.9 264.9 1750409 0.58 1750410 0.6 1750411 0.7 1750412 0.8 1750413 0.9 1750414 1. 224. 224. *_____ * Line D * 1800000 H3tubo pipe * partizioni 1800001 2 * sez.(m 2) elemento 1800101 4.0579e-3 1 1800102 0.00737 2 lung.(m) elem. 1800301 0.050 1 1800302 0.600 2 vol(m 3) elem. 1800401 0. 2 1800401 J. * azimut elem. 1800501 360. 2 * ang.vertic elem.



1800601 0. 2 Didr(m) elem. * rugos(m) 18008014.e-50.07218008024.e-50.097 1 2 Kinvr * Kdir giunzione 1800901 1.0 0.75 1 * tlpvbfe elem. 1801001 00000 2 ک 1 * efvcahs giunz. 1801101 001000 * ebt P(Pa) T(K) stato ? ? 1801201 004 5.0e6 361.16 0.0 0.0. elem. 2 * 0:(m/s) 1:(kg/s) 1801300 1 * mliq mgas ! giunz. 1801301 0. .225 0. 1 *_____ _____ _____ * Line D - Economizer 1850000 ingserb sngljun * da sez.giun(m 2) Kf Kr a efvcahs 1850101 180010000 200000000 4.0579e-3 1.0 0.5 001100 * (kg/s) mliq mgas ! 1850201 1 0. .225 0. *_____ * Economizer shell side 2000000 econom1 pipe * partizioni 2000001 19 * sez.(m 2) elemento 2000101 0.0288 19 * lung.(m) elem. 2000301 0.263 19 * vol(m 3) elem. 2000401 0. 19 * azimut elem. 2000501 0. 19 * ang.vertic elem. 2000601 90. 19 rugos(m) Didr(m) elem. * 2000801 4.e-5 0.01818 19 Kinvr giunzione * Kdir 2000901 8. 8. 18 tlpvbfe elem. * 2001001 00000 19 efvcahs giunz. 2001101 001000 18 ebt P(Pa) T(K) stato ? ? elem. 2001201 004 5.0e6 345.16 0.0 0. 0. 1 2001202 004 5.0e6 360.16 0.0 0. 0. 2 2001203 004 5.0e6 375.16 0.0 0. 0. 3 2001204 004 5.0e6 390.16 0.0 0. 0. 4 2001205 004 5.0e6 405.16 0.0 0. 0. 5 2001206 004 5.0e6 420.16 0.0 0. 0. б 2001207 004 5.0e6 435.16 0.0 0. 0. 7 2001208 004 5.0e6 460.16 0.0 0. 0. 8 2001209 004 5.0e6 475.16 0.0 0. 0. 9 2001210 004 5.0e6 490.16 0.0 0. 0. 10

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2001211 2001212 2001213 2001214 2001215 2001216 2001217 2001218 2001219 * 2001300	004 5.0e6 004 5.0e6 0:(m/s) 1:	505.16 0.0 0. 520.16 0.0 0. 535.16 0.0 0. 560.16 0.0 0. 575.16 0.0 0. 590.16 0.0 0. 605.16 0.0 0. 605.16 0.0 0. 605.16 0.0 0. (kg/s)	0. 11 0. 12 0. 13 0. 14 0. 15 0. 16 0. 17 0. 18 0. 19					
* 2001301 * *	mliq mgas 0225	! giunz. 0. 18						
* Line f * 2100000 * 2100101 * 2100200 * 2101101 2102101 * * 2101201 2102201 *	eltubo b: tipo? (kg/s 2 1 sez(m 2) 1 0.007371 0 ebt P(Pa) 004 5.0e6 da a 200010000 2 210010000 2 condizion mliq mgas 0225 0225	ranch s) ung(m) vol(m 3) .626 0. T(K) 605.16 0.0 a sez.gi 210000000 0. 220000000 0. i iniziali ! 0.	azim incli 90. 0. u(m 2) Kdir 0.5 1.5	elev(m) rug 0. 4.e Kinv efvo 1. 0011 1.5 0010	g(m) D: 2-5 0 2ahs 100 000	idr(m) t .097 (lpvbf)0000	e
<pre>* Line F * 2200000 * 2200001 * 2200101 * 2200301 * 2200401 * 2200501 * 2200501 * 2200601 * 2200801 * 2200901 * 2201001 * 2201101 * 2201201 *</pre>	<pre>e2tubo pipe partizioni 2 sez.(m 2) 0.007371 lung.(m) 1.166 vol(m 3) 0. azimut 0. ang.vertic -90. rugos(m) 4.e-5 Kdir 0. tlpvbfe 00000 efvcahs 001000 ebt P(Pa) 004 5.0e6 0:(m/g) 1:</pre>	e elemento 2 elem. 2 elem. 2 elem. 2 Didr(m) elem. 0.097 2 Kinvr giunzio 0. 1 elem. 2 giunz. 1 T(K) stato ? 605.16 0.0 0.	ne ? elem. 0. 2					



```
2201300 1
* mliq mgas ! giunz.
2201301 0. .225 0. 1
*_____
* Valvola HV250
2250000 HV250 sngljun
* da a sez.giun(m 2) Kf Kr efvcahs
2250101 220010000 230000000 0.007371 5.35 5.35 001000
*
       (kg/s) mliq mgas !
2250201 1
          0. .225 0.
* _ _ _
         _____
* Line E
2300000 e3tubo branch
     tipo? (kg/s)
*
2300001 1 1
* sez(m 2) lung(m) vol(m 3) azim incli elev(m) rug(m) Didr(m) tlpvbfe
2300101 0.007371 2.084 0. 180. 0. 0. 4.e-5 0.097 00000
* ebt P(Pa) T(K)
2300200 004 5.0e6 605.16 0.0
      da
          a sez.giu(m 2) Kdir Kinv efvcahs
2301101 230010000 240000000 0.
                             2.0 1.5 001100
*2301101 220010000 230000000 0. 2.0 2.0 001000
      condizioni iniziali
*
      mliq mgas !
2301201 0. .225 0.
*2302201 0. 0.35 0.
*_____
* Heater E219/3
*
2400000 e219/3 pipe
* partizioni
2400001 14
*
      sez.(m 2) elemento
2400101 0.0572 1
2400102 0.0466
                14
       lung.(m) elem.
2400301 0.130
                1
2400302 0.16363
                12
2400303 0.150
                14
*
      vol(m 3) elem.
2400401 0.
                14
*
      azimut
               elem.
2400501 0.
                14
* ang.vertic elem.
2400601 90.
                14
      rugos(m) Didr(m) elem.

        2400801
        4.e-5
        0.0
        1

        2400802
        4.e-5
        0.066
        14

2400801 4.e 5
2400802 4.e-5 0.066 14
* Kdir Kinvr giunzione
2400901 0.0 0.0 1
12. 13
* tlpvbfe elem.
                14
2401001 00000
     efvcahs
                giunz.
```



2401101 001000 13 ebt P(Pa) T(K) stato ? ? * elem. 2401201 004 5.0e6 590.16 0.0 0. 0. 14 * 0:(m/s) 1:(kg/s) 2401300 1 * mliq mgas ! giunz. 2401301 0. .225 0. 13 *_____ * Line F 2500000 fltubo branch tipo? (kg/s) * 2500001 2 1 sez(m 2) lung(m) vol(m 3) azim incli elev(m) rug(m) Didr(m) tlpvbfe * 2500101 0.008012 0.528 0. 90. 0. 0. 4.e-5 0.101 00000 * ebt P(Pa) T(K) 2500200 004 5.0e6 590.16 0.0 * da sez.giu(m 2) Kdir Kinv efvcahs а 25011012400100002500000000.0.51.000110025021012500100002600000000.1.00.5001100 condizioni iniziali mliq mgas ! * 2501201 0. .225 0. 2502201 0. .225 0. *_____ * Heater 219/2 * 2600000 e219/2 pipe * partizioni 2600001 14 * sez.(m 2) elemento 2600101 0.0466 13 2600102 0.0572 14 * lung.(m) elem. 2600301 0.150 2 2600302 0.16363 13 2600303 0.130 14 * vol(m 3) elem. 2600401 0. 14 * azimut elem. 2600501 0. 14 ang.vertic elem. * 2600601 -90. 14 rugos(m) Didr(m) elem. * 2600801 4.e-5 0.066 13 2600802 4.e-5 0.0 14 Kdir Kinvr giunzione 2600901 12. 12. 12 2600902 0.0 0.0 13 tlpvbfe elem. 2601001 00000 14 efvcahs giunz. 2601101 001000 13 * ebt P(Pa) T(K) stato ? ? elem. 2601201 004 5.0e6 620.16 0.0 0. 0. 14 * 0:(m/s) 1:(kg/s) 2601300 1



*_____

```
* mliq mgas ! giunz.
2601301 0. .225 0. 13
*_____
* Line F parte
2700000 f2tubo branch
      tipo? (kg/s)
*
2700001 1 1
      sez(m 2) lung(m) vol(m 3) azim incli elev(m) rug(m) Didr(m) tlpvbfe
*
2700101 0.01205 0.933 0. 90. 0. 0. 4.e-5 0.124 00000
* ebt P(Pa) T(K)
2700200 004 5.0e6 620.16 0.0
      da a sez.giu(m 2) Kdir Kinv efvcahs
*
2701101 260010000 270000000 0. 2.5 3.0 001100
      condizioni iniziali
*
      mliq mgas !
2701201 0. .225 0.
*_____
* Valve HV252
2750000 HV252 sngljun
2750000 HV252 sngljun
* da a sez.(m 2) Kf Kr efvcahs
2750101 270010000 280000000 0.0 3.85 3.85 001000
* (kg/s) mliq mgas !
2750201 1 0. .225 0.
*_____
* Line F
2800000 f3tubo pipe
* partizioni
2800001 2
*
      sez.(m 2) elemento
2800101 0.01205 2
* lung.(m) elem.
2800301 1.115 2
*
      vol(m 3) elem.
2800401 0.
                2
* azimut elem.
2800501 0. 2
      ang.vertic elem.
*
2800601 90.
                2
      rugos(m) Didr(m) elem.
*

      2800801
      4.e-5
      0.124
      2

      *
      Kdir
      Kinvr
      giunzione

      2800901
      0.
      1

* tlpvbfe elem.
2801001 00000
                2
      efvcahs giunz.
1 001000 1
2801101 001000
      ebt P(Pa) T(K) stato ? ? elem.
*
2801201 004 5.0e6 620.16 0.0 0. 0. 2
      0:(m/s) 1:(kg/s)
*
2801300 1
       mliq mgas ! giunz.
*
2801301 0. .225 0. 1
```



```
* Line F
2900000 f4tubo branch
*
      tipo? (kg/s)
          1
2900001 2
      sez(m 2) lung(m) vol(m 3) azim incli elev(m) rug(m) Didr(m) tlpvbfe
*
2900101 0.01205 0.528 0. 90. 0. 0. 4.e-5 0.124 00000
      ebt P(Pa) T(K)
*
2900200 004 4.9e6 620.16 0.0
                       sez.giu(m 2) Kdir Kinv efvcahs
*
      da
             а
2901101 280010000 290000000 0.
                                  1.5
                                       1.5 001000
0.5 001100
2902101 290010000 30000000 0.
                                  1.0
       condizioni iniziali
* mliq mgas !
2901201 0. .225 0.
2902201 0.
          .225 0.
*_____
* Heater E219/1
3000000 e219/1 pipe
* partizioni
3000001 14
     sez.(m 2) elemento
3000101 0.0466 13
               14
3000102 0.0572
      lung.(m) elem.
3000301 0.150
              2
              13
3000302 0.16363
               14
3000303 0.130
              elem.
*
      vol(m 3)
3000401 0.
               14
*
     azimut
              elem.
3000501 0.
               14
* ang.vertic elem.
3000601 -90. 14
*
     rugos(m) Didr(m) elem.
3000801 4.e-5 0.066
                     13
3000802 4.e-5
              0.0
                      14
*
      Kdir
              Kinvr giunzione
3000901 12.
              12.
                      12
3000902 0.0
              0.0
                      13
      tlpvbfe elem.
*
3001001 00000
               14
*
      efvcahs
               giunz.
3001101 001000
               13
     ebt P(Pa) T(K) stato ? ? elem.
3001201 004 4.9e6 653.16 0.0 0. 0. 14
      0:(m/s) 1:(kg/s)
3001300 1
      mliq mgas ! giunz.
*
3001301 0. .225 0. 13
*_____
* Line G
3100000 gltubo branch
* tipo? (kg/s)
          1
3100001 3
```



sez(m 2) lung(m) vol(m 3) azim incli elev(m) rug(m) Didr(m) tlpvbfe 3100101 0.01168 1.01 0. 0. 0. 0. 4.e-5 0.122 00000 * ebt P(Pa) T(K) 3100200 004 4.9e6 653.16 0.0 sez.giu(m 2) Kdir Kinv efvcahs * da а 31011013000100003100000000.1.01.500110031021013100100003200000000.2.02.000100031031013150100003100100000.1.51.5001000 condizioni iniziali * mliq mgas !
 3101201
 0.
 .225
 0.

 3102201
 0.
 .225
 0.
 3103201 0. 0. 0. *_____ * Line I 3150000 itubo2 pipe * partizioni 3150001 4 * sez.(m 2) elemento 3150101 0.007371 4 * lung.(m) elem. 3150301 0.66625 4 * vol(m 3) elem. 3150401 0. 4 * azimut elem. 3150501 0. 4 * ang.vertic elem. 3150601 90. 4 * rugos(m) Didr(m) elem. 3150801 4.e-50.0974*KdirKinvrgiunzione3150901 0.00.03 * tlpvbfe elem. 3151001 00000 4 * efvcahs giunz. 3151101 001000 3 * ebt P(Pa) T(K) stato ? ? elem. 3151201 004 4.9e6 650.16 0.0 0.0.4 * 0:(m/s) 1:(kg/s) 3151300 1 * mliq mgas ! giunz. 3151301 0. 0. 3 *_____ * Line G 3200000 g2tubo pipe * partizioni 3200001 4 * sez.(m 2) elemento 3200101 0.01168 4 lung.(m) elem. * 3200301 1.115 2 3200302 1.027 4 * vol(m 3) elem. 3200401 0. 4 * azimut elem. 3200501 0. 2



```
3200502 0.
                4
* ang.vertic elem.
3200601 90. 2
                4
3200602 0.
3200602 0. 4

* rugos(m) Didr(m) elem.

3200801 4.e-5 0.122 4

* Kdir Kinvr giunzione

3200901 0. 0. 1

3200902 0.5 0.5 2

3200903 0. 0. 3

* tlpvbfe elem.

3201001 00000 4

* efvcahs giunz.

3201101 001000 3

* ebt P(Pa) T(K) state 2 2
* ebt P(Pa) T(K) stato ? ? elem.
3201201 004 4.9e6 650.16 0.0 0. 0. 4
* 0:(m/s) 1:(kg/s)
3201300 1
* mliq mgas ! giunz.
3201301 0. .225 0. 3
  _____
* Valve Fv230
3230000 Fv230 sngljun
* da a sez.giun(m 2) Kf Kr efvcahs
3230101 320010000 325000000 0.01168 4.31 4.31 001000
* (kg/s) mliq mgas !
3230201 1 0. .225 0.
*_____
* Line G
3250000 gltubo branch
* tipo? (kg/s)
3250001 1 1
* sez(m 2) lung(m) vol(m 3) azim incli elev(m) rug(m) Didr(m) tlpvbfe
3250101 0.01168 0.678 0. 270. 0. 0. 4.e-5 0.122 00000
*
      ebt P(Pa) T(K)
3250200 004 4.9e6 650.16 0.0
* da
            a sez.giu(m 2) Kdir Kinv efvcahs
3251101 325010000 330000000 0. 0.0 0.0 001000
* condizioni iniziali
*
      mliq mqas !
3251201 0. .225 0.
*3252201 0. 0.35 0.
*_____
* Test Section
3300000 test1 branch
* tipo? (kg/s)
3300001 2
           1
* sez(m 2) lung(m) vol(m 3) azim incli elev(m) rug(m) Didr(m) tlpvbfe
                      0. 270.0. 0. 4.e-5 0.0 00000
3300101 0.0042614 0.695
* ebt P(Pa) T(K)
3300200 004 4.9e6 650.16 0.0
            a sez.giu(m 2) Kdir Kinv efvcahs
* da
3301101 325010000 330000000 0. 0.0 0.0 001000
```



*3302101 330010000 340000000 0. 1. 1. 001100 2.0 2.0 001100 3302101 330010000 340000000 0. condizioni iniziali mliq mgas ! 3301201 0. .225 0. .225 0. 3302201 0. *_____ * Test Section 3400000 test2 pipe partizioni * 3400001 18 * sez.(m 2) elemento 3400101 0.00668 1 3400102 0.0031023 2 3400103 0.001762 3 3400104 0.0015514 18 lung.(m) elem. 3400301 0.105 1 3400302 0.326 2 3 4 3400303 0.155 3400304 0.14 3400305 0.20 8 3400306 0.2214 18 *heating rods (2.214 m) vol(m 3) elem. 18 3400401 0. * elem. azimut 3400501 0. 18 * ang.vertic elem. 3400601 -90. 18 * rugos(m) Didr(m) elem

 3400801
 4.e-5
 0.0566
 1
 *0.0

 3400802
 4.e-5
 0.0316
 2
 *0.0

 3400803
 4.e-5
 0.0198
 3
 *0.0

 3400804
 4.e-5
 0.01492
 18
 *0.0

 *
 Kdir
 Kipyr
 giupzione

 * Kdir Kinvr giunzione 3400901 0.0 0.0 2 3 3400902 0.1 0.1 3400903 0.0 0.0 0.0 0.1 o 17 7 3400904 0.1 34009040.10.134009050.00.0 * tlpvbfe elem. 3401001 00000 18 * efvcahs giunz. 3401101 001000 17 * ebt P(Pa) T(K) stato ? ? elem. 3401201 004 4.9e6 650.16 0.0 0. 0. 18 0:(m/s) 1:(kg/s) 3401300 1 * mliq mgas ! giunz. 3401301 0. .225 0. 17 *_____ * Test Section *3520000 test2 pipe * partizioni *3520001 3 * sez.(m 2) elemento



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```
*3520101 0.00376 1
*3520102 0.00719
                2
*3520103 0.0112
               3
*
              elem.
      lung.(m)
*3520301 0.0875 1
*3520302 0.127
              2
*3520303 0.485 3
* vol(m 3) elem.
*3520401 0. 3
               elem.
* azimut
*3520501 0. 3
* ang.vertic elem.
*3520601 -90. 3
* rugos(m) Didr(m) elem
*3520801 4.e-5 0.0342
*3520802 4.e-5 0.0563
                            1
*3520802 4.e-5 0.0563 2
*3520803 4.e-5 0.0758 3
* Kdir Kinvr giunzione
*3520901 0.0 0.0 2
* tlpvbfe elem.
*3521001 00000 3
* efvcahs giunz.
*3521101 001000 2
* ebt P(Pa) T(K) stato ? ? elem.
*3521201 004 4.9e6 650.16 0.0 0.0. 3
*
     0:(m/s) 1:(kg/s)
*3521300 1
*
     mliq mgas ! giunz.
*3521301 0. .225 0. 2
*_____
* Test Section
3520000 test2 branch
* tipo? (kg/s)
3520001 2 1
* sez(m 2) lung(m) vol(m 3) azim incli elev(m) rug(m) Didr(m) tlpvbfe
3520101 0.00954 0.6995 0. 270. -90. -0.6995 4.e-5 0.0
00000
*
      ebt P(Pa) T(K)
3520200 004 4.9e6 650.16 0.0
* da a sez.giu(m 2) Kdir Kinv efvcahs
3521101 340010000 352000000 0. 0.62 0.62 001100
3522101 352000000 360000000 0.
                                  0.65 0.65 001100
      condizioni iniziali
*
*
      mliq mgas !
3521201 0. .225 0.
3522201 0.
          .225 0.
*_____
* Test Section
3600000 test3 pipe
* partizioni
3600001 18
* sez.(m 2) elemento
3600101 0.0008344
               10
3600102 0.0013305
                 18
* lung.(m) elem.
```

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```
36003010.22141036003020.2014
3600303 0.14
                 15
                 16
17
3600304 0.155
3600305 0.326
               18
3600306 0.105
      vol(m 3) elem.
*
                   18
3600401 0.
                 ele
18
*
        azimut
                   elem.
3600501 0.
*
        ang.vertic elem.
3600601 90. 18
* rugos(m) Didr(m) elem
3600801 0. 0.0122 10
               0.0 18
3600802 0.
               Kinvr
                          giunzione
        Kdir
*
                         1
2
3600901 0.0
                  0.0
3600902 0.5
                   0.5
                            2 * 0.1
                                              0.1

    3600904 0.5
    0.5
    4
    * 0.1

    3600905 0.0
    0.0
    9

    3600906 0.5
    0.5
    10
    * 0.1

    3600907 0.0
    0.0
    17

    *
    tlpubfo
    -

3600903 0.0
                   0.0 3
                                               0.1
                                              0.1
* tlpvbfe elem.
3601001 00000
                   18
* efvcahs giunz.
3601101 001000 17
*
        ebt P(Pa) T(K) stato ? ? elem.
3601201 004 4.9e6 650.16 0.0 0.0. 18
*
        0:(m/s) 1:(kg/s)
3601300 1
* mliq mgas ! giunz.
3601301 0. .225 0. 17
*
*_____
* Test Section
* L=0.672 A=0.0013305m2, Didr=0.04116 m
3650000 test4 branch
*
       tipo? (kq/s)
3650001 2 1
       sez(m 2) lung(m) vol(m 3) azim incli elev(m) rug(m) Didr(m) tlpvbfe
*
3650101 0.0013305 0.672 0. 0. 90. 0.672 4.e-5 0.0 00000
       ebt P(Pa) T(K)
*
3650200 004 4.9e6 650.16 0.0
              a sez.giu(m 2) Kdir Kinv efvcahs
* da

      3651101
      360010000
      365000000
      0.
      0.0
      001000

      3652101
      365010000
      367000000
      0.
      0.5
      0.5
      001000
      * Allargamento

     condizioni iniziali
*
       mliq mgas !
3651201 0. .225 0.
3652201 0.
             .225 0.
*_____
* Test Section
3670000 test4 branch
* tipo? (kg/s)
3670001 1 1
```



sez(m 2) lung(m) vol(m 3) azim incli elev(m) rug(m) Didr(m) tlpvbfe 3670101 0.0042614 0.429 0. 0. 90. 0.429 4.e-5 0.07366 00000 * ebt P(Pa) T(K) 3670200 004 4.9e6 650.16 0.0 * da a sez.giu(m 2) Kdir Kinv efvcahs 3671101 367010000 37000000 0. 0.35 001000 * curva condizioni iniziali mliq mgas ! 3671201 0. .225 0. *_____ * Test Section * L=0.561 m, A=0.0042614 m2, Didr=0.07366 m 3700000 test5 branch * tipo? (kg/s) 3700001 1 1 * sez(m 2) lung(m) vol(m 3) azim incli elev(m) rug(m) Didr(m) tlpvbfe 3700101 0.0042614 0.561 0. 270. 0. 0. 4.e-5 0.0 00000 * ebt P(Pa) T(K) 3700200 004 4.9e6 650.16 0.0 da a sez.giu(m 2) Kdir Kinv efvcahs 37011013700100003800000000.70.7001000*37011013700100003800000000.450.35001000 condizioni iniziali * mliq mgas ! 3701201 0. .225 0. *_____ * Line A 3800000 atubo1 pipe * partizioni 3800001 2 * sez.(m 2) elemento 3800101 0.01168 2 * lung.(m) elem. 3800301 0.667 2 * vol(m 3) elem. 3800401 0. 2 * azimut elem. 3800501 270. 1 3800502 180. 2 ang.vertic elem. 3800601 0. 1 3800602 0. 2 rugos(m) Didr(m) elem

 3800801
 4.e-5
 0.122
 2

 *
 Kdir
 Kinvr
 giunzione

 3800901
 0.5
 0.5
 1

 tlpvbfe elem. 3801001 00000 2 efvcahs giunz. 3801101 001000 * ebt P(Pa) T(K) stato ? ? elem. 3801201 004 4.9e6 630.16 0.0 0.0.2 * 0:(m/s) 1:(kg/s)



3801300 1 * mliq mgas ! giunz. 3801301 0. .225 0. 1 *_____ _____ _____ * Valvola Fv231 3850000 Fv231 sngljun * da a sez.giun(m 2) Kf Kr efvcahs 3.81 3.81 001000 3850101 380010000 390000000 0. * (kg/s) mliq mgas ! 3850201 1 0. .225 0. *_____ * Line A 3900000 atubo2 pipe * partizioni 3900001 2 * sez.(m 2) elemento 3900101 0.01168 2 * lung.(m) elem. 3900301 0.510 2 * vol(m 3) elem. 3900401 0. 2 * azimut elem. 3900501 0. 2 * ang.vertic elem. 3900601 -90. 2 * rugos(m) Didr(m) elem 39008014.e-50.1222*KdirKinvrgiunzione39009010.50.51 * tlpvbfe elem. 3901001 00000 2 * efvcahs giunz. 3901101 001000 1 * ebt P(Pa) T(K) stato ? ? elem. 3901201 004 4.9e6 630.16 0.0 0.0. 2 * 0:(m/s) 1:(kg/s) 3901300 1 * mliq mgas ! giunz. 3901301 0. .225 0. 1 *_____ _____ * Line A - economizer * 3950000 inecon sngljun * da a sez.giun(m 2) Kf Kr efvcahs 1.0 0.5 001000 3950101 390010000 400000000 0. * (kg/s) mliq mgas ! 3950201 1 0. .225 0. *_____ * Economizer tubes side 4000000 econtub pipe * partizioni 4000001 23 * sez.(m 2, 4000101 0.05726 1 * sez.(m 2) elemento



4000103 0.02063 21 4000104 0.266 22 4000105 0.05726 23 lung.(m) elem. 4000301 0.196 1 2 4000302 0.060 4000303 0.263 21 22 4000304 0.075 4000305 0.460 23 vol(m 3) elem. * 4000401 0. 23 elem. * azimut 4000501 0. 23 * ang.vertic elem. 4000601 -90. 23 rugos(m) Didr(m) elem 4000801 4.e-5 0.0 2 21 4000802 4.e-5 0.0176 4000803 4.e-5 0.0 23 giunzione Kdir Kinvr 4000901 1. 0.5 1 4000902 0.5 1.0 2 4000903 0.0 0.0 20 4000904 1.0 21 0.5 22 4000905 0.5 1.0 tlpvbfe elem. 4001001 00000 23 * efvcahs giunz. 4001101 001000 22 * ebt P(Pa) T(K) stato ? ? elem. 4001201 004 4.9e6 630.16 0.0 0. 0. 1 4001202 004 4.9e6 610.16 0.0 0. 0. 2 0. 0. 4.9e6 595.16 0.0 4001203 004 3 0. 0. 4001204 004 4.9e6 570.16 0.0 4 4001205 004 4.9e6 520.16 0.0 0. 0. 5 4001206 004 4.9e6 510.16 0.0 0. 0. б 4001207 004 4.9e6 505.16 0.0 0. 0. 7 4001208 004 4.9e6 505.16 0.0 0. 0. 8 4001209 004 4.9e6 495.16 0.0 0. 0. 9 4001210 004 4.9e6 485.16 0.0 0. 0. 10 4001211 004 4.9e6 482.16 0.0 0. 0. 11 4001212 004 4.9e6 479.16 0.0 0. 0. 12 4001213 004 4.9e6 467.16 0.0 0. 0. 13 4001214 004 4.9e6 467.16 0.0 0. 0. 14 4.9e6 466.16 0.0 0. 0. 4001215 004 15 4.9e6 465.16 0.0 4001216 004 0. 0. 16 4.9e6 464.16 0.0 4001217 004 0. 0. 17 4.9e6 463.16 0.0 4001218 004 0. 0. 18 4001219 004 4.9e6 460.16 0.0 0. 0. 19 4001220 004 4.9e6 458.16 0.0 0. 0. 20 4001221 004 4.9e6 456.16 0.0 0. 0. 21 4001222 004 4.9e6 456.16 0.0 0. 0. 22 4001223 004 4.9e6 455.16 0.0 0. 0. 23 0:(m/s) 1:(kg/s) 4001300 1 mliq mgas ! giunz. 4001301 0. .225 Ο. 22 *_____



* Economizer - Line B 4100000 jun8 sngljun sez.giun(m 2) Kf Kr efvcahs * da a 4100101 400010000 420000000 0. 0.5 1.0 001100 * (kg/s) mliq mgas ! 4100201 1 0. .225 0. * Line B 4200000 btubol pipe * partizioni 4200001 4 sez.(m 2) elemento * 4200101 0.00737 1 3 4200102 0.00144 4200103 0.00737 4 * lung.(m) elem. 4200301 0.502 4 * vol(m 3) elem. 4200401 0. 4 * azimut elem. 4200501 0. 4 * ang.vertic elem. 4200601 -90. 4 * rugos(m) Didr(m) elem 4200801 4.e-5 0.043 4 * Kdir Kinvr giunzione 4200901 0.5 1.0 1 42009027.7.242009031.00.53 * tlpvbfe elem. 4201001 00000 4 * efvcahs giunz. 4201101 001000 3 * ebt P(Pa) T(K) stato ? ? elem. 4201201 004 4.9e6 455.16 0.0 0.0.4 * 0:(m/s) 1:(kg/s) 4201300 1 * mliq mgas ! giunz. 4201301 0. .225 0. 3 *____. _____ * Line B * 4300000 btubo2 branch * tipo? (kg/s) 4300001 2 1 * sez(m 2) lung(m) vol(m 3) azim incli elev(m) rug(m) Didr(m) tlpvbfe 4300101 0.00737 1.718 0. 0. -90. -1.718 4.e-5 0.097 00000 * ebt P(Pa) T(K) 4300200 004 4.9e6 455.16 0.0 a sez.giu(m 2) Kdir Kinv efvcahs da

 4301101
 420010000
 430000000
 0.0
 0.0
 001000

 43001000
 430000000
 0.0
 0.0
 0.0
 001000

 4302101 430010000 440000000 0. 6.5 6.5 001000 * condizioni iniziali mliq mgas ! 4301201 0. .225 0. 4302201 0. .225 0. *_____



```
* Line B
4400000 btubo3 pipe
*
      partizioni
4400001 2
*
      sez.(m 2) elemento
4400101 0.00737 2
* lung.(m) el
                elem.
4400301 1.31
               2
              elem.
*
      vol(m 3)
4400401 0.
                2
* azimut elem.
4400501 90. 2
*
      ang.vertic elem.
4400601 0.
               2
* rugos(m) Didr(m) elem
4400801 4.e-5 0.097 2
* Kdir Kinvr giunzione
4400901 0.0 0.0 1
*
      tlpvbfe elem.
               2
4401001 00000
* efvcahs giunz.
4401101 001000 1
* ebt P(Pa) T(K) stato ? ? elem.
4401201 004 4.9e6 455.16 0.0 0. 0. 2
*
      0:(m/s) 1:(kg/s)
4401300 1
* mliq mgas ! giunz.
4401301 0. .225 0. 1
*_____
*
4500000 jun9 sngljun
* da a
                        sez.giun(m 2) Kf Kr
                                             efvcahs
4500101 440010000 460000000 0. 1.0 0.5
                                            001100
* (kg/s) mliq mgas !
4500201 1 0. .225 0.
*_____
* Aircooler tubes side
*
4600000 aero pipe
* partizioni
4600001 13
*
      sez.(m 2) elemento
4600101 0.007371 1
4600102 0.005661 12
4600103 0.007371 13
*
      lung.(m) elem.
4600301 1.251
               1
4600302 1.000
               12
4600303 1.251
               13
* vol(m 3)
               elem.
4600401 0.
               13
* azimut
               elem.
             13
4600501 0.
*
      ang.vertic elem.
4600601 0.
          1
4600602 -90.
               12
4600603 0.
              13
  Dzx(m) elem
*
```



```
4600701 0.
                       1
4600702 -0.052 12
4600703 0. 13

      *
      rugos(m)
      Didr(m) elem

      4600801
      4.e-5
      0.097
      1

      4600802
      4.e-5
      0.018
      12

      4600803
      4.e-5
      0.097
      13

      *
      Kdir
      Kinvr
      giunzione

      4600901
      0.5
      1.0
      1

      4600902
      0.8
      0.8
      11

      4600903
      1.0
      0.5
      12

* tlpvbfe elem.
4601001 00000 13
* efvcahs giunz.
4601101 001000 12
* ebt P(Pa) T(K) stato ? ? elem.
4601201 004 4.9e6 455.16 0.0 0. 0. 13
          0:(m/s) 1:(kg/s)
*
4601300 1
* mliq mgas ! giunz.
4601301 0. .225 0. 12
*_____
*Aircooler - Line C
4700000 jun10 sngljun
4700000 junl0 sngljun
* da a sez.giun(m 2) Kf Kr
                                                                         efvcahs
4700101 460010000 480000000 0. 0.5 1.0 001100
* (kg/s) mliq mgas !
4700201 1 0. .225 0.
*_____
* Line C
*
4800000 ctubo3 pipe
* partizioni
4800001 9
* sez.(m 2) elemento
4800101 0.007371 5
4800102 0.002163
                           9
           lung.(m) elem.
*
                    5
4800301 0.47
4800302 0.275
                         9
*
          vol(m 3) elem.
4800401 0.
                         9
*
                        elem.
          azimut
4800501 90.
                        8
4800502 0.
                         9
* ang.vertic elem.
4800601 0.
                  9
* rugos(m) Didr(m) elem
4800801 4.e-5 0.097 5
4800802 4.e-5 0.052 9
         Kdir Kinvr giunzione
4800901 0.5
                              5
                    1.0

      4800902 50.5
      50.5
      6

      4800903 3.
      3.
      7

      4800904 0.5
      0.5
      8

                                          *vlv FV 10
                                          *filtro
*
```



* tlpvbfe elem. 9 4801001 00000 * efvcahs giu: 4801101 001000 8 giunz. * ebt P(Pa) T(K) stato ? ? elem. 4801201 004 4.9e6 343.16 0.0 0.0.9 * 0:(m/s) 1:(kg/s) 4801300 1 * mliq mgas ! giunz. 4801301 0. .225 0. 8 *_____ * Compressor 6000000 compres pump sez(m 2) lung(m) vol(m 3) azim inclin elev(m) tlpvbfe * 6000101 0. 0.2 2.e-3 0. 90. 0.2 0000000 * da sez(m 2) Kdir Kinv efvcahs 6000108 480010000 .001 1. 1. 0000000 * a sez(m 2) Kdir Kinv efvcahs 6000109 12000000 .001 1. 1. 0000000 ebt P(Pa) T(K) 6000200 004 4.9e6 358.16 0.0 condizioni iniziali ingresso * (kg/s) mliq mgas ! 6000201 1 0. .225 0. condizioni iniziali uscita (kg/s) mliq mgas ! 6000202 1 0. .225 0. * dati sper monofasico ! torque w trip retromarcia 6000301 0 -1 -3 -1 0 501 0 w(rad/s) wi/w Vi'(m 3/s) head(m) torque(Nm) Inerzia(kg*m 2) * *6000302 1361.0.9760.038813896.2528.0000.0016000302 1361.1.00.03063634.09.50.001 * ro(kg/m 3) (Nm) TF2 TF0 TF1 TF3 tutti in (Nm) *6000303 6.75 0. 0. 0. 0. 0. 0. 0. 0. 0. 6000303 3.17 Ο. * ______ * head curves for new rotor (after 25/2/99) * 6001100 1 1 h/a 2 * v/a 6001101 0. 2.0062 6001102 0.1 1.8885 6001103 0.2 1.7789 6001104 0.3 1.6755 6001105 0.4 1.5764 6001106 0.5 1.4797 6001107 0.6 1.3833 6001108 0.7 1.2853 6001109 0.8 1.1838 6001110 0.9 1.0769 6001111 1. 1. 6001200 1 2 a/v h/v 2 * 0.1 6001201 0. 0.2 6001202 Ο. 0.3 6001203 Ο.



6001204 6001205 6001206 6001207 6001208 6001209 6001210 6001211	0.4 0.5 0.6 0.7 0.8 0.9 0.937 1.0	0.0666 0.1288 0.2209 0.3485 0.5172 0.7328 0.8255
* * *	(v/a)	
6001300 6001301 6001302	1 3 -1. 0.	2.0062 2.0062
* *	(a/v)	
* 6001400 6001401 6001402	1 4 -1. 0.	0.1 0.1
*		(v/a)
* 6001500 6001501 6001502	1 5 0. 1.	2.0062 2.0062
*		(a/v)
6001600 6001601 6001602	1 6 0. 1.	.1 .1
*		(v/a)
6001700 6001701 6001702 *	1 7 -1. 0.	2.0062 2.0062
*		(a/v)
6001800 6001801 6001802 *	1 8 -1. 0.	0.1 0.1
* * *	torque	curves dopo 25/2/99
* 6001900 * 6001901 6001902 6001903 6001904 6001905 6001906	2 1 v/a 0.1 0.2 0.3 0.4 0.5	b/a 2 1.5294 1.4494 1.3759 1.3091 1.2487 1.1950
6001907 6001908	0.6	1.1478 1.1071



6001909 6001910 6001911 6001912 *	0.8 0.9 0.937 1.	1.0731 1.0455 1.0370 1.	
* 6002000 *	2 2	h/w 2	
6002001 6002002 6002003 6002004 6002005 6002006 6002007 6002008 6002009 6002010 6002011 6002012 *	0. 0.1 0.2 0.3 0.4 0.5 0.6 0.7 0.8 0.9 0.937 1.0	0. 0. 0.1225 0.2028 0.2899 0.3826 0.4798 0.5812 0.6861 0.7942 0.8349 1.	
*		(v/a)	
^ 6002100 6002101 6002102 *	2 3 -1. 0.	1.5294 1.5294	
*		(a/v)	
* 6002200 6002201 6002202 *	2 4 -1. 0.	0.0 0.0	
6002300 6002301 6002302 *	2 5 0. 1.	1.5294 1.5294	
6002400 6002401 6002402 *	2 6 0. 1.	0.0 0.0	
6002500 6002501 6002502 *	2 7 -1. 0.	1.5294 1.5294	
6002600 6002601 6002602 *	2 8 -1. 0.	0.0 0.0	
* Compre	essor Re	gulation on massflo	wrate
6006100 * 6006101	610 c search 0.	ntrlvar 100 N? w(rad/s) 0.0	
6006102 * * Compre	2000. essor Re	2000.0 gulation on	
* *6006100	0 610		



*

time w(rad/s) 0. *6006101 1361. 300. 1361. *6006102 1257. *6006103 350. 1257. *6006104 400. 1047. 450. *6006105 500. 1047. *6006106 *_____ Heat Structures *_____ * Heaters E219/3 * 12401000 13 15 2 1 0. 12401100 0 2 12401101 7.5e-04 2 12401102 5.0e-04 12 12401103 5.0e-04 14 12401201 3 12 12401202 1 14 12401301 1. 14 12401400 0 12401401 800. 15 12401501 0 0 0 0 0. 13 12401601 240020000 10000 1 1 9.8181 11 12401602 240130000 10000 1 1 9.0 13 12401701 101 0.0909 0. 0. 11 12401702 0 0. 0. 0. 13 12401901 1.67e-2 15. 15. 0. 0. 0. 0. 1. 13 * *_____ * Heaters E219/2 * 12601000 13 15 2 1 0. 12601100 0 2 12601101 7.5e-04 2 12601102 5.0e-04 12 12601103 5.0e-04 14 12601201 3 12 12601202 1 14 12601301 1. 14 12601400 0 12601401 835. 15 12601501 0 0 0 0 0. 13 12601601 260010000 10000 1 1 9.0 2 12601602 260030000 10000 1 1 9.8181 13 12601701 0 0. 0. 0. 2 12601702 102 0.0909 0. 0. 13 12601901 1.67e-2 15. 15. 0. 0. 0. 0. 1. 13 *_____ * Heaters E219/1 13001000 13 15 2 1 0. 13001100 0 2 13001101 7.5e-04 2 13001102 5.0e-04 12



13001103 5.0e-04 14 13001201 3 12 13001202 1 14 13001301 1. 14 13001400 0 13001401 870. 15 13001501 0 0 0 0 0. 13 13001601 300010000 10000 1 1 9.0 2 13001602 300030000 10000 1 1 9.8181 13 13001701 0 0. 0. 0. 2 13001702 103 0.0909 0. 0. 13 13001901 1.67e-2 15. 15. 0. 0. 0. 0. 1. 13 _____ * Economizer tubes 1/2" 14001000 19 9 2 1 0.00905 14001100 0 1 14001101 8 0.01065 14001201 1 8 14001301 0. 8 14001400 -1 14001501 400210000 -10000 1 1 19.21 19 14001601 200010000 10000 1 1 19.21 19 14001701 0 0. 0. 0. 19 14001801 0. 15. 15. 0. 0. 0. 0. 1. 19 14001901 5.0e-3 15. 15. 0. 0. 0. 0. 1. 19 * 1.65e-3 *_____ * Economizer tubes 3/8" 14002000 19 9 2 1 0.007 14002100 0 1 14002101 8 0.008 14002201 1 8 14002301 0. 8 14002400 -1



14002404 14002405 14002406 14002407 14002408 14002409 14002410 14002411 14002412 14002413 14002414 14002415 14002416 14002417 14002418 14002419 14002501 14002501	507. 507. 507. 507. 507. 507. 507. 507.
14002701	$\begin{array}{cccccccccccccccccccccccccccccccccccc$
14002901 *	5.0e-3 15. 15. 0. 0. 0. 0. 1. 19 * 1.65e-3
* * Line D	External Wall
* ттпе ь	EXCELLAT MAIL
11201000	2 9 2 1 0.02609
11201100	0 2
11201101	1.95e-3 1
11201102	1.95e-3 2
11201103	0.01 8
11201201	1 2
11201202	2 8
11201301	0.8
11201400	0
11201401	433. 3
11201402	408. 4 202 E
11201403	383. D 250 6
11201404	333 7
11201406	308 8
11201407	295 9
11201501	120010000 10000 1 1 0.5 2
11201601	-200 0 4300 1 0.5 2
11201701	0 0. 0. 0. 2
11201801	0. 15. 15. 0. 0. 0. 0. 1. 2
11201901	0. 15. 15. 0. 0. 0. 0. 1. 2
*	
*	
* Vessel *	External Wall
11401000	5 16 2 1 0.455
11401100	0 2
11401101	0.009 5
11401104	0.01 15
11401201	1 5
11401202	2 15
11401301	0. 15
11401400	0.
11401401	431. 6



11401402 416. 7 11401403 401. 8 11401404 386. 9 11401405 371. 10 11401406 356. 11 11401407 341. 12 11401408 326. 13 11401409 311. 14 11401410 300. 15 11401411 290. 16 11401501 140010000 10000 1 1 0.923 5 11401601 -200 0 4300 1 0.923 5 11401701 0 0. 0. 0. 5 11401801 0. 15. 15. 0. 0. 0. 0. 1. 5 11401901 0. 15. 15. 0. 0. 0. 0. 1. 5 *_____ * Line D External Wall 11601000 9 9 2 1 0.0484 11601100 0 2 11601101 0.00428 1 11601102 0.00428 2 11601103 0.01 8 11601201 1 2 11601202 2 8 11601301 0. 8 11601400 0 11601401 432. 3 11601402 408. 4 11601403 383. 5 11601404 358. 6 11601405 333. 7 11601406 308. 8 11601407 295. 9 11601501 160010000 10000 1 1 0.8799 9 11601601 -200 0 4300 1 0.8799 9 11601701 0 0. 0. 0. 9 11601801 0. 15. 15. 0. 0. 0. 0. 1. 9 11601901 0. 15. 15. 0. 0. 0. 0. 1. 9 *_____ _____ * Line D External Wall * 11701000 1 9 2 1 0.0484 11701100 0 2 11701101 0.00428 2 11701102 0.01 8 11701201 1 2 11701202 2 8 11701301 0. 8 11701400 0 11701401 431. 3 11701402 408. 4 11701403 383. 5 11701404 358. 6 11701405 333. 7 11701406 308. 8 11701407 295. 9



11701501 170010000 0 1 1 2.902 1 11701601 -200 0 4300 1 2.902 1 11701701 0 0. 0. 0. 1 11701801 0. 15. 15. 0. 0. 0. 0. 1. 1 11701901 0. 15. 15. 0. 0. 0. 0. 1. 1 *_____ * Line I External Wall 11711000 4 9 2 1 0.0484 11711100 0 2 11711101 0.00428 2 11711102 0.01 8 11711201 1 2 11711202 2 8 11711301 0. 8 11711400 0 11711401 420. 3 11711402 408. 4 11711403 383. 5 11711404 358. 6 11711405 333. 7 11711406 308. 8 11711407 295. 9 11711501 171010000 0 1 1 0.6266 4 11711601 -200 0 4302 1 0.6266 4 11711701 0 0. 0. 0. 4 11711801 0. 15. 15. 0. 0. 0. 0. 1. 4 $11711901 \ 0. \ 15. \ 15. \ 0. \ 0. \ 0. \ 1. \ 4$ *_____ * Line I External Wall * 13151000 4 9 2 1 0.0484 13151100 0 2 13151101 0.00428 2 13151102 0.01 8 13151201 1 2 13151202 2 8 13151301 0. 8 13151400 0 13151401 423. 3 13151402 408. 4 13151403 383. 5 13151404 358. 6 13151405 333. 7 13151406 308. 8 13151407 295. 9 13151501 315010000 0 1 1 0.66625 4 13151601 -200 0 4300 1 0.66625 4 13151701 0 0. 0. 0. 4 13151801 0. 15. 15. 0. 0. 0. 0. 1. 4 $13151901 \ 0. \ 15. \ 15. \ 0. \ 0. \ 0. \ 1. \ 4$ *_____ * Line D External Wall 11731000 1 9 2 1 0.0484 11731100 0 2



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11731101 0.00428 2 11731102 0.01 8 11731201 1 2 11731202 2 8 11731301 0. 8 11731400 0 11731401 431. 3 11731402 408. 4 11731403 383. 5 11731404 358. 6 11731405 333. 7 11731406 308. 8 11731407 295. 9 11731501 173010000 10000 1 1 0.600 1 11731601 -200 0 4300 1 0.600 1 11731701 0 0. 0. 0. 1 $11731801 \ 0. \ 15. \ 15. \ 0. \ 0. \ 0. \ 1. \ 1$ 11731901 0. 15. 15. 0. 0. 0. 0. 1. 1 *_____ * Line D External Wall * 11801000 1 9 2 1 0.0484 11801100 0 2 11801101 0.00428 2 11801102 0.01 8 11801201 1 2 11801202 2 8 11801301 0. 8 11801400 0 11801401 421. 3 11801402 408. 4 11801403 383. 5 11801404 358. 6 11801405 333. 7 11801406 308. 8 11801407 295. 9 11801501 180020000 10000 1 1 0.600 1 11801601 -200 0 4300 1 0.600 1 11801701 0 0. 0. 0. 1 11801801 0. 15. 15. 0. 0. 0. 0. 1. 1 11801901 0. 15. 15. 0. 0. 0. 0. 1. 1 *_____ * Economizer External Wall * 12001000 19 16 2 1 0.135 12001100 0 2 12001101 4.0e-3 5 12001102 0.016 15 12001201 1 5 12001202 4 15 12001301 0. 15 12001400 0 12001401 660. 6 12001402 622. 7 12001403 584. 8 12001404 546. 9 12001405 506. 10



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12001406 470. 11 12001407 432. 12 12001408 394. 13 12001409 356. 14 12001410 318. 15 12001411 295. 16 12001501 200010000 10000 1 1 0.263 19 12001601 -200 0 4303 1 0.263 19 12001701 0 0. 0. 0. 19 12001801 0.001 15. 15. 0. 0. 0. 0. 1. 19 12001901 0. 15. 15. 0. 0. 0. 0. 1. 19 *_____ * Line E External Wall 12101000 1 13 2 1 0.04843 12101100 0 2 12101101 0.00428 2 12101102 0.016 12 12101201 1 2 12101202 4 12 12101301 0. 12 12101400 0 12101401 900. 3 12101402 838. 4 12101403 776. 5 12101404 714. 6 12101405 652. 7 12101406 590. 8 12101407 528. 9 12101408 466. 10 12101409 404. 11 12101410 342. 12 12101411 300. 13 12101501 210010000 0 1 1 0.626 1 12101601 -200 0 4300 1 0.626 1 12101701 0 0. 0. 0. 1 12101801 0. 15. 15. 0. 0. 0. 0. 1. 1 12101901 0.0 15. 15. 0. 0. 0. 0. 1. 1 *_____ * Line E External Wall * 12201000 2 13 2 1 0.04843 12201100 0 2 12201101 0.00428 2 12201102 0.016 12 12201201 1 2 12201202 4 12 12201301 0. 12 12201400 0 12201401 900. 3 12201402 838. 4 12201403 776. 5 12201404 714. 6 12201405 652. 7 12201406 590. 8 12201407 528. 9 12201408 466. 10



12201409 404. 11 12201410 342. 12 12201411 300. 13 12201501 220010000 10000 1 1 1.166 2 12201601 -200 0 4300 1 1.166 2 12201701 0 0. 0. 0. 2 12201801 0. 15. 15. 0. 0. 0. 0. 1. 2 12201901 0. 15. 15. 0. 0. 0. 0. 1. 2 *_____ * Line E External Wall 12301000 1 13 2 1 0.04843 12301100 0 2 12301101 0.00428 2 12301102 0.016 12 12301201 1 2 12301202 4 12 12301301 0. 12 12301400 0 12301401 900. 3 12301402 838. 4 12301403 776. 5 12301404 714. 6 12301405 652. 7 12301406 590. 8 12301407 528. 9 12301408 466. 10 12301409 404. 11 12301410 342. 12 12301411 300. 13 12301501 230010000 0 1 1 2.084 1 12301601 -200 0 4300 1 2.084 1 12301701 0 0. 0. 0. 1 12301801 0. 15. 15. 0. 0. 0. 0. 1. 1 12301901 0. 15. 15. 0. 0. 0. 0. 1. 1 *_____ * Heater 219/3 External Wall * 12402000 14 15 2 1 0.135 12402100 0 2 12402101 5.0e-3 4 12402102 0.016 14 12402201 1 2 12402202 4 14 12402301 0. 14 12402400 0 12402401 930. 5 12402402 865. 6 12402403 800. 7 12402404 735. 8 12402405 670. 9 12402406 605. 10 12402407 540. 11 12402408 475. 12 12402409 410. 13 12402410 345. 14 12402411 300. 15







12801410 349. 12 12801411 305. 13 12801501 280010000 10000 1 1 1.115 2 12801601 -200 0 4300 1 1.115 2 12801701 0 0. 0. 0. 2 12801801 0. 15. 15. 0. 0. 0. 0. 1. 2 12801901 0. 15. 15. 0. 0. 0. 0. 1. 2 *_____ * Line F External Wall 12901000 1 13 2 1 0.06194 12901100 0 2 12901101 4.28e-3 2 12901102 0.016 12 12901201 1 2 12901202 4 12 12901301 0. 12 12901400 0 12901401 970. 3 12901402 901. 4 12901403 832. 5 12901404 763. 6 12901405 694. 7 12901406 625. 8 12901407 556. 9 12901408 487. 10 12901409 418. 11 12901410 349. 12 12901411 305. 13 12901501 290010000 0 1 1 0.528 1 12901601 -200 0 4300 1 0.528 1 12901701 0 0. 0. 0. 1 12901801 0. 15. 15. 0. 0. 0. 0. 1. 1 12901901 0. 15. 15. 0. 0. 0. 0. 1. 1 *_____ * Heater 219/1 External Wall * 13002000 14 15 2 1 0.135 13002100 0 2 13002101 5.0e-3 4 13002102 0.016 14 13002201 1 2 13002202 4 14 13002301 0. 14 13002400 0 13002401 1010. 5 13002402 937. 6 13002403 864. 7 13002404 791. 8 13002405 718. 9 13002406 645. 10 13002407 572. 11 13002408 499. 12 13002409 426. 13 13002410 353. 14 13002411 315. 15 13002501 300010000 10000 1 1 0.150 2



```
13002502 300030000 10000 1 1 0.16363 13
13002503 300140000 10000 1 1 0.130
                                   14
13002601 -200 0 4301 1 0.150
                             2
13002602 -200 0 4301 1 0.16363 13
13002603 -200 0 4301 1 0.130
                             14
13002701 0 0. 0. 0. 14
13002801 0.001 15. 15. 0. 0. 0. 0. 1. 14
13002901 0. 15. 15. 0. 0. 0. 0. 1. 14
*___
    _____
* Line G External Wall
13101000 1 13 2 1 0.06098
13101100 0 2
13101101 4.76e-3 2
13101102 0.016
               12
13101201 1 2
13101202 5 12
13101301 0. 12
13101400 0
13101401 1010. 3
13101402 937. 4
13101403 864. 5
13101404 791. 6
13101405 718. 7
13101406 645. 8
13101407 572. 9
13101408 499. 10
13101409 426. 11
13101410 353. 12
13101411 315. 13
13101501 310010000 0 1 1 1.01 1
13101601 -200 0 4300 1 1.01
                             1
13101701 0 0. 0. 0. 1
13101801 0. 15. 15. 0. 0. 0. 0. 1. 1
13101901 0. 15. 15. 0. 0. 0. 0. 1. 1
*_____
* Line G External Wall
*
13201000 4 13 2 1 0.06098
13201100 0 2
13201101 4.76e-3 2
13201102 0.016
                 12
13201201 1 2
13201202 5 12
13201301 0. 12
13201400 0
13201401 1010. 3
13201402 937. 4
13201403 864. 5
13201404 791. 6
13201405 718. 7
13201406 645. 8
13201407 572. 9
13201408 499. 10
13201409 426. 11
13201410 353. 12
13201411 315. 13
```


13201501 320010000 10000 1 1 1.071 4 13201601 -200 0 4300 1 1.071 4 13201701 0 0. 0. 0. 4 13201801 0. 15. 15. 0. 0. 0. 0. 1. 4 13201901 0. 15. 15. 0. 0. 0. 0. 1. 4 *_____ * Line G External Wall 13251000 1 13 2 1 0.06097 13251100 0 2 13251101 4.76e-3 2 13251102 0.016 12 13251201 1 2 13251202 5 12 13251301 0. 12 13251400 0 13251401 1010. 3 13251402 937. 4 13251403 864. 5 13251404 791. 6 13251405 718. 7 13251406 645. 8 13251407 572. 9 13251408 499. 10 13251409 426. 11 13251410 353. 12 13251411 315. 13 13251501 325010000 0 1 1 0.678 1 13251601 -200 0 4300 1 0.678 1 13251701 0 0. 0. 0. 1 13251801 0. 15. 15. 0. 0. 0. 0. 1. 1 13251901 0. 15. 15. 0. 0. 0. 0. 1. 1 *_____ * Test Section External Wall * 13301000 1 13 2 1 0.03683 13301100 0 2 13301101 3.81e-3 2 13301102 0.016 12 13301201 1 2 13301202 5 12 13301301 0. 12 13301400 0 13301401 1010. 3 13301402 937. 4 13301403 864. 5 13301404 791. 6 13301405 718. 7 13301406 645. 8 13301407 572. 9 13301408 499. 10 13301409 426. 11 13301410 353. 12 13301411 315. 13 13301501 330010000 0 1 1 0.695 1 13301601 -200 0 4300 1 0.695 1 13301701 0 0. 0. 0. 1



```
13301801 0. 15. 15. 0. 0. 0. 0. 1. 1
13301901 0. 15. 15. 0. 0. 0. 0. 1. 1
*_____
* Test Section External Wall
13401000 2 15 2 1 0.05165
13401100 0 2
13401101 4.75e-3 4
13401102 0.016
                 14
13401201 1 4
13401202 5 14
13401301 0. 14
13401400 0
13401401 1010. 3
13401402 937. 4
13401403 864. 5
13401404 791. 6
13401405 718. 7
13401406 645. 8
13401407 572. 9
13401408 499. 10
13401409 426. 11
13401410 353. 12
13401411 315. 13
13401412 315. 15
134015013400100000110.1051134015023400200000110.3262
13401601 -200 0 4300 1 0.105 1
13401602 -200 0 4300 1 0.326 2
13401701 0 0. 0. 0. 2
13401801 0. 15. 15. 0. 0. 0. 0. 1. 2
13401901 0. 15. 15. 0. 0. 0. 0. 1. 2
*_____
* Test Section External Wall
*
13402000 1 19 2 1 0.03326
13402100 0 2
13402101 4.673e-3 8
13402102 0.016
                18
13402201 1 8
13402202 5 18
13402301 0. 18
13402400 0
13402401 1010. 3
13402402 937. 4
13402403 864. 5
13402404 791. 6
13402405 718. 7
13402406 645. 8
13402407 572. 9
13402408 499. 10
13402409 426. 11
13402410 353. 12
13402411 315. 13
13402412 315. 19
13402501 340010000
                    0 1 1 0.155 1
13402601 -200 0 4300 1 0.155 1
```



13402701 0 0. 0. 0. 1 13402801 0. 15. 15. 0. 0. 0. 0. 1. 1 13402901 0. 15. 15. 0. 0. 0. 0. 1. 1 *_____ * Test Section External Wall 13403000 15 14 2 1 0.03683 13403100 0 2 13403101 3.666e-3 3 13403102 0.016 13 13403201 1 3 13403202 5 13 13403301 0. 13 13403400 0 13403401 1010. 3 13403402 937. 4 13403403 864. 5 13403404 791. 6 13403405 718. 7 13403406 645. 8 13403407 572. 9 13403408 499. 10 13403409 426. 11 13403410 353. 12 13403411 315. 13 13403412 315. 14 13403501 340010000 1 1 0.140 1 0 13403502 340020000 10000 1 1 0.200 5 13403503 340060000 10000 1 1 0.2214 15 13403601 -200 0 4300 1 0.140 1 13403602 -200 0 4300 1 0.200 5 13403603 -200 0 4300 1 0.2214 15 13403701 0 0. 0. 0. 15 13403801 0. 15. 15. 0. 0. 0. 0. 1. 15 13403901 0. 15. 15. 0. 0. 0. 0. 1. 15 *_____ * Test Section Internal Wall * 13601000 15 7 2 1 0.02058 13601100 0 1 13601101 2 0.02335 13601102 2 0.02660 13601103 2 0.02937 13601201 1 2 13601202 8 4 * Helium gap 13601203 1 6 13601301 0. 6 13601400 -1 13601401 1039. 1039. 1039. 1039. 1039. 1039. 1039. 13601402 1039. 1039. 1039. 1039. 1039. 1039. 1039. 13601403 1039. 1039. 1039. 1039. 1039. 1039. 1039. 13601404 1039. 1039. 1039. 1039. 1039. 1039. 1039. 13601405 1039. 1039. 1039. 1039. 1039. 1039. 1039. 13601406 1039. 1039. 1039. 1039. 1039. 1039. 1039. 13601407 1039. 1039. 1039. 1039. 1039. 1039. 1039. 13601408 1039. 1039. 1039. 1039. 1039. 1039. 1039. 13601409 1039. 1039. 1039. 1039. 1039. 1039. 1039.



```
13601410 1039. 1039. 1039. 1039. 1039. 1039. 1039.
13601411 1039. 1039. 1039. 1039. 1039. 1039. 1039.
13601412 1039. 1039. 1039. 1039. 1039. 1039. 1039.
13601413 1039. 1039. 1039. 1039. 1039. 1039. 1039.
13601414 1039. 1039. 1039. 1039. 1039. 1039. 1039.
13601415 1039. 1039. 1039. 1039. 1039. 1039. 1039.
13601501 360010000 10000 1 1 0.2214 10
13601502 360110000 10000 1 1 0.20
                                        14
13601503 360150000
                         0 1 1 0.14
                                        15
13601601 340180000 -10000 1 1 0.2214 10
13601602 340080000 -10000 1 1 0.20
                                          14
13601603 340040000
                           0 1 1 0.14
                                          15
13601701 0 0. 0. 0. 15
13601801 0.0 15. 15. 0. 0. 0. 0. 1. 10
13601802 0. 15. 15. 0. 0. 0. 0. 1. 15
13601901 0.0336 15. 15. 0. 0. 0. 0. 1. 10
13601902 0.0336 15. 15. 0. 0. 0. 0. 1. 15
*_____
* Test Section Internal Wall
13602000 3 3 2 1 0.02058
13602100 0 1
13602101 2 0.02335
13602201 1 2
13602301 0. 2
13602400 -1
13602401 1039. 1039. 1039.
13602402 1039. 1039. 1039.
13602403 1039. 1039. 1039.

      13602501
      360160000
      0
      1
      0.155
      1

      13602502
      360170000
      0
      1
      0.326
      2

      13602503
      360180000
      0
      1
      0.14
      3

      13602601
      340030000
      0
      1
      0.155
      1

13602602 340020000
                         0 1 1 0.326 2
13602603 340010000
                         0 1 1 0.14
                                          3
13602701 0 0. 0. 0. 3
13602801 0.0 15. 15. 0. 0. 0. 0. 1. 1
13602802 0.0 15. 15. 0. 0. 0. 0. 1. 2
13602803 0.0 15. 15. 0. 0. 0. 0. 1. 3
13602901 0.0480 15. 15. 0. 0. 0. 0. 1. 1
13602902 0.0845 15. 15. 0. 0. 0. 0. 1. 2
13602903 0.1810 15. 15. 0. 0. 0. 0. 1. 3
*_____
* Test Section Heaters
13603000 10 14 2 1 0.
13603100 0 2
13603101 4.0e-05 5
13603102 3.5e-04 11
13603103 6.0e-04 13
13603201 3 5
13603202 6 11
13603203 7 13
13603301 0. 5
13603302 1. 7
13603303 0. 13
13603400 0
```





```
13671801 0. 15. 15. 0. 0. 0. 0. 1. 1
13671901 0. 15. 15. 0. 0. 0. 0. 1. 1
*_____
* Test Section External Wall
13701000 1 13 2 1 0.03683
13701100 0 2
13701101 3.81e-3 2
13701102 0.016
              12
13701201 1 2
13701202 5 12
13701301 0. 12
13701400 0
13701401 1010. 3
13701402 937. 4
13701403 864. 5
13701404 791. 6
13701405 718. 7
13701406 645. 8
13701407 572. 9
13701408 499. 10
13701409 426. 11
13701410 353. 12
13701411 315. 13
13701501 370010000 0 1 1 0.561 1
13701601 -200 0 4300 1 0.561 1
13701701 0 0. 0. 0. 1
13701801 0. 15. 15. 0. 0. 0. 0. 1. 1
13701901 0. 15. 15. 0. 0. 0. 0. 1. 1
*_____
* Test Section External Wall
*
13702000 1 13 2 1 0.03683
13702100 0 2
13702101 3.81e-3 2
13702102 0.016
               12
13702201 1 2
13702202 5 12
13702301 0. 12
13702400 0
13702401 1010. 3
13702402 937. 4
13702403 864. 5
13702404 791. 6
13702405 718. 7
13702406 645. 8
13702407 572. 9
13702408 499. 10
13702409 426. 11
13702410 353. 12
13702411 315. 13
13702501 352010000 0 1 1 0.0875 1
13702601 -200 0 4300 1 0.0875 1
13702701 0 0. 0. 0. 1
13702801 0. 15. 15. 0. 0. 0. 0. 1. 1
13702901 0. 15. 15. 0. 0. 0. 0. 1. 1
*
```



*_____

* Test Section External Wall * 13703000 1 13 2 1 0.04898 13703100 0 2 13703101 3.81e-3 2 13703102 0.016 12 13703201 1 2 13703202 5 12 13703301 0. 12 13703400 0 13703401 1010. 3 13703402 937. 4 13703403 864. 5 13703404 791. 6 13703405 718. 7 13703406 645. 8 13703407 572. 9 13703408 499. 10 13703409 426. 11 13703410 353. 12 13703411 315. 13 13703501 352010000 0 1 1 0.127 1 13703601 -200 0 4300 1 0.127 1 13703701 0 0. 0. 0. 1 13703801 0. 15. 15. 0. 0. 0. 0. 1. 1 13703901 0. 15. 15. 0. 0. 0. 0. 1. 1 *_____ * Test Section External Wall 13704000 1 13 2 1 0.06113 13704100 0 2 13704101 3.81e-3 2 13704102 0.016 12 13704201 1 2 13704202 5 12 13704301 0. 12 13704400 0 13704401 1010. 3 13704402 937. 4 13704403 864. 5 13704404 791. 6 13704405 718. 7 13704406 645. 8 13704407 572. 9 13704408 499. 10 13704409 426. 11 13704410 353. 12 13704411 315. 13 13704501 352010000 0 1 1 0.485 1 13704601 -200 0 4300 1 0.485 1 13704701 0 0. 0. 0. 1 13704801 0. 15. 15. 0. 0. 0. 0. 1. 1 13704901 0. 15. 15. 0. 0. 0. 0. 1. 1 *_____ * Line A External Wall



13801000 2 13 2 1 0.06098 13801100 0 2 13801101 4.76e-3 2 13801102 0.016 12 13801201 1 2 13801202 5 12 13801301 0. 12 13801400 0 13801401 1010. 3 13801402 937. 4 13801403 864. 5 13801404 791. 6 13801405 718. 7 13801406 645. 8 13801407 572. 9 13801408 499. 10 13801409 426. 11 13801410 353. 12 13801411 315. 13 $13801501 \ 380010000 \ 10000 \ 1 \ 1 \ 0.667 \ 2$ $13801601 \ -200 \ 0 \ 4300 \ 1 \ 0.667 \ 2$ 13801701 0 0. 0. 0. 2 13801801 0. 15. 15. 0. 0. 0. 0. 1. 2 13801901 0. 15. 15. 0. 0. 0. 0. 1. 2 *_____ * Line A External Wall * 13901000 2 13 2 1 0.06098 13901100 0 2 13901101 4.76e-3 2 13901102 0.016 12 13901201 1 2 13901202 5 12 13901301 0. 12 13901400 0 13901401 1010. 3 13901402 937. 4 13901403 864. 5 13901404 791. 6 13901405 718. 7 13901406 645. 8 13901407 572. 9 13901408 499. 10 13901409 426. 11 13901410 353. 12 13901411 315. 13 13901501 390010000 10000 1 1 0.510 2 13901601 -200 0 4300 1 0.510 2 13901701 0 0. 0. 0. 2 13901801 0. 15. 15. 0. 0. 0. 0. 1. 2 13901901 0. 15. 15. 0. 0. 0. 0. 1. 2 *_____ * Line B External Wall 14201000 4 13 2 1 0.04844 14201100 0 2 14201101 4.28e-3 2

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```
14201201 1 2
14201202 2 12
14201301 0. 12
14201400 0
14201401 554. 3
14201402 527. 4
14201403 500. 5
14201404 473. 6
14201405 446. 7
14201406 419. 8
14201407 392. 9
14201408 365. 10
14201409 338. 11
14201410 311. 12
14201411 392. 13
14201501 420010000 10000 1 1 0.502 4
14201601 -200 0 4300 1 0.502 4
14201701 0 0. 0. 0. 4
14201801 0. 15. 15. 0. 0. 0. 0. 1. 4
14201901 \ 0. \ 15. \ 15. \ 0. \ 0. \ 0. \ 1. \ 4
*_____
* Line B External Wall
14301000 1 13 2 1 0.04844
14301100 0 2
14301101 4.28e-3 2
14301102 0.01
             12
14301201 1 2
14301202 2 12
14301301 0. 12
14301400 0
14301401 554. 3
14301402 527. 4
14301403 500. 5
14301404 473. 6
14301405 446. 7
14301406 419. 8
14301407 392. 9
14301408 365. 10
14301409 338. 11
14301410 311. 12
14301411 392. 13
14301501 430010000 0 1 1 1.718 1
14301601 -200 0 4300 1 1.718 1
14301701 0 0. 0. 0. 1
14301801 0. 15. 15. 0. 0. 0. 0. 1. 1
14301901 0. 15. 15. 0. 0. 0. 0. 1. 1
*_____
* Line B External Wall
14401000 2 13 2 1 0.04844
14401100 0 2
14401101 4.76e-3 2
14401102 0.01 12
14401201 1 2
14401202 2 12
```

ENER

14201102 0.01

12



14401301 0. 12 14401400 0 14401401 554. 3 14401402 527. 4 14401403 500. 5 14401404 473. 6 14401405 446. 7 14401406 419. 8 14401407 392. 9 14401408 365. 10 14401409 338. 11 14401410 311. 12 14401411 392. 13 14401501 440010000 10000 1 1 1.31 2 14401601 -200 0 4300 1 1.31 2 14401701 0 0. 0. 0. 2 $14401801 \ 0. \ 15. \ 15. \ 0. \ 0. \ 0. \ 1. \ 2$ 14401901 0. 15. 15. 0. 0. 0. 0. 1. 2 *_____ * Aircooler Tubes Wall 14601000 11 15 2 1 0.00905 14601100 0 1 14601101 14 0.01065 14601201 1 14 14601301 1. 14 14601400 0 14601401 373. 15 14601501 460020000 10000 3400 1 22.0 11 14601601 -500 0 1000 1 22.0 11 14601701 0 0. 0. 0. 11 14601801 0. 15. 15. 0. 0. 0. 0. 1. 11 14601901 0. 15. 15. 0. 0. 0. 0. 1. 11 *_____ * Line C External Wall * 14801000 5 9 2 1 0.04844 14801100 0 2 14801101 4.28e-3 2 14801102 0.01 8 14801201 1 2 14801202 2 8 14801301 0. 8 14801400 0 14801401 373. 3 14801402 358. 4 14801403 343. 5 14801404 328. 6 14801405 313. 7 14801406 298. 8 14801407 288. 9 14801501 480010000 10000 1 1 0.47 5 14801601 -200 0 4300 1 0.47 5 14801701 0 0. 0. 0. 5 14801801 0. 15. 15. 0. 0. 0. 0. 1. 5 14801901 0. 15. 15. 0. 0. 0. 0. 1. 5 *



*_____ * Line C External Wall 14802000 4 9 2 1 0.02624 14802100 0 2 14802101 1.955e-3 2 14802102 0.01 8 14802201 1 2 14802202 2 8 14802301 0. 8 14802400 0 14802401 373. 3 14802402 358. 4 14802403 343. 5 14802404 328. 6 14802405 313. 7 14802406 298. 8 14802407 288. 9 14802501 480060000 10000 1 1 0.275 4 14802601 -200 0 4300 1 0.275 4 14802701 0 0. 0. 0. 4 $14802801 \ 0. \ 15. \ 15. \ 0. \ 0. \ 0. \ 1. \ 4$ 14802901 0. 15. 15. 0. 0. 0. 0. 1. 4 *_____ * Dummy Structure for compressor cooling 12571000 1 5 2 1 0.015 12571100 0 1 12571101 4 0.0165 12571201 1 4 12571301 1. 4 12571400 0 12571401 352.66 5 12571501 257010000 10000 3400 1 22.0 1 12571601 -600 0 1000 1 22.0 1 12571701 0 0. 0. 0. 1 12571801 0. 15. 15. 0. 0. 0. 0. 1. 1 12571901 0. 15. 15. 0. 0. 0. 0. 1. 1 *_____ _____ * materials tables *_____ * 20100100 tbl/fctn 1 1 * Stainless Steel 316 * conductivity k (w/m/K) 20100101 253. 13.223 20100102 323. 14.322 20100103 353. 14.793 20100104 373. 15.108 20100105 473. 16.679 20100106 573. 18.249 20100107 673. 19.821 20100108 773. 21.392 20100109 873. 22.963 20100110 973. 24.534 20100111 1973. 24.534 20100112 2500. 24.534



```
* heat capacity rocp (j/m3/K)
20100151 253. 4.02e3
20100152 323. 4.09e3
20100153 353. 4.12e3
20100154 373. 4.14e3
20100155 473. 4.20e3
20100156 573. 4.25e3
20100157 673. 4.28e3
20100158 773. 4.31e3
20100159 873. 4.34e3
20100160 973. 4.39e3
20100161 1973. 4.39e3
20100162 2500. 4.39e3
*_____
20100200 tbl/fctn 1 1 * rockwool1
* conductivity k (w/m/K)
20100201 273. 0.035
20100202 423. 0.05
20100203 573. 0.075
20100204 723. 0.10
20100205 873. 0.125
20100206 2500. 0.125
* heat capacity rocp (j/m3/K)
20100251 253. 0.615e3
20100252 323. 0.615e3
20100253 353. 0.615e3
20100254 373. 0.615e3
20100255 473. 0.615e3
20100256 573. 0.615e3
20100257 673. 0.615e3
20100258 773. 0.615e3
20100259 873. 0.615e3
20100260 973. 0.615e3
20100261 1973. 0.615e3
20100262 2500. 0.615e3
*_____
20100300 tbl/fctn 1 1 * Magnesia Oxide
* conductivity k (w/m/K)
20100301 253. 2.077
20100302 323. 2.077
20100303 353. 2.077
20100304 373. 2.077
20100305 473. 2.077
20100306 573. 2.077
20100307 673. 2.077
20100308 773. 2.077
20100309 873. 2.077
20100310 973. 2.077
20100311 1973. 2.077
20100312 2500. 2.077
*
 heat capacity rocp (j/m3/K)
20100351 253. 2.681e3
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20100352 323. 2.681e3
20100353 353. 2.681e3
20100354 373. 2.681e3
20100355 473. 2.681e3
20100356 573. 2.681e3
20100357 673. 2.681e3
20100358 773. 2.681e3
20100359 873. 2.681e3
20100360 973. 2.681e3
20100361 1973. 2.681e3
20100362 2500. 2.681e3
*_____
20100400 tbl/fctn 1 1 * Rockwool in heaters/economizer zone
* conductivity k (w/m/K)
20100401 273. 0.035
20100402 423. 0.05
20100403 573. 0.075
20100404 723. 0.10
20100405 873. 0.125
20100406 2500. 0.125
* heat capacity rocp (j/m3/K)
20100451 253. 0.615e3
20100452 323. 0.615e3
20100453 353. 0.615e3
20100454 373. 0.615e3
20100455 473. 0.615e3
20100456 573. 0.615e3
20100457 673. 0.615e3
20100458 773. 0.615e3
20100459 873. 0.615e3
20100460 973. 0.615e3
20100461 1973. 0.615e3
20100462 2500. 0.615e3
*_____
20100500 tbl/fctn 1 1 * Rockwool in Test Section zone
* conductivity k (w/m/K)
20100501 273. 0.035
20100502 423. 0.05
20100503 573. 0.075
20100504 723. 0.10
20100505 873. 0.125
20100506 2500. 0.125
* heat capacity rocp (j/m3/K)
20100551 253. 0.615e3
20100552 323. 0.615e3
20100553 353. 0.615e3
20100554 373. 0.615e3
20100555 473. 0.615e3
20100556 573. 0.615e3
20100557 673. 0.615e3
20100558 773. 0.615e3
20100559 873. 0.615e3
20100560 973. 0.615e3
```



20100561 1973. 0.615e3 20100562 2500. 0.615e3 *_____ 20100600 tbl/fctn 1 1 * Boro Nitrade(TS pin) 20100601 253. 30. 20100602 2500. 30. 20100651 253. 3.059e3 20100652 2500. 3.059e3 _____ *_____ 20100700 tbl/fctn 1 1 * Ni-Cr-Fe Alloy (TS pin) 20100701 253. 12.456 20100702 373. 12.456 20100703 1143. 25.085 20100704 2500. 25.085 20100751 253. 4.1e3 20100752 2500. 4.1e3 *_____ 20100800 tbl/fctn 1 1 * Helium Gap 20100801 253. 0.244 20100802 573. 0.244 20100803 673. 0.273 20100804 773. 0.302 20100805 2500. 0.302 20100851 253. 5.20e3 20100852 2500. 5.20e3 *_____ * general tables *_____ * Heater 219/3 Power (Max 70 kw) * 20210100 power 0 1. 70000. -1. 0.0 20210101 20210102 0.0 Ο. 20210103 1.e6 0.0 20550100 pwhtr1 function 1. 0. 1 20550101 time 0 101 *_____ * Heater 219/2 Power (Max 70 kw) power 0 1. 70000. 20210200 -1. 20210201 0.0 20210202 Ο. 0.0 50. 20210203 0. 0.0 100. 20210204 0.0 1.e6 20210205 20550200 pwhtr2 function 1. 0. 1 20550201 time 0 102



```
*
*_____
* Heater 219/1 Power (Max 70 kw)
                1. 70000.
20210300
        power O
        -1.
0.
                0.16
20210301
                0.16
20210302
         50.
                0.16
20210303
        100.
                0.143
20210304
       500.
550.
1.e6
                0.143
0.0
20210305
20210306
               0.0
20210307
20550300 pwhtr3 function 1. 0. 1
20550301 time 0 103
*_____
* Test Section pins power (Max 300 kw)
20215000 power 0 1. 300.0e3

        20215001
        -1.
        0.

        20215002
        0.
        0.

        20215003
        50.
        0.

              0.
0.237
0.237
20215004 100.
20215005 500.
20215006 550.
               0.25
20215007 1.e6
               0.25
20555000 pwtsts function 1. 0. 1
20555001 time 0 150
*_____
* Room temperature
*
20220000
        temp
                298.
20220001 -1.
20220002
         Ο.
                 298.
20220003
         50.
                 288.16
                288.16
278.16
20220004
         100.
20220005
         500.
20220006
         99999. 278.16
*_____
* Thermal Exchange Coefficient external pipes-room (air natural convection)
*
20230000
        htc-temp
        293. 10.0
20230001
20230002
         373. 10.0
*_____
* Thermal Exchange Coefficient for heaters external pipes-room (air natural
convection)
20230100
        htc-temp
        293. 10.0
20230101
         373. 10.0
20230102
*_____
```



```
* Thermal Exchange Coefficient for vol 171 external wall-room (air natural
convection)
20230200
        htc-temp
       293. 10.0
20230201
        373. 10.0
20230202
*_____
* Thermal Exchange Coefficient for economizer external wall-room (air
natural convection)
20230300
        htc-temp
20230301
        293. 10.0
        373. 10.0
20230302
*_____
* Dummy Thermal Exchange Coefficient for air-cooler tubes
20240000
        htc-t
        -1.
20240001
              1000.
20240002
        Ο.
              1000.
20240003
        1.e6
              1000.
*_____
*
  Thermal Sink for Aircooler Outlet Temperature Regulation
*
20250000
       temp
20250001 -1. 347.66
        0.
20250002
             347.66
20250003 50.
             347.66
20250004 100.
             348.16
20250005 1.e6
             348.16
*_____
* Compressor Cooling Control
*
* Mass flowrate depending from compressor head
20205000 reac-t 530
        head
               massflowrate
20205001
      -1.
                0.
20205002
      0.
                  Ο.
20205003
      0.57e5
                 0.018
        0.79e5
20205004
                 0.023
       0.92e5
20205005
                 0.024
20205006
       1.05e5
                 0.026
20205007
        1.2e5
                  0.028
20205008
        1.26e5
                  0.029
20205009
       1.37e5
                  0.030
* heat sink for temperature regulation
20260000 temp 530
20260001
              352.66
        -1.
20260002
              327.5
         0.
        50.
             327.5
20260002
      99999. 327.5
20260003
*_____
* Control variables
*_____
```



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* 007 tempera 20500700 ec 20500701 0 20500702	ature drop cotbdt	aircool sum 1. -1.	er tube 1. tempg tempg	es side 0. 1 460010000 460130000
* 008 tempera 20500800 r: 20500801 0 20500802 *	ature drop iscldt	heater sum 1. -1.	E219/3 1. tempg tempg	0. 1 240100000 240010000
* 009 tempera 20500900 r: 20500901 0 20500902 *	ature drop isc2dt	heater sum 1. -1.	E219/2 1. tempg tempg	0. 1 260100000 260010000
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20501417 1. q 200170000 20501418 1. q 200180000 20501419 1. q 200190000 * * 015 power from helium in economizer tubes 20501500 Pecotub sum 1. 0. 1 20501501 0. 1. q 400030000 20501502 1. q 400040000 20501503 1. q 400050000 20501504 1. q 400070000 20501505 1. q 400090000 20501506 1. q 400100000 20501507 1. q 400120000 20501508 1. q 400120000 20501510 1. q 400140000 20501511 1. q 400150000 20501512 1. q 400150000 20501513 1. q 400180000 20501514 1. q 400180000 20501515 1. q 40020000 20501518 1. q 40020000 20501519 1. q 40020000 20501519 1. q 40020000 20501519 1. q	20501416	1.	q	200160000				
20501418 1. q 200180000 20501419 1. q 200190000 * * * 015 power from helium in economizer tubes 20501500 Pecotub sum 1. 0. 1 20501501 0. 1. q 400030000 20501502 1. q 400060000 20501503 1. q 400060000 20501504 1. q 400070000 20501505 1. q 400080000 20501506 1. q 400100000 20501507 1. q 400120000 20501508 1. q 400120000 20501510 1. q 400130000 20501511 1. q 400130000 20501512 1. q 400160000 20501513 1. q 400170000 20501514 1. q 400180000 20501515 1. q 400180000 20501516 1. q 40020000 20501518 1. q 40020000 20501519 1. q 40020000 20501519 1. q 400210000 <td>20501417</td> <td>1.</td> <td>q</td> <td>200170000</td> <td></td> <td></td> <td></td> <td></td>	20501417	1.	q	200170000				
20501419 1. q 200190000 * * * 015 power from helium in economizer tubes 20501500 Pecotub sum 1. 0. 1 20501501 0. 1. q 40003000 20501502 1. q 40004000 20501503 1. q 400050000 20501504 1. q 40007000 20501505 1. q 40009000 20501506 1. q 40010000 20501507 1. q 400120000 20501510 1. q 400120000 20501511 1. q 400120000 20501512 1. q 400120000 20501513 1. q 400120000 20501514 1. q 400120000 20501515 1. q 400140000 20501516 1. q 400180000 20501516 1. q 400180000 20501517 1. q 400210000 20501519 1. q 400210000 20501519 1. q 400210000 20501519 1. q 400210000 20501519	20501418	1.	q	200180000				
* 015 power from helium in economizer tubes 20501500 Pecotub sum 1. 0. 1 20501501 0. 1. q 400030000 20501502 1. q 400040000 20501503 1. q 400050000 20501504 1. q 400060000 20501505 1. q 400070000 20501506 1. q 400080000 20501507 1. q 400100000 20501508 1. q 40010000 20501510 1. q 400110000 20501510 1. q 400120000 20501511 1. q 400130000 20501512 1. q 400140000 20501513 1. q 400150000 20501514 1. q 400170000 20501515 1. q 400170000 20501516 1. q 400180000 20501516 1. q 400120000 20501517 1. q 400120000 20501518 1. q 400120000 20501518 1. q 400120000 20501519 1. q 400120000 *	20501419	1.	q	200190000				
20501500 Pecotub sum 1. 0. 1 20501501 0. 1. q 400030000 20501502 1. q 400050000 20501503 1. q 400060000 20501504 1. q 400070000 20501505 1. q 400080000 20501506 1. q 40009000 20501507 1. q 400100000 20501508 1. q 400120000 20501510 1. q 400120000 20501510 1. q 400120000 20501511 1. q 400140000 20501512 1. q 400150000 20501513 1. q 400160000 20501514 1. q 400180000 20501515 1. q 400190000 20501517 1. q 400200000 20501518 1. q 400210000 * * * * *	* 015 p	ower from helium in eco	onom	nizer tubes				
20501501 0. 1. q 400030000 20501502 1. q 400050000 20501503 1. q 40006000 20501504 1. q 40007000 20501505 1. q 40007000 20501506 1. q 40008000 20501507 1. q 40010000 20501508 1. q 40010000 20501510 1. q 400120000 20501510 1. q 400130000 20501511 1. q 400140000 20501512 1. q 400170000 20501513 1. q 400170000 20501514 1. q 400180000 20501515 1. q 400180000 20501517 1. q 400200000 20501518 1. q 400210000 20501519 1. q 400210000 * * * *	20501500	Pecotub sum	1	. 0. 1				
20501502 1. q 400040000 20501503 1. q 400050000 20501504 1. q 400070000 20501505 1. q 400090000 20501506 1. q 400100000 20501507 1. q 400100000 20501508 1. q 400120000 20501510 1. q 400120000 20501511 1. q 400130000 20501512 1. q 400150000 20501513 1. q 400140000 20501514 1. q 400150000 20501515 1. q 400170000 20501516 1. q 400180000 20501518 1. q 400190000 20501519 1. q 400200000 20501519 1. q 400210000 * * * * *	20501501	0. 1.	q	400030000				
20501503 1. q 400050000 20501504 1. q 400070000 20501505 1. q 400080000 20501506 1. q 400090000 20501507 1. q 400100000 20501508 1. q 400110000 20501509 1. q 400120000 20501510 1. q 400130000 20501511 1. q 400140000 20501512 1. q 400150000 20501513 1. q 400170000 20501514 1. q 400170000 20501515 1. q 400180000 20501516 1. q 400190000 20501518 1. q 400200000 20501519 1. q 400210000 * * * *	20501502	1.	q	400040000				
20501504 1. q 400060000 20501505 1. q 400070000 20501506 1. q 400090000 20501507 1. q 400100000 20501508 1. q 400120000 20501510 1. q 400120000 20501511 1. q 400130000 20501512 1. q 400150000 20501513 1. q 400160000 20501514 1. q 400170000 20501515 1. q 400180000 20501517 1. q 400190000 20501518 1. q 400200000 20501519 1. q 400200000 20501519 1. q 400200000 * 016 power from helium in aircooler -	20501503	1.	q	400050000				
20501505 1. q 400070000 20501506 1. q 400080000 20501507 1. q 400090000 20501508 1. q 400100000 20501509 1. q 400120000 20501510 1. q 400130000 20501511 1. q 400140000 20501512 1. q 400150000 20501513 1. q 400160000 20501514 1. q 400170000 20501515 1. q 400180000 20501517 1. q 400190000 20501518 1. q 400200000 20501519 1. q 400200000 20501519 1. q 400210000 * * * * *	20501504	1.	q	400060000				
20501506 1. q 400080000 20501507 1. q 400090000 20501508 1. q 40010000 20501509 1. q 400120000 20501510 1. q 400130000 20501511 1. q 400140000 20501512 1. q 400150000 20501513 1. q 400160000 20501514 1. q 400170000 20501515 1. q 400180000 20501517 1. q 400190000 20501518 1. q 400200000 20501519 1. q 400200000 20501519 1. q 400210000 * * * * *	20501505	1.	q	400070000				
20501507 1. q 40009000 20501508 1. q 40010000 20501509 1. q 400120000 20501510 1. q 400130000 20501512 1. q 400150000 20501513 1. q 400160000 20501514 1. q 400160000 20501515 1. q 400170000 20501516 1. q 400190000 20501517 1. q 400190000 20501518 1. q 400200000 20501519 1. q 400210000 * * * *	20501506	1.	q	400080000				
20501508 1. q 40010000 20501509 1. q 400120000 20501510 1. q 400130000 20501512 1. q 400140000 20501513 1. q 400160000 20501514 1. q 400170000 20501515 1. q 400180000 20501516 1. q 400190000 20501518 1. q 400200000 20501519 1. q 400210000 * 016 power from helium in aircooler 1	20501507	1.	q	400090000				
20501509 1. q 400110000 20501510 1. q 400120000 20501511 1. q 400130000 20501512 1. q 400140000 20501513 1. q 400150000 20501514 1. q 400160000 20501515 1. q 400170000 20501516 1. q 400180000 20501517 1. q 400190000 20501518 1. q 400210000 * 016 power from helium in aircooler 1	20501508	1.	q	400100000				
20501510 1. q 400120000 20501511 1. q 400130000 20501512 1. q 400140000 20501513 1. q 400150000 20501514 1. q 400160000 20501515 1. q 400170000 20501516 1. q 400180000 20501517 1. q 400190000 20501518 1. q 400210000 * 016 power from helium in aircooler 1	20501509	1.	q	400110000				
20501511 1. q 400130000 20501512 1. q 400140000 20501513 1. q 400150000 20501514 1. q 400160000 20501515 1. q 400170000 20501516 1. q 400180000 20501517 1. q 400190000 20501518 1. q 400200000 20501519 1. q 400210000 * 016 power from helium in aircooler 1	20501510	1.	q	400120000				
20501512 1. q 400140000 20501513 1. q 400150000 20501514 1. q 400160000 20501515 1. q 400170000 20501516 1. q 400180000 20501517 1. q 400190000 20501518 1. q 400200000 20501519 1. q 400210000 * 016 power from helium in aircooler 1	20501511	1.	q	400130000				
20501513 1. q 400150000 20501514 1. q 400160000 20501515 1. q 400170000 20501516 1. q 400180000 20501517 1. q 400190000 20501518 1. q 400200000 20501519 1. q 400210000 * 016 power from helium in aircooler 1	20501512	1.	q	400140000				
20501514 1. q 400160000 20501515 1. q 400170000 20501516 1. q 400180000 20501517 1. q 400190000 20501518 1. q 400200000 20501519 1. q 400210000 * 016 power from helium in aircooler 1	20501513	1.	q	400150000				
20501515 1. q 400170000 20501516 1. q 400180000 20501517 1. q 400190000 20501518 1. q 400200000 20501519 1. q 400210000 * * 016 power from helium in aircooler 1	20501514	1.	q	400160000				
20501516 1. q 400180000 20501517 1. q 400190000 20501518 1. q 400200000 20501519 1. q 400210000 *	20501515	1.	q	400170000				
20501517 1. q 400190000 20501518 1. q 400200000 20501519 1. q 400210000 * * 016 power from helium in aircooler	20501516	1.	q	400180000				
20501518 1. q 40020000 20501519 1. q 400210000 * * 016 power from helium in aircooler	20501517	1.	q	400190000				
20501519 1. q 400210000 * * 016 power from helium in aircooler	20501518	1.	q	400200000				
* * 016 power from helium in aircooler	20501519	1.	q	400210000				
	* * 016 m	ower from helium in air	raoo	oler				
20501600 Paero sum 1. 0. 1	20501600	Paero sum	1.	0. 1				

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ENEL C	ENEN Centro Ricerche Bologna		FPN – P9LU – 015	0	R	124	132
20501601	0. 1.	q	460020000				
20501602	1.	q	460030000				
20501603	1.	q	460040000				
20501604	1.	q	460050000				
20501605	1.	q	460060000				
20501606	1.	q	460070000				
20501607	1.	q	460080000				
20501608	1.	q	460090000				
20501609	1.	q	460100000				
20501610	1.	q	460110000				
20501611	1.	q	460120000				
*							
*							
* 017 Heat	Losses in TS acti	ve z	one				
20501700	Pbach sum		1. 0. 0				
20501701	0. 1.	q	360010000				
20501702	1.	q	360020000				
20501703	1.	q	360030000				
20501704	1.	q	360040000				
20501705	1.	q	360050000				
20501706	1.	q	360060000				
20501707	1.	q	360070000				
20501708	1.	q	360080000				
20501709	1.	q	360090000				
20501710	1.	q	360100000				
20501711	1.	q	360110000				
20501712	1.	q	360120000				
20501713	1.	q	360130000				
20501714	1.	q	360140000				
20501715	1.	q	360150000				
20501716	1.	q	360160000				
20501717	1.	q	360170000				
20501718	1.	q	360180000				
20501719	-1.	CI	ntrlvar 550				
*							
* 000 1	-						
^ 020 neat	CINC1	r-eco	onom. line				
20502000		⊥.	U. 1 120010000				
20502001	0. 1.	q	120020000				
20502002	1	q	140010000				
20502003	1.	Ч С	140020000				
20502004	1.	Ч С	140020000				
20502005	1	Ч с	140040000				
20502000	±• 1	ч а	140050000				
20502007	±• 1	Ч с	160010000				
20502000	±• 1	ч а	160020000				
20502009	±• 1	ч а	160020000				
20502010	⊥• 1	ч ~	160040000				
20502012	±• 1	ч л	160050000				
20502013	±• 1	r n	160060000				
20502014	±• 1	r n	160070000				
20502015	1.	r n	160080000				
20502016	1.	a a	160090000				
20502017	1.	a a	170010000				
20502018	1.	a	173010000				
20502019	1.	a	180010000				
20502020	1.	a	180020000				
*		1					



*					
* 021 heat	losses	by-pass	line		
20502100	SUM1	sum	1.	0.	1
20502101	0.	1.	. q		171010000
20502102		1.	q		171020000
20502103		1.	q		171030000
20502104		1.	q		171040000
20502105		1.	q		315010000
20502106		1.	q		315020000
20502107		1.	q		315030000
20502108		1.	q		315040000
*					
* 022 heat	losses	heaters	connecti	ons	
20502200	SUM2	sum	1.	0.	1
20502201	0.	1.	q		210010000
20502202		1.	q		220010000
20502203		1.	q		220020000
20502204		1.	q		230010000
20502205		1.	q		250010000
20502206		1.	р		270010000
20502207		1.	q		280010000
20502208		1.	q		280020000
20502209		1.	a		290010000
*			Ľ		
* 023 heat	losses	TS inlet	-		
20502300	SUM3	sum	1.	0.	1
20502301	0.	1.	р		310010000
20502302		1.	q		320010000
20502303		1.	q		320020000
20502304		1.	a		320030000
20502305		1.	a		320040000
20502306		1.	a		325010000
20502307		1.	a		330010000
*			Ľ		
* 024 heat	losses	TS			
20502400	SUM4	sum	1.	0.	1
20502401	0.	1.	q		340010000
20502402		1.	q		340020000
20502403		1.	q		340030000
20502404		1.	q		340040000
20502405		1.	q		340050000
20502406		1.	q		340060000
20502407		1.	q		340070000
20502408		1.	q		340080000
20502409		1.	a		340090000
20502410		1.	a		340100000
20502411		1	r D		340110000
20502412		1	P		340120000
20502112		1	P		340130000
20502415		1	Ч Ф		340140000
20302714 20502715		⊥. 1	Ч ~		340150000
20202712		±• 1	Ч ~		340160000
20302410		⊥. 1	Ч ~		340170000
2030241/ 20502410		⊥. 1	ч ~		3401/0000
∠UDU∠4⊥8 *		1.	q		240100000
* 025 Heat	losses	TS-econd	omizer li	ne	
20502500	SUM5	sum	1.	0.	1
20502501	0.	1.	a		352010000
20502502		1.	q		365010000

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ENEL	Centro Rice	erche Bol	logna	FPN	– P	9LU – 015	0	R	126	132
20502503		1.		q	367	010000				
20502504		1.		a	370	010000				
20502505		1.		q	380	010000				
20502506		1.		q	380	020000				
20502507		1.		a	390	010000				
20502508		1.		q	390	020000				
*				-						
* 026 h	eat losses	economi	zer-ai:	rcooler	lin	9				
20502600	SUM6	sum	1.	0.	1					
20502601	0.	1.		q	420	010000				
20502602		1.		q	420	020000				
20502603		1.		q	420	030000				
20502614		1.		q	420	040000				
20502615		1.		q	430	010000				
20502616		1.		q	440	010000				
20502617 *		1.		d	440	020000				
* 027 h	eat losse a	ircoole	r-comp:	ressor						
20502700	SUM7	sum	1.	0.	1					
20502701	0.	1.		q	480	010000				
20502702		1.		q	480	020000				
20502703		1.		q	480	030000				
20502704		1.		q	480	040000				
20502705		1.		q	480	050000				
20502706		1.		q	480	060000				
20502707		1.		q	480	070000				
20502708		1.		q	480	080000				
20502709 *		1.		q	480	090000				
* 031 he	at losse ec	onomize	r							
20503100	pexecon	L	sum	1.	0.	1				
20503101	0.	1.	cntrl	var 015						
20503102		1.	cntrl	var 014						
*										
* 032 he	at losses h	leaters								
20503200	pexheat		sum	1.	0.	1				
20503201	0.	1.	cntrl	var 011						
20503202		1.	cntrl	var 012						
20503203		1.	cntrl	var 013						
20503204		1.	cntrl	var 022						
*										
* 033 he	at losses t	est sec	tion							
20503300	pextest		sum -	1.	0.	1				
20503301	0. 1		cntrlv	ar 017						
20503302		1.	C	ntrlvar	024					
20503303		1.	C	ntrlvar	023					
20503304 *		⊥.	C:	ntrlvar	025					
* 034 he	at losses l	oop col	d zone							
20503400	pexcold	l ;	sum	1.	0.	1				
20503401	0.	1.	cntrl	var 020						
20503402		1.	cntrl	var 026						
20503403 *		1.	cntrl	var 027						
* 030 t	otal heat l	osses								
20503000	pext	sum	1	. 0.	1					
20503001	0.	1.		cntrlva	03	1				
20503002		1.		cntrlva	c 03	2				
20503003		1.		cntrlvai	c 03	3				



20503005 1. cntrlvar 034 20503006 1. cntrlvar 021 * 040 Compressor pressure drop 1. Ο. 20504000 DP sum 1 p 120010000 Ο. 20504001 1. 20504002 p 480090000 -1. * _ _ _ _ _____ * Temperatures in Celsius ° 20520000 t215 sum 1. 0. 1 20520001 -273.16 1. tempg 180020000 20520100 t216 sum 1. 0. 1 20520101 -273.16 1. tempg 210010000 20520200 t221 sum 1. 0. 1 20520201 -273.16 1. tempg 250010000 20520300 t222 sum 1. 0. 1 20520301 -273.16 1. tempg 270010000 20520400 t223 sum 1. 0. 1 20520401 -273.16 1. tempg 300140000 20520500 t232 sum 1. 0. 1 20520501 -273.16 1. tempg 310010000 20520600 t217 sum 1. 0. 1 20520601 -273.16 1. tempg 390020000 * 20520700 t218 sum 1. 0. 1 20520701 -273.16 1. tempg 420010000 20520800 t202 sum 1. 0. 1 20520801 -273.16 1. tempg 460130000 20520900 t204 sum 1. 0. 1 20520901 -273.16 1. tempg 120010000 20521000 ts0222 sum 1. 0. 1 20521001 -273.16 0.5 httemp 360300114 0.5 httemp 360300113 20521002 20521100 ts1776 sum 1. 0. 1 20521101 -273.16 0.5 httemp 360300814 0.5 httemp 360300813 20521102 20521200 t215cr sum 1. 0. 1 20521201 -273.16 0.5 httemp 180100101 0.5 httemp 180100102 20521202 20521300 t216cr sum 1. 0. 1 -273.16 0.5 httemp 210100101 20521301 0.5 httemp 210100102 20521302 20521400 t217cr sum 1. 0. 1 20521401 -273.16 0.5 httemp 390100201



Centro Ricerche Bologna

0.5 httemp 390100202 20521402 20521500 t218cr sum 1. 0. 1 20521501 -273.16 0.5 httemp 420100101 0.5 httemp 420100102 20521502 *_____ * 050 Compressor Cooling Control 20505000valve_rifunction 1.0.120505001cntrlvar040050 20505600 valfalse mult 1. 0. 1 20505601 mflowj 256000000 *_____ * 041 Test Section Pressure Drop sum 1. 0. 1 1. p 365010000 20504100 DP 1 20504101 0. p 330010000 20504102 -1. *_____ * Control of Test Section Inlet Temperature trough valve 172 20515200 constant constant 573.16 * TS inlet Temperature imposed 0.1 0.0 20515300 errt sum 1 20515301 0.0 -1. cntrlvar 152 1. tempg 310010000 *err. of TS inlet 20515302 temperature 20515400 re-pi prop-int 5.0 0. 1 3 0.000 1.000 1. 0.08 cntrlvar 153 20515401 * 13-1.1. 20515500 difp sum 1. 0. 20515501 0.0 1. cntrlvar 154 20515502 -1. vlvarea 172 20515600 attbeam integral 0.05 0.13-0.01.0 20515601 cntrlvar 155 20515700 adder sum 1. 0. 0 20515701 0.0 1.0 cntrlvar 156 -1.0 vlvstem 172 *_____ * Loop Mass Flowrate to control pump velocity 20260100 temp 530 20260101 -1. 0.2255 20260102 0. 0.2255 20260103 50. 0.2255 20260104 100. 0.2166 20260105 200. 0.2166 20260106 500. 0.15 20260107 99999. 0.15 20509900 dmflow sum 1. 0. 1 20509901 0. 1. cntrlvar 101 -1. mflowj 150000000 *20509901 .1 -1. mflowj 15000000



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*
20510000 dngiri integral 100. 1361. 1
20510001 cntrlvar 99
*
* portata nel circuito in funzione del tempo
20510100 port function 1. 1. 1
20510101 time 0 601
*
.
```



APPENDIX B: Test Specifications

Procedure for the Start-up by steps

At the beginning of the start-up the HE-FUS3 loop will be in a cold state at 30 bar. The compressor velocity will be settled at about 1000 rad/s (9500 rpm) that corresponds to 0,095 kg/s massflowrate in the loop.

The air mass flowrate in the air cooler will be regulated in order to maintain the helium temperature at the compressor inlet at 75 °C for the whole duration of the start-up. The helium temperature at the inlet of the test section will be controlled by means the by-pass valve FV234 in order not to exceed 300 °C for the whole duration of the start-up. These controls will be maintained active for the whole duration of the experimental campaign.

To take advantage of the new acquisition system implemented in the Test Section that allows a more precise measurements of the electrical power, it is recommended to use the test section to supply the power to the loop rather than the heaters.

<u>First step</u>: The power in the test section will be settled at 36 kW according to the test section control timing. In order to be sure to get acceptable steady state conditions the loop should operate in these conditions for about 15 hours (according to the numerical simulation), anyway the variation of the loop temperature (TR223) should not exceed 1 °C in half an hour. The acquisition of the loop parameters is required every second for the first 500s and every minute until the achievement of the new steady state conditions.

When the steady state conditions are attained the actual heat losses in the loop will be calculated by means of a loop thermal balance in order to compensate them in the following steps. Before starting the next step the loop pressure will be checked and just in case that, owing to the helium leak, it is decreased under 30 bar, this initial value will be restored.

<u>Second step</u>: Starting from the steady state conditions at 30-32 bar pressure and 36 kW power, the compressor velocity will be increased from 1000 rad/s up to 1200 rad/s (11500 rpm) according to the compressor control timing. The achievement of acceptable steady state conditions is expected after 15 hours of the loop operation in these conditions.

The verification of the steady state achievement as well as the pressure control have to be performed as in the previous step before going on with the next one.

<u>Third step</u>: Starting from the steady state conditions at 30-32 bar pressure and 1200 rad/s the power in the test section will be increased from 36 kW to 52,5 kW (value to be revised if the heat losses compensation is required) according to the test section control timing. The achievement of acceptable steady state conditions is expected after 15 hours of the loop operation in these conditions.

The verification of the steady state achievement as well as the pressure control have to be performed as in the previous steps before going on with the next one.



<u>Forth step</u>: Starting from the steady state conditions at 30-33 bar pressure and 52,5 kW power, the compressor velocity will be increased from 1200 rad/s up to 1480 rad/s (14100 rpm) according to the compressor control timing. The final compressor velocity cold be reduced in case that the technologic limits in the compressor operation could be exceeded (e.g. maximum bearing temperature). The achievement of acceptable steady state conditions is expected after 15 hours of the loop operation in these conditions.

The verification of the steady state achievement as well as the pressure control have to be performed as in the previous steps before going on with the next one.

<u>Fifth step</u>: Starting from the steady state conditions at 30-33 bar pressure and 1480 rad/s (or the revised value) the power in the test section will be increased from 52,5 kW (or the revised value) to 75 kW (value to be revised taking into account the heat losses compensation and the possible compressor speed reduction) according to the test section control timing. The achievement of acceptable steady state conditions is expected after 15 hours of the loop operation in these conditions.

The verification of the steady state achievement as well as the pressure control have to be performed as in the previous steps before going on with the next one.

Procedure for the LOFA through bypass valve opening

The loop will be in the steady state conditions attained at the end of the start-up: 30-35 bar pressure, 1480 rad/s (or the revised value) compressor velocity and 75 kW (or the revised value) TS power.

The LOFA transient will be started by means of the sharp opening of the by-pass valve FV235 (minimum time allowed by the valve mechanism). After 1000 s the valve will be closed again and the initial conditions will be restored in the loop.

The acquisition of the loop parameters is required every 0.5 s during the 1000 s in which the valve is opened and for 1000 s after its closure, than every minute until the restore of the initial steady state conditions.

The verification of the steady state achievement as well as the pressure control have to be performed as in the start-up procedure.

Procedure for the LOFA through Compressor Speed Reduction

The loop will be at the reference conditions attained at the end of the start-up and re-stabilized after the first LOFA transient: 30-35 bar pressure, 1480 rad/s (or the revised value) compressor velocity and 75 kW (or the revised value) TS power.

The LOFA transient will be piloted by means of the compressor speed reduction from 1480 rad/s down to about 800 rad/s (7600 rpm) in 50 s (or similar time interval according to the



speed compressor control system. After 1000 s the speed compressor will be set again at 1480 rad/s in the same time interval than the initial conditions will be restored in the loop.

The acquisition of the loop parameters is required every 0.5 s during the 1000 s in which the compressor speed has been reduced and for 1000 s after the restoration of the initial speed, then every minute until the restore of the initial steady state conditions.

The verification of the steady state achievement as well as the pressure control have to be performed as in the start-up procedure.

Procedure for the LOCA at higher pressure

Initially the loop will be at the reference conditions restored after the second LOFA: 30-35 bar pressure, 1480 rad/s (or the revised value) compressor velocity and 75 kW (or the revised value) TS power.

The LOCA transient will be started by means of the manual opening of the depressurization valve at the bottom of the tank. A loop depressurization down to about 18 bar in 50 s represents an indicative estimation of the pressure transient to reproduce experimentally, then the valve will be closed again. After 1000 s from the beginning of the LOCA transient the TS power will be reduced from 75 kW to 36 kW (value to be revised taking into account the heat losses compensation and the possible compressor speed reduction) then a new steady state will be attained in the loop.

The acquisition of the loop parameters is required every 0.5 s for 1000 s before and after the power reduction, then every minute until the restore of the new steady state conditions.

The verification of the steady state achievement as well as the pressure control have to be performed as in the start-up procedure.

Procedure for the LOCA at lower pressure

Initially the loop will be at the steady state conditions attained after the first LOCA: about 18 bar pressure, 1480 rad/s (or the revised value) compressor velocity and 36 kW (or the revised value) TS power.

The LOCA transient will be started by means of the manual opening of the depressurization valve at the bottom of the tank. A loop depressurization down to about 9 bar in 50 s represents an indicative estimation of the pressure transient to reproduce experimentally, then the valve will be closed again. After 1000 s from the beginning of the LOCA transient the TS power will be shut off to cool down the loop.

The acquisition of the loop parameters is required every 0.5 s for 1000 s before and after the power shut off, then every minute until the complete cooling down of the loop.