



Advanced gas turbine cycles: new solutions for the near future needs

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Roma, 24 June 2015



Sustainable Combustion
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- Solar eclipse: a real “stress test”
- Flexibility from power generation
- S-CO₂ Power Cycles



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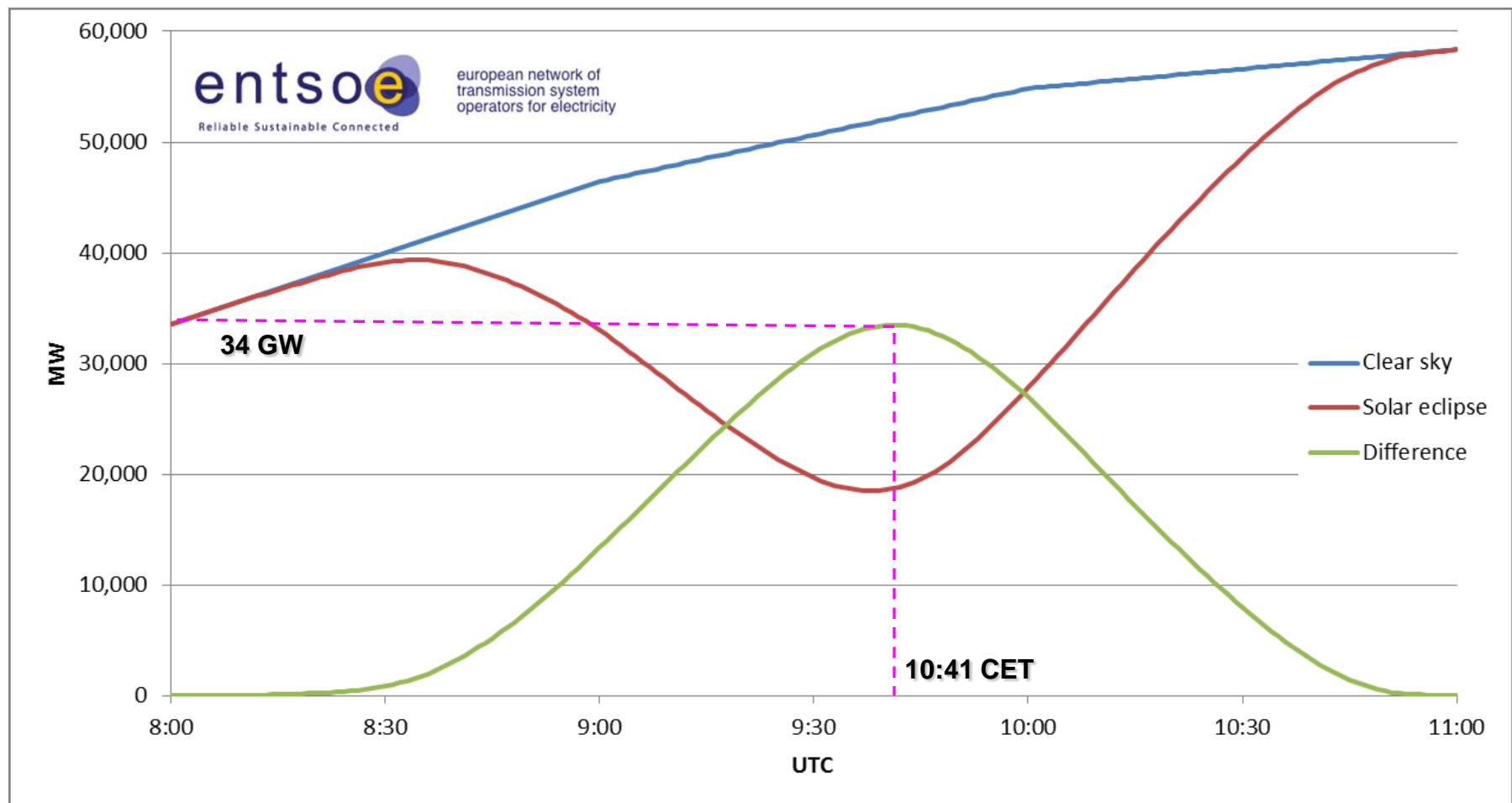
Solar Eclipse: a real “stress test”



People watch as a solar eclipse begins over the Eden Project near St Austell in Cornwall, England, March 20, 2015.
Ben Birchall / AP Photo
From: abcnews.go.com



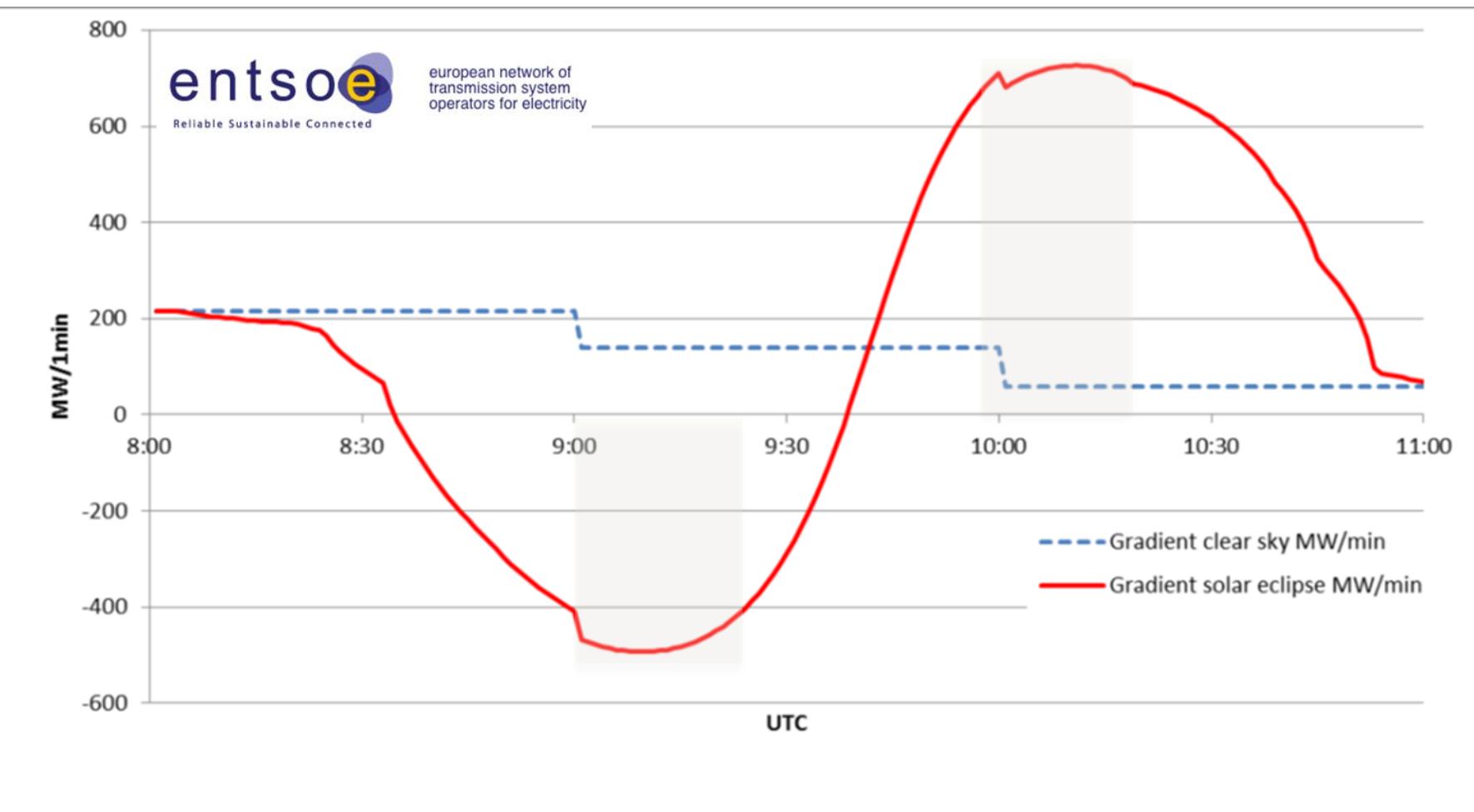
Solar Eclipse: a real “stress-test”



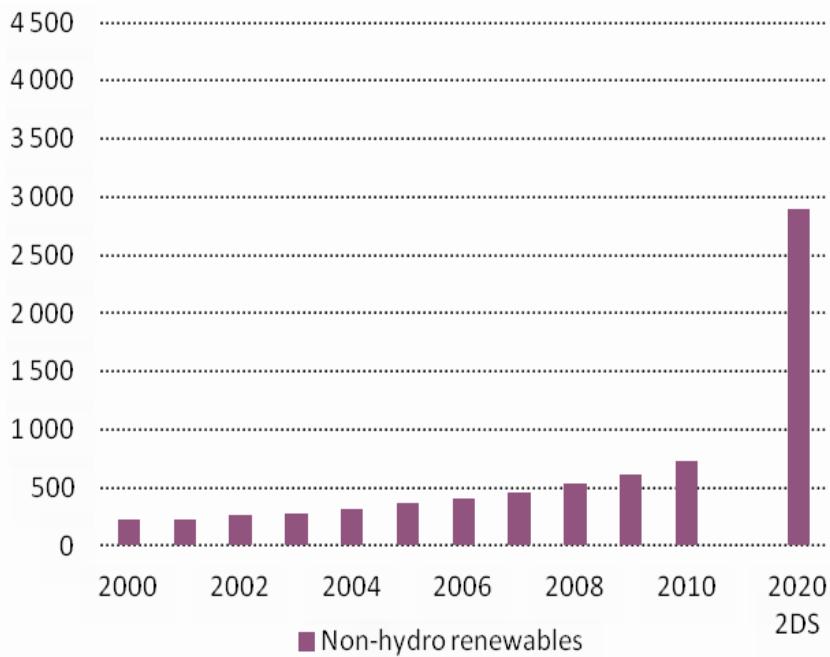
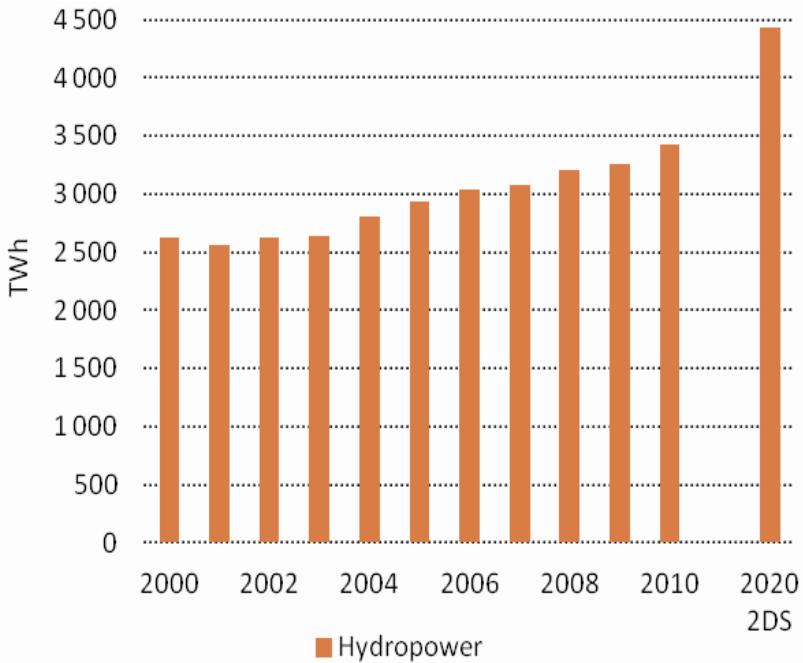
From: ENTSOE - Solar Eclipse 2015 - Impact Analysis, 19 February 2015



Solar Eclipse: a real “stress-test”



From: ENTSOE - Solar Eclipse 2015 - Impact Analysis, 19 February 2015



42%

Average annual
growth in Solar PV

75%

Cost reductions in
Solar PV in just
three years in
some countries

27%

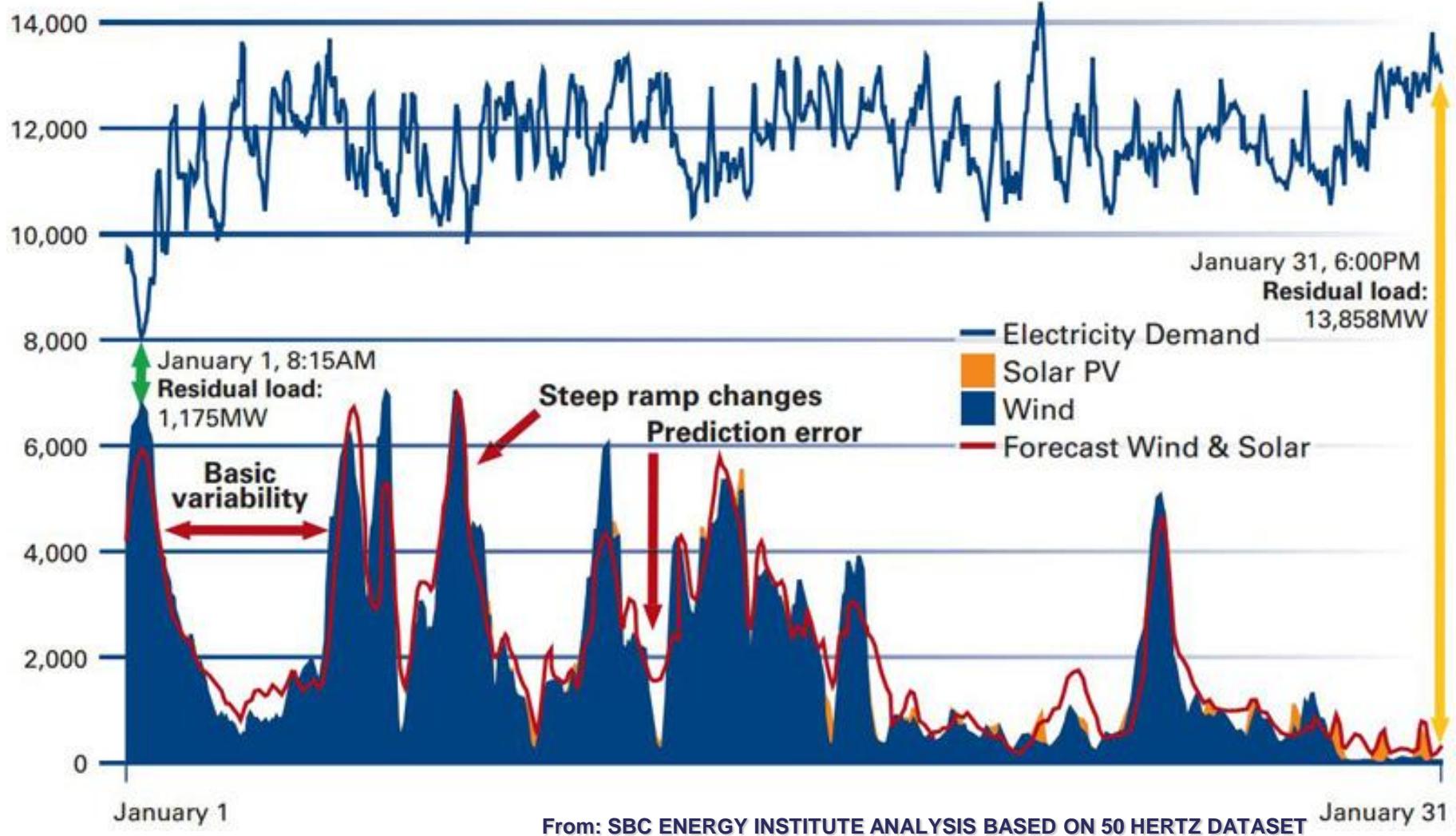
Average annual
growth in wind

From: IEA – Energy Technology Perspectives 2012



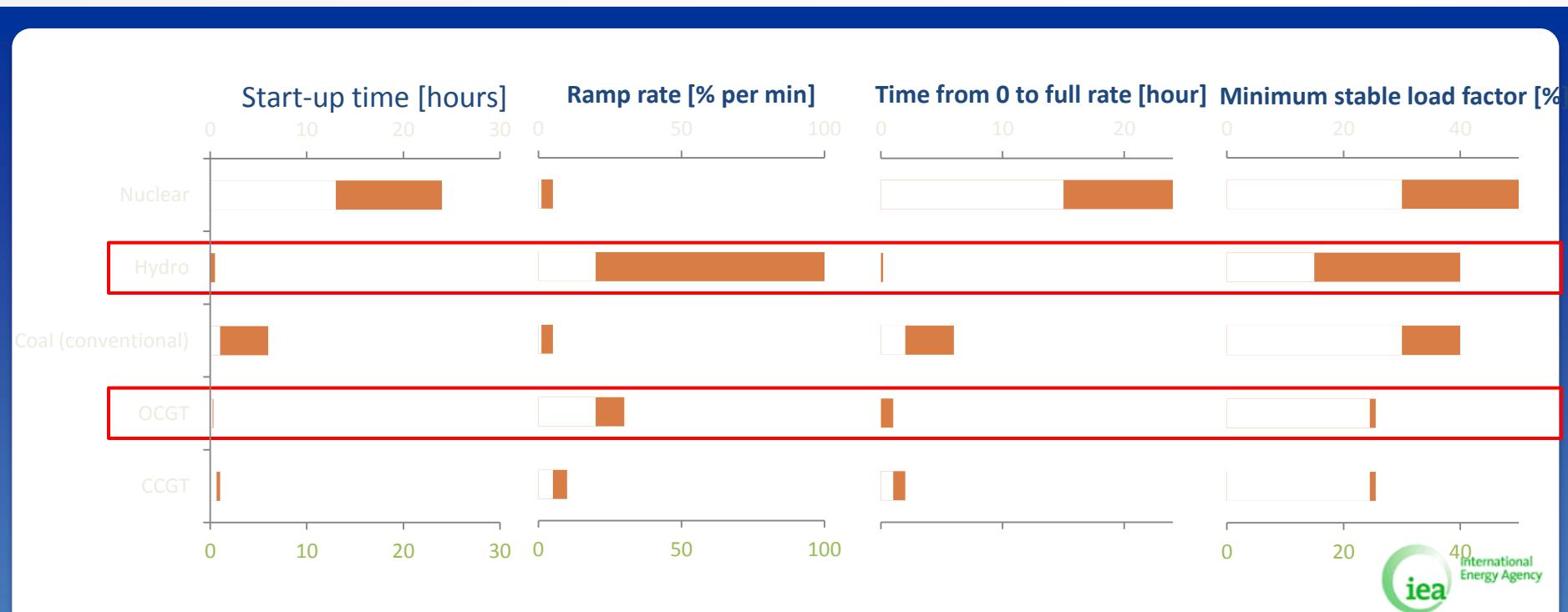
Renewables growth...and load-flexibility

MW, 2011 in northern Germany





Flexibility from Power Generation



- Hydro generation can respond more quickly than other technologies, but the resource is geographically limited
- Open Cycle Gas Turbines are therefore very often considered
- For the traditional base load power plants, a change in operation would translate into reduced load factors, while maintenance cost increase and thus lower financial revenue

From: IEA – Energy Technology Perspectives 2012



and...with CCS?

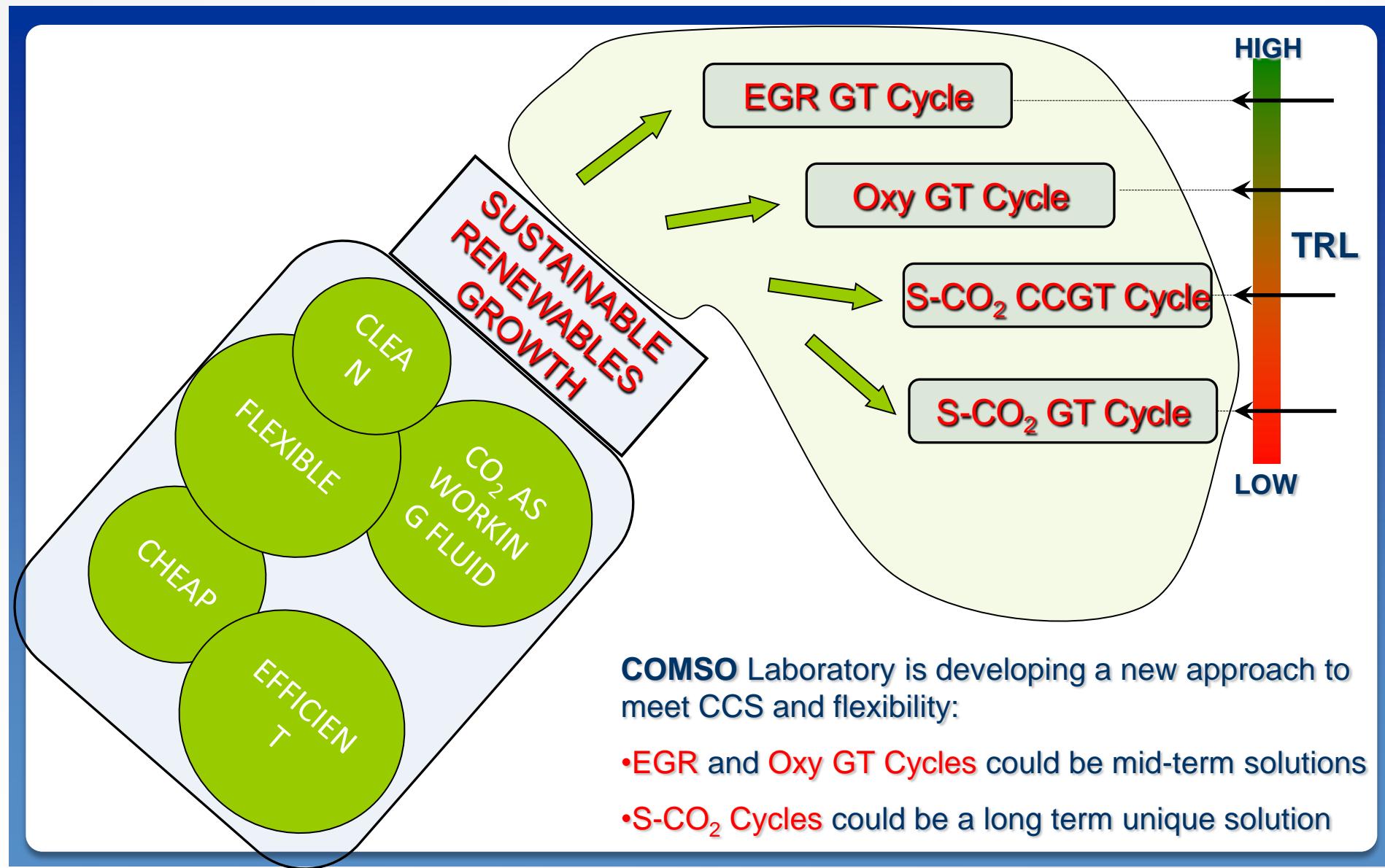
New operational constraints
Larger start-up time
Higher CAPEX and OPEX

Results:

CCS can meet the future flexibility requirements

OCGT without CCS still continue to be a viable cost-effective option for peak load

	Turndown	Cycling capability		Part load efficiency
		Start-up to full load	Ramp rates	
NGCC	Low load operation: 15-25% CC load (10-20% GT load) Min. environmental Load: 40-50% CC NPO (30-40% GT load)	Hot start-up: 45-55 min Warm start-up: 120 min Cold start-up: 180 min	35 - 50 MW/minute max Hot start-up load change rate: - 0-40% GT load: 3-5%/min - HRSRG press.: 1-2%/min - 40-85% GT load: 4-6%/min - 85-100% GT load: 2-3%/min	Approx. constant efficiency down to 85% GT load
with CCS	Post-combustion unit min. load: 30% CO ₂ compressor min. efficient load: 70%	Regenerator preheating: - hot start-up: 1-2 h - warm start-up: 3-4 h	Same as plant w/o CCS	Same as plant w/o CCS
IGCC	Min. env. GT Load: 60% PO. Process unit /air separation unit (ASU) cold box min. load: 50% ASU compr. min. load: 70%	Cold start-up: 80-90 h Gasification hot start-up: 6-8 h ASU hot start-up: 6 h	Gasification ramp rate: 3-5%/min ASU ramp rate: 3%/min	Gross electrical efficiency: 2 percentage points less @ 70% CC load
with CCS	CO ₂ compressor min. efficient load: 70%	Same as plant w/o CCS	Same as plant w/o CCS	Same as plant w/o CCS
USC PC	Min. boiler load: 25- 30%	Very hot start-up: < 1h Hot start-up: 1.5-2.5 h Warm start-up: 3-5 h Cold start-up: 6-7 h	30-50% load: 2-3%/min 50-90% load: 4-8%/min 90-100% load: 3-5%/min	Subcritical boiler: -4 perc. point @ 75% load Supercritical boiler: -2 perc. point @ 75% load
with CCS	Post-combustion unit min. load: 30% CO ₂ compressor min. efficient load: 70%	Regenerator preheating: - hot start-up: 1-2 h - warm start-up: 3-4 h	Same as plant w/o CCS	Same as plant w/o CCS
Oxy fuel				
Air-firing mode	Min. boiler load: 25- 30%	Very hot start-up: < 1h Hot start-up: 1.5-2.5 h Warm start-up: 3-5 h Cold start-up: 6-7 h	30-50% load: 2-3%/min 50-90% load: 4-8%/min 90-100% load: 3-5%/min	Subcritical boiler: -4 perc. point @ 75% load Supercritical boiler: -2 perc. point @ 75% load
Oxy-firing mode	Cold box min. load: 40- 50%. ASU compressor min. efficient load: 70% CO ₂ compressor min. efficient load: 70%	Start-up in air-firing mode, ASU start-up completed in approx. 36 h	ASU ramp rate: 3%/min	Same as plant in air- firing mode

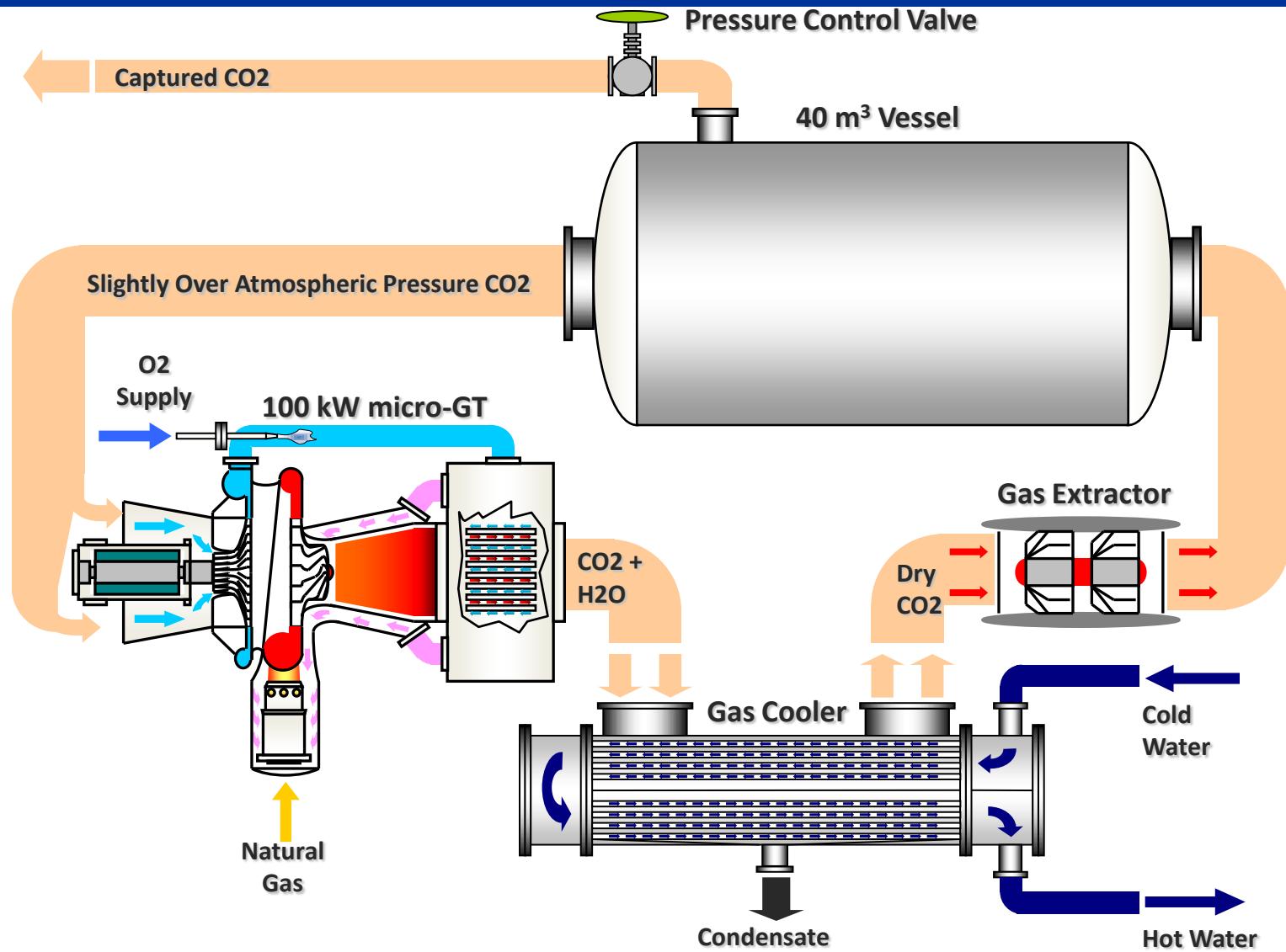




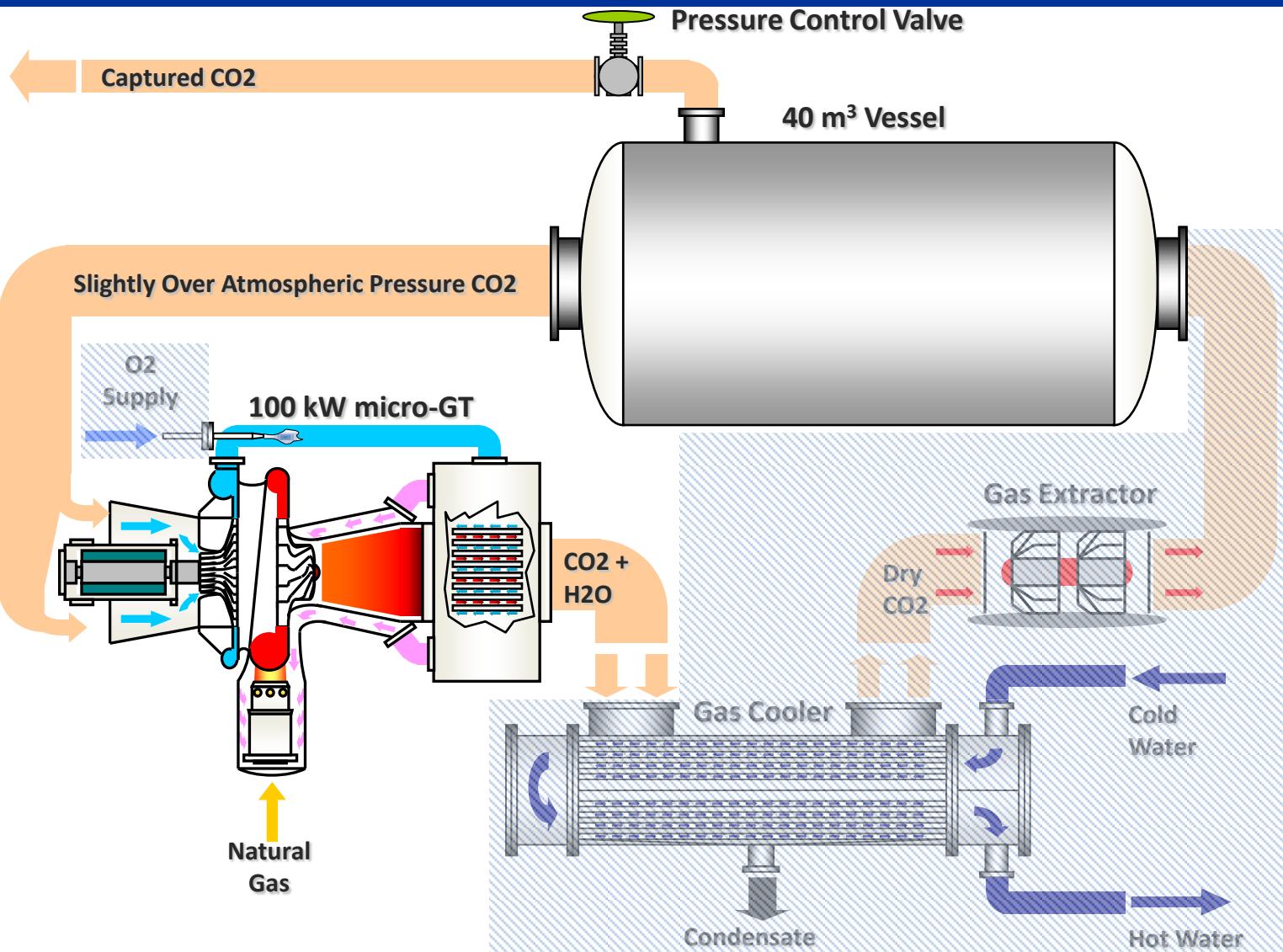
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Advanced GAs TUrbines Rising





G. Messina



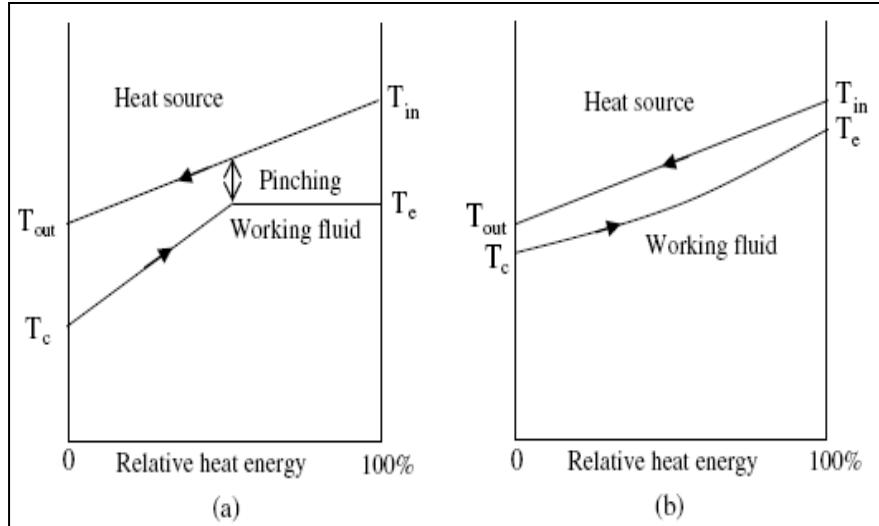
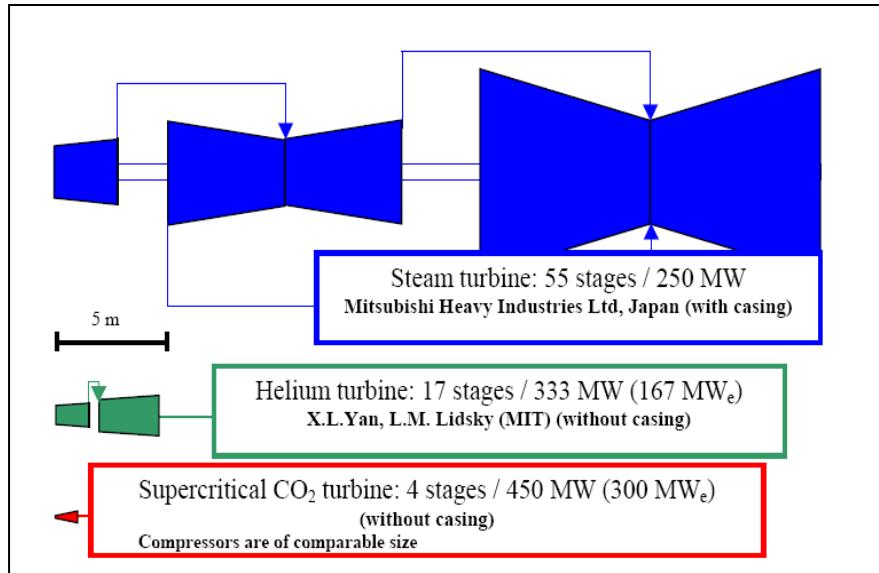


S-CO₂ Peculiarities

Characteristics of an ideal power cycle

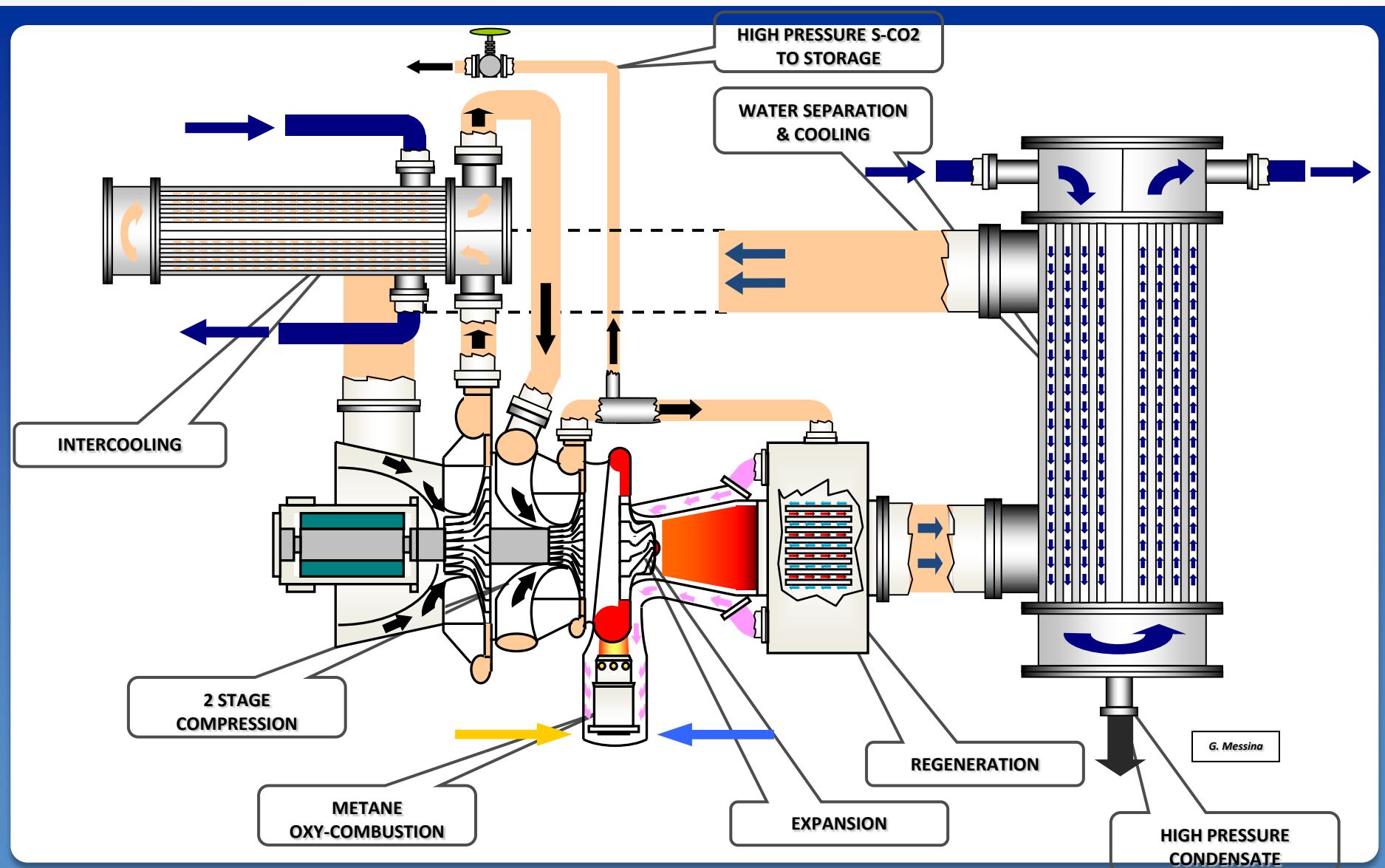
- Good utilization of available heat
 - High expansion, low compression work
 - Direct coupling to heat source
- Benign working fluid
 - Non-corrosive, non-toxic, thermally stable
 - Dry expansion to avoid erosion
- Low capital cost
- Low operation & maintenance (O&M) costs

Supercritical CO₂ meets these characteristics

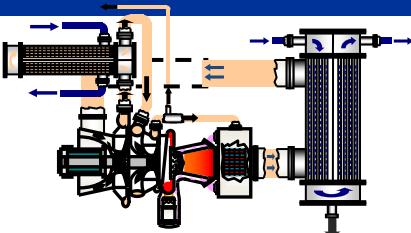




OXY S-CO₂ Cycle: plant layout



OXY S-CO₂ Cycle: simulation results



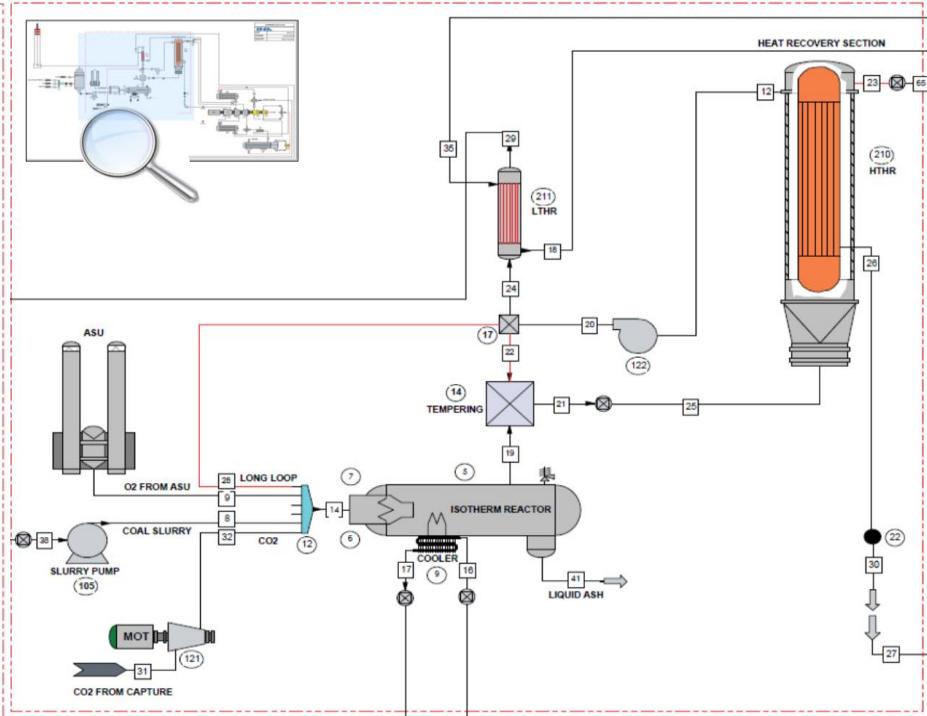
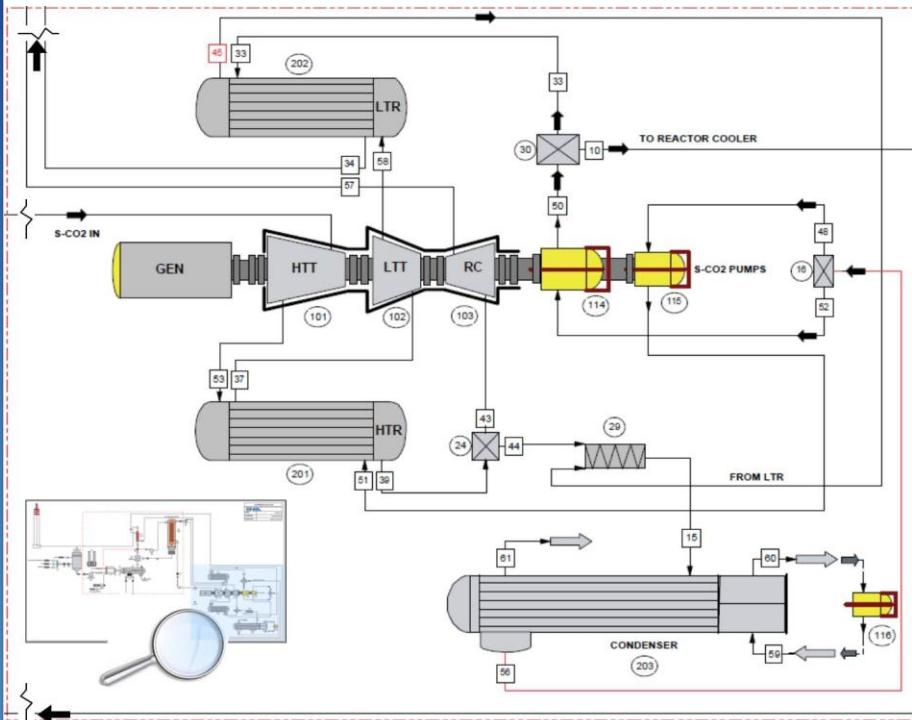
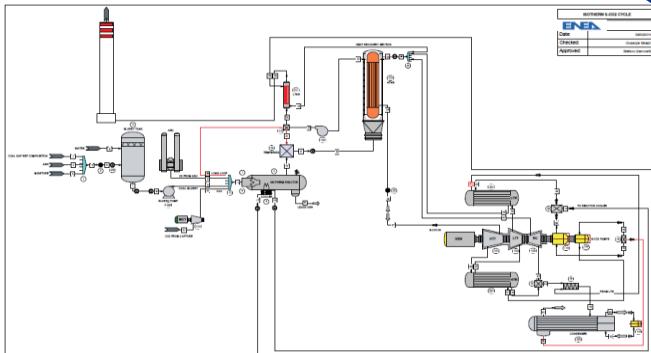
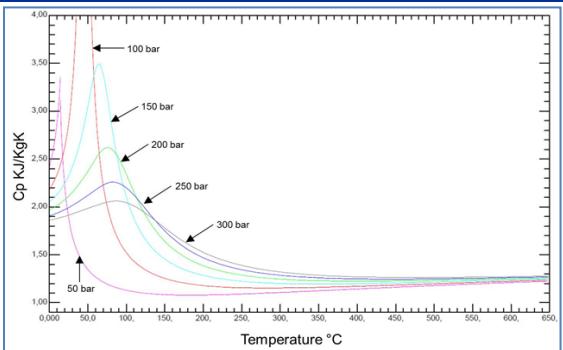
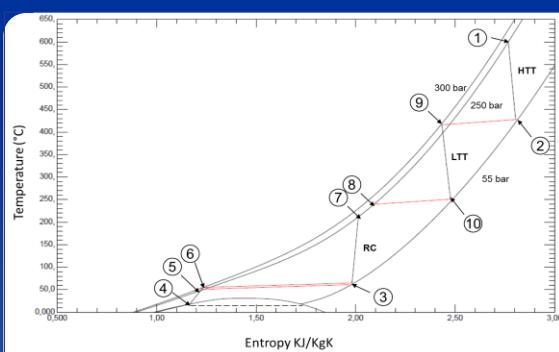
·Fuel ·kg/s	·LHV kJ/kg	·HCOMPRESSOR · kW	·TURB ·kW	·TIT · °C	·TOT · °C	·TOR · °C	·Oxygen ·kg/s	·Oxygen kJ/kg	·EFF
.0,01443	.50010	.32	.80	.1151	.781	.702	.0,058	.42	.0,535
.0,01392	.50010	.36	.83	.1100	.734	.659	.0,058	.42	.0,525
.0,01354	.50010	.35	.83	.1050	.696	.613	.0,056	.40	.0,511

- Regenerator cold side outlet temperature is a key parameter on cycle performance, because of both direct and indirect impact through the TIT limitation.
- A rough sensitivity study was performed by varying TIT, in order to evaluate the “Technological level” on the cycle performance.
- The first principle efficiency LHV basis, is always more than 50%, also with a “state-of-the-art” temperature setting. Energy consumption for oxygen production was included (720 kJ/kg).
- Beside of mechanical energy, other cycle products are a stream of “pipeline ready” CO₂ (300 bar) and a water stream at 30 bar.
- The cycle is virtually “zero emission”.

Giuseppe Messina, “Supercritical Carbon Dioxide Power Cycle”, presentation to European Turbine Network, London, 2013



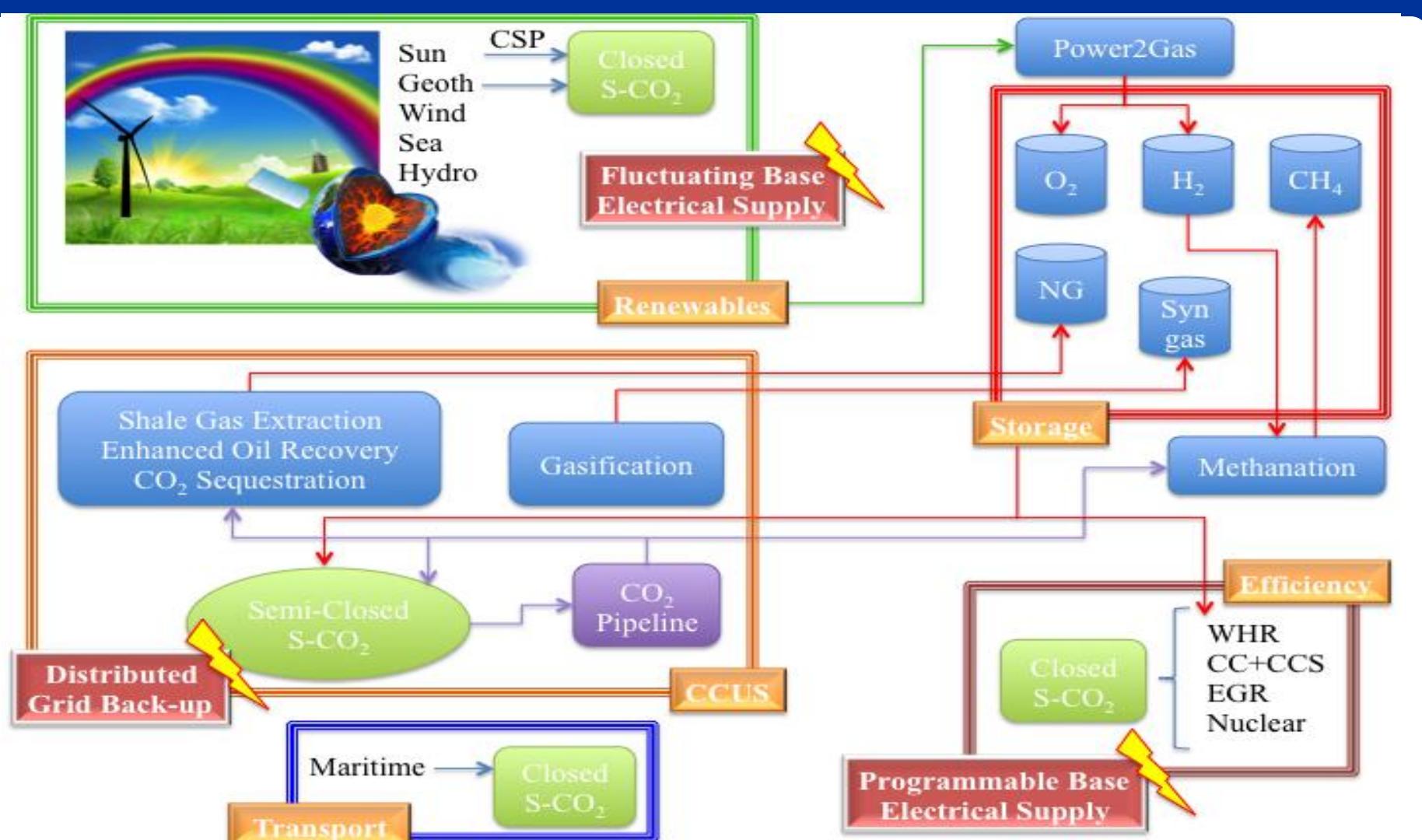
OXYCoal fired S-CO₂ Closed Cycle



G.Messina, E. Giacomazzi, "Modellazione di un Ciclo di Potenza a CO₂ Supercritica da 48 MWt alimentato dal Loop ISOTHERM PWR", Ricerca di Sistema Elettrico, PAR 2013.



An Holistic Solution



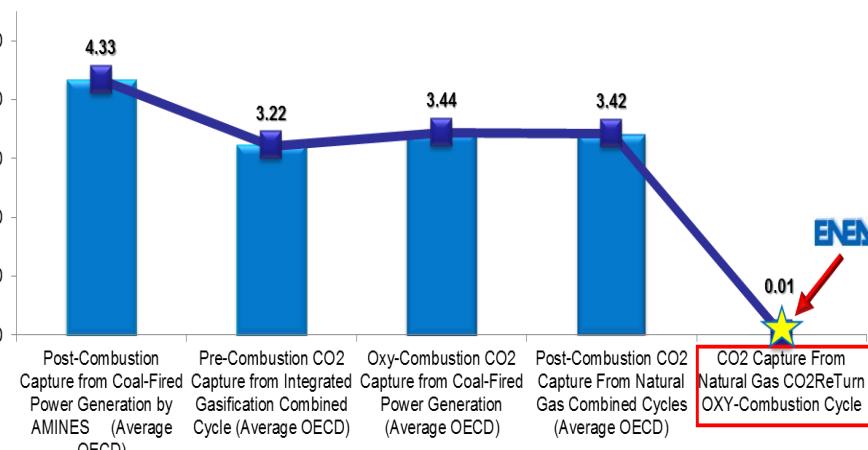
E. Giacomazzi and G. Messina, Exploitation of Supercritical CO₂ Properties – An Holistic Solution for the 21st Century Power Generation, Implantistica Italiana, 2015



S-CO₂ ALBA Cycle

the COMSO Laboratory proposal in figures

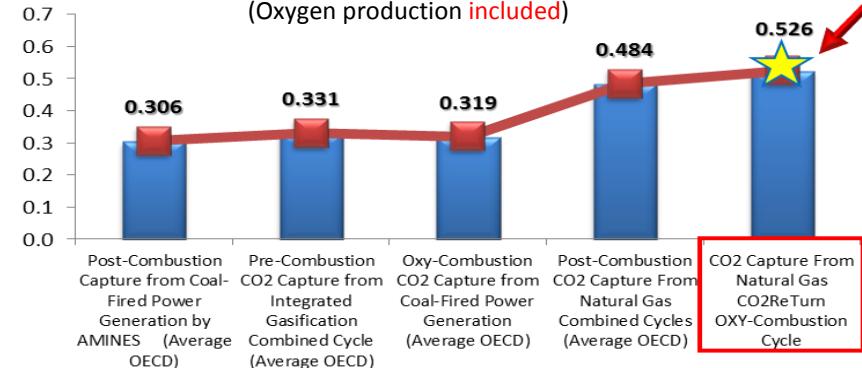
MJ/kg CO₂



Net Efficiency

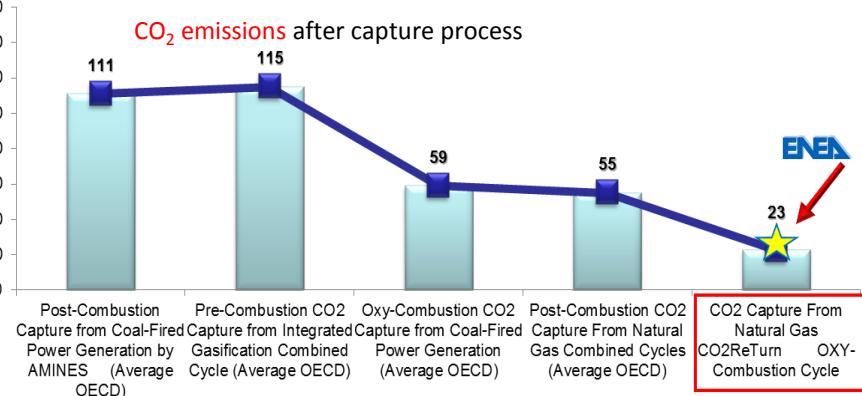
Efficiency (LHV) after capture process
(Oxygen production included)

ENEA



SPECCA: Specific Primary Energy Consumption for CO₂ Avoided. Data elaborated by ENEA from: 1) Rahul Anantharaman et al. "European Best Practice Guidelines for Assessment of CO₂ Capture Technologies", CAESAR Project – FP7, 2011; 2) Matthias Finkenrath, "Cost and Performance of Carbon Dioxide Capture from Power Generation", IEA, 2011.

kg CO₂/MWh



S-CO₂ Advanced Liquid compression BrAyton Cycle

Patenting procedure in progress



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UTTEI – Unit of Advanced Technologies for Energy and Industry

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